

MAIN FILE

PER20240001

original to IOA

918
copy to Petro/62/Nguyen.T

LDEQ RECEIPT

PAAR

2024 JAN 22 PM 3:44



HAND DELIVERED

January 17, 2024

Ms. Bliss Higgins
Assistant Secretary
Louisiana Department of Environmental Quality
Office of Environmental Services
P.O. Box 4313
Baton Rouge, LA 70821-4313

**RE: ET Gathering & Processing LLC
Ajax Amine Plant – A.I. No. 237065
Minor Modification Application to Title V Permit No. 0760-01944-V0
Carbon Capture Project**

Dear Ms. Higgins:

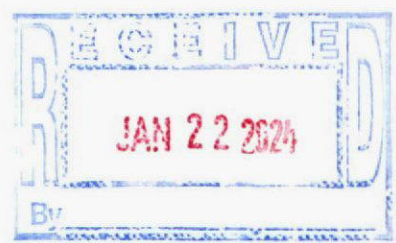
ET Gathering & Processing LLC (ETGP), a subsidiary of Energy Transfer LP, is submitting this minor modification application for Title V Permit No. 0760-01944-V0 seeking to authorize the construction of the Carbon Capture Project at the Ajax Amine Plant.

The minor modification application has been prepared in accordance with LAC 33:III.507.D and LAC 33:III.525.A; therefore, ETGP requests the permit issuance procedures for minor modifications be utilized to revise the permit.

A request for expedited permit processing is being submitted simultaneously with this application. To accommodate the Carbon Capture Project schedule, ETGP is requesting final action on the permit decision as soon as practicable.


As required by the Louisiana Department of Environmental Quality (LDEQ), three copies of the application are being submitted. In accordance with LAC 33:III.525.B.3, an additional copy of the permit application is being submitted electronically to the United States Environmental Protection Agency (USEPA), Region 6.

The permit application fee, in the amount of \$1,960.20 (Online Payment Transaction Number O25F1C0TGF), has been paid to process this application. For a detailed explanation of the fee determination, please refer to Appendix B.



ETGP appreciates your review of this application. If you have any questions regarding the information included in this application, please contact Ms. Hanh Duong of my staff at (713) 989-7158.

Sincerely,

A handwritten signature in blue ink, appearing to read "Joe Perez", with a stylized flourish at the end.

Joe Perez
VP of Operations



Louisiana Department of Environmental Quality

DEQ Online Payment Receipt

AI #	Reference #	Description	Type	Base Fee	Quantity	Line Total
237065	--	Fee Code 0130 - Minor Mod	Product	\$2,053.00	1	\$2,053.00

Payment Totals

Sub Total: \$2,053.00

Fee: \$40.03

Total: \$2,093.03

Payee Information

Name: LISA M GARCIA

Email: LISA.GARCIA@ENERGYTRANSFER.COM

Transaction Information

Receipt Number: 55750

Authorization Code: N/A

Transaction Number: O25F1COTGF

Transaction Date: Wednesday, January 17, 2024 3:07 PM

Transaction Status: pro

Transaction Message: N/A

[All Receipts](#)

Louisiana Department of Environmental Quality 602 N. Fifth Street Baton Rouge, LA 70802

For issues call 1-866-896-LDEQ.

**ET Gathering & Processing LLC
Ajax Amine Plant- AI No. 237065**

ORIGINAL

**Title V Operating Permit
Minor Modification Application to
Permit No. 0760-01944-V0**

Prepared by:

Alliance Technical Group

Baton Rouge Office
450 Laurel Street, Suite 2050
Baton Rouge, LA 70801

January 2024

**Part 70 Operating Permit
Minor Modification Application to
Permit No. 0760-01944-V0**

**ET Gathering & Processing LLC
Ajax Amine Plant
AI No. 237065**

Alliance Technical Group

Baton Rouge Office
450 Laurel Street, Suite 2050
Baton Rouge, LA 70801

January 2024



TABLE OF CONTENTS

1. INTRODUCTION	1
1.1. Facility Description	1
1.2. Facility Information and Location	1
1.3. Application Overview	2
2. PROJECT DETAILS	5
2.1. Project Overview	5
2.2. Project Schedule	5
2.3. Project Affected Sources	5
2.3.1. Engines	6
2.3.2. Loading	6
2.3.3. Dehydrator	7
2.3.4. Storage Vessels	7
2.3.5. Fugitive Emission Components	8
3. NSR APPLICABILITY	9
3.1. Regulatory Applicability	9
4. REGULATORY APPLICABILITY	10
4.1. Regulatory Applicability Background	10
4.2. New Source Performance Standards – 40 CFR 60 (NSPS)	10
4.2.1. Engines	10
4.2.2. Storage Vessels	11
4.2.3. Fugitive Emission Components	12
4.3. National Emission Standards for Hazardous Air Pollutants (NESHAP) – 40 CFR 61	13
4.4. National Emission Standards for Hazardous Air Pollutants for Source Categories (MACT) – 40 CFR 63	13
4.4.1. Engines	14
4.4.2. Dehydrators	14
4.4.3. Storage Vessels	15
4.4.4. Fugitive Emission Components	15
4.5. Compliance Assurance Monitoring	16
4.6. Louisiana State Air Quality Regulations	16
4.6.1. Engines	17
4.6.2. Sulfur Loading and Handling	18
4.6.3. Glycol Dehydrators (CO ₂ Dehydrator Unit Vents)	18
4.6.4. Heaters (CO ₂ Dehydrator Reboiler)	18
4.6.5. Storage Vessels	19
4.6.6. Loading	20
4.6.7. Fugitive Emission Components	20
4.7. LAC 33:III Chapter 51 – Comprehensive Toxic Air Pollutant Emission Control Program	20
4.7.1. Louisiana MACT Applicability	20
4.7.2. LA MACT Reporting Requirements	21
4.7.3. Emission Control and Reduction Requirements and Standards	21
4.7.4. Air Toxics Fees	21

5. SUMMARY OF PERMIT RECONCILIATIONS	23
5.1. Reconciliation Background	23
5.2. Permit Revision Summary	23
5.2.1. <i>SO₂ Calculation Methodology</i>	23
5.2.2. <i>Revision to Uncontrolled Vents</i>	23
5.2.3. <i>Applicable Regulations and Specific Requirements Updates</i>	24
6. APPLICATION FOR APPROVAL OF EMISSIONS OF AIR POLLUTANTS FROM PART 70 SOURCES (AAEAP)	25
APPENDIX A: PTE CALCULATION DOCUMENTATION	A
APPENDIX B: FEE CALCULATION	B
APPENDIX C: SECRETARY OF STATE CERTIFICATION	C

LIST OF TABLES

- Table 2-1. Carbon Capture Project Affected Source List
- Table 2-2. Fugitive Emission Components Summary
- Table 4-1. Emissions Unit NSPS Summary
- Table 4-2. Project Affected Storage Vessel Characteristics
- Table 4-3. Emissions Unit MACT Summary
- Table 4-4. Emissions Unit LAC Summary
- Table 4-5. Project Affected Storage Vessel Characteristics
- Table 4-6. LA MACT Analysis for Benzene
- Table 5-1. Maximum Hourly SO₂ Revision
- Table 5-2. Emission Rate Changes to Uncontrolled Vents

LIST OF FIGURES

Figure 1-1. Site Location Map

Figure 1-2. Process Flow Diagram

1. INTRODUCTION

1.1. FACILITY DESCRIPTION

ET Gathering & Processing LLC (ETGP), a subsidiary of Energy Transfer LP, owns and operates the Ajax Amine Plant, in DeSoto Parish, Louisiana. The Ajax Amine Plant currently operates under Title V Permit No. 0760-01944-V0, issued on July 18, 2023.

At the Ajax Amine Plant, there are two natural gas amine treating and dehydration plants capable of processing up to 150 MMSCFD of natural gas each (300 MMSFCD total). Natural gas is transported to the facility via a pipeline gathering system and routed to inlet separators, where water is initially removed from the inlet stream. The produced water is routed to four (4) produced water storage tanks (EQT0015 through EQT0018) and then removed from the facility via trucks (EQT0019).

From the separators, the natural gas is routed through the Plant 1 Amine Treater (EQT0001) and the Plant 2 Amine Treater (EQT0005) to reduce hydrogen sulfide (H₂S) and carbon dioxide (CO₂) in the natural gas. In the amine treater system, inlet gas passes through a contactor vessel where H₂S and CO₂ are absorbed by the amine solution. The "rich" amine solution is then be flashed, filtered, and heated by the amine reboiler to regenerate the amine. The heat for the amine reboilers in Plant 1 and 2 is supplied by an 85.0 million British Thermal Units per hour (MMBtu/hr) hot oil heater (EQT0002 and EQT0006 respectively). The acid gas and flash gas from the Plant 1 and 2 amine treater regenerator vents and flash tanks are routed to either the facility's fuel system or the Plant 1 and 2 thermal oxidizers (EQT0009 and EQT0010 respectively).

After the gas passes through the amine treater system, the Plant 1 glycol dehydrator (EQT0003) and Plant 2 glycol dehydrator (EQT0007) are used to remove water from the gas. The dehydration process gas passes through a contactor vessel where water is absorbed by triethylene glycol (TEG). The "rich" glycol-containing water goes to a glycol reboiler, where heat is used to boil off the water. The heat ratings for the Plant 1 and 2 glycol reboilers are 5.0 MMBtu/hr (EQT0004 and EQT0008 respectively). Water removed from the "rich" glycol is then stored in the produced water storage tanks. The glycol dehydrator flash and BTEX vents are routed to the Plant 1 and 2 thermal oxidizers.

Four (4) Caterpillar G3606 A4 natural gas-fired compressor engines (EQT0011 through EQT0014) rated at 1,875 horsepower (HP) each are used to transport the natural gas out of the facility. Each of the four engines are equipped with oxidation catalysts.

1.2. FACILITY INFORMATION AND LOCATION

The Ajax Amine Plant is located on Highway 174 approximately 4.9 miles east of Pleasant Hill on the right-hand side (See Figure 1-1 at the end of this section). A process flow diagram (PFD) associated with the Carbon Capture Project is included as Figure 1-2 at the end of this section.

Facility Information:

Responsible Official:

Mr. Joe Perez
VP of Operations
Energy Transfer LP
4550 Marlana St
Bossier City, LA 71111
Phone Number: (713) 989-7030
Email Address: Joe.Perez3@energytransfer.com

Technical contact for questions about the application or facility:

Ms. Hanh Duong
Staff Engineer
Energy Transfer LP
1300 Main Street
Houston, TX 77002
Phone Number: (713) 989-7158
Email Address: Hanh.Duong@energytransfer.com

Mailing Address: Same as contact information, above.


1.3. APPLICATION OVERVIEW


This submittal is seeking authorization for the implementation of the Carbon Capture Project at the Ajax Amine Plant, as detailed in Section 2. The Carbon Capture Project constitutes a minor modification as defined via Louisiana Administrative Code (LAC) Title 33 Part III Chapter 525 (LAC 33:III.525).

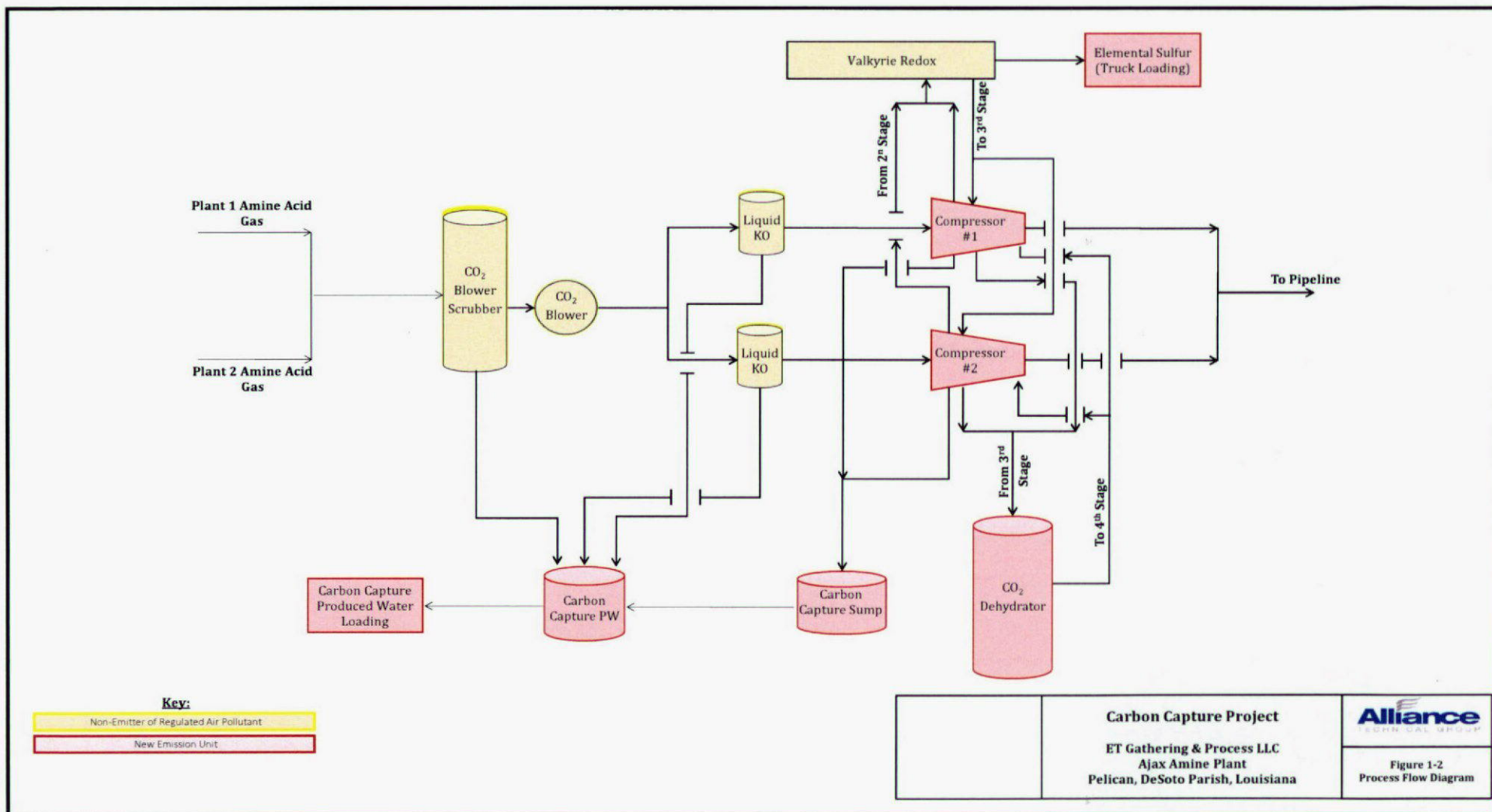
This permit application has been prepared in accordance with LAC 33:III.507.D and the proposed minor modification meets the criteria listed in LAC 33:III.525.A; therefore, ETGP requests that minor modification procedures be used to revise the permit. All information required to process this minor modification application can be found as organized as follows:

- Section 1 - Introduction
- Section 2 - Project Details
- Section 3 - New Source Review (NSR) Applicability
- Section 4 - Regulatory Applicability
- Section 5 - Reconciliations and Permit Revisions
- Section 6 - Application for Approval of Emissions of Air Pollutants from Part 70 Sources (AAEAP)
- Appendix A - Potential to Emit (PTE) Calculation Documentation
- Appendix B - Fee Calculation
- Appendix C - Secretary of State Certificate



 Approx. Plant Boundary

DESIGNED BY JB		SHEET TITLE AERIAL SITE MAP	JOB NAME AJAX AMINE PLANT ET GATHERING & PROCESS LCC	PROJECT NO. AES-2023-0088	REV. NO.
CHECKED BY JB		DATE 10/24/2023	SCALE SHOWN	DWG. NO. 1-1	
APPROVED BY JB					
DRAWN BY ALB					



2. PROJECT DETAILS

2.1. PROJECT OVERVIEW

The Ajax Amine Plant currently operates under Title V Permit No. 0760-01944-V0, issued on July 18, 2023. With this minor modification application, ETGP is proposing to modify Title V Permit No. 0760-01944-V0 in order to authorize the proposed Carbon Capture Project.

With the Carbon Capture Project, ETGP proposes to produce a purified CO₂ gas stream that utilizes the acid gas produced from the existing Plant 1 Amine Unit and Plant 2 Amine Unit as the feedstock. The purified CO₂ stream will be sent offsite via pipeline. The proposed scope of work associated with the Carbon Capture Project at the Ajax Amine Plant includes the following physical modifications and construction activities:

- The installation of two (2) new 2,500 HP caterpillar natural gas-fired compressor engines, CAT G3608 Compressor Engine (EPN: 1-23; EQT TBD) and CAT G3608 Compressor Engine (EPN: 2-23; EQT TBD) equipped with oxidation catalyst for control of carbon monoxide (CO) and volatile organic compounds (VOC).
- The installation of a new Valkyrie Redox unit for the removal and conversion of H₂S to elemental sulfur.
- The installation of a new TEG Dehydration System that includes a contact tower and associated regeneration system equipped with a 1 MMBTU/hr reboiler, CO₂ Dehydrator Unit Reboiler (EPN: 5-23B; EQT TBD).
- The installation of two new 750 barrel produced water storage vessels, Carbon Capture Produced Water Storage Tank (EPN: 6-23; EQT TBD) and Carbon Capture Produced Water Storage Tank (EPN: 7-23; EQT TBD).
- Various miscellaneous chemical tanks and totes that qualify as and are proposed to be permitted as insignificant activities (IA).
- The addition of new fugitive components to accommodate the proposed changes.

2.2. PROJECT SCHEDULE

The scope of work for the proposed Carbon Capture Project, as detailed in Section 2.1, is currently anticipated to commence construction in second quarter (2Q) of 2025 and anticipated to commence operation in fourth quarter (4Q) of 2026.

2.3. PROJECT AFFECTED SOURCES

ETGP has conducted a thorough analysis of the sources affected due to the Carbon Capture Project, including all potential upstream and downstream impacts. For a detailed list of the affected sources, including those proposed new emission sources, see Table 2-1, below. A narrative of the emission increases associated with each affected source, categorized by source type, can be found in the subsections that follow.

Table 2-1. Carbon Capture Project Affected Source List

Source Type	TEMPO ID	Source ID	Description	New Source
Engine	EQT TBD	1-23	CAT G3608 Compressor Engine	Yes
Engine	EQT TBD	2-23	CAT G3608 Compressor Engine	Yes
Loading	EQT TBD	3-23	Sulfur Loading and Handling	Yes
Dehydrator	EQT TBD	5-23B	CO ₂ Dehydrator Reboiler	Yes
Tank	EQT TBD	6-23	Carbon Capture Produced Water Storage Tank	Yes
Tank	EQT TBD	7-23	Carbon Capture Produced Water Storage Tank	Yes
Loading	EQT TBD	8-23	Carbon Capture Produced Water Loading	Yes
Fugitive	FUG 0001	FUG	Fugitive Emissions	No
Tank	IA	N/A	Carbon Capture Sump	Yes
Tank	IA	N/A	Surfactant (S200) Storage Tank	Yes
Tank	IA	N/A	TEG Storage Tank	Yes

2.3.1. Engines

With the Carbon Capture Project, and as referenced in Section 2.1, ETGP proposes the installation of two new 2,500 HP natural gas fired, five-stage reciprocating compressors, CAT G3608 Compressor Engine (EPN: 1-23; EQT TBD) and CAT G3608 Compressor Engine (EPN: 2-23; EQT TBD), allowing for the purified CO₂ stream to be sent offsite via pipeline. The compressors are proposed to be equipped with oxidation catalyst allowing for the control of CO and VOC emissions. For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup for the reciprocating compressors can be found in Appendix A of this application.

2.3.2. Loading

2.3.2.1. Sulfur Loading and Handling

As previously referenced in Section 2.1, with the Carbon Capture Project, ETGP proposes the installation of a new Valkyrie Redox unit that will allow for the removal and conversion of H₂S to elemental sulfur. The elemental sulfur will be produced at a rate of 1,000 pounds per day (lb/day) and will be conveyed from the Valkyrie Redox unit to a roll-off box that will then be trucked offsite.

For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup for Sulfur Loading and Handling (EPN 3-23; EQT TBD) can be found in Appendix A of this application.

2.3.2.2. Produced Water Loading

With the proposed Carbon Capture Project, ETGP will remove liquids from the process stream via the installation of a blower scrubber and previously referenced installation of the reciprocating compressors. The liquids will be routed to the proposed two new Carbon Capture Produced Water Storage Tanks, at a rate of 200 barrels per day (BPD), and then subsequently sent offsite via the existing truck loading operations, Carbon Capture Produced Water Loading (EPN: 8-23; EQT TBD).

For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup for the Carbon Capture Produced Water Loading (EPN: 8-23; EQT TBD) can be found in Appendix A of this application.

2.3.3. Dehydrator

2.3.3.1. Dehydrator Unit Process Vents

With the Carbon Capture Project and as referenced in Section 2.1, ETGP proposes to install a new TEG Dehydration System for the removal of any remaining moisture entrained within the process. The TEG Dehydration System will have two atmospheric process vents; however, will not have any regulated pollutant entrained in the atmospheric process vents. Therefore, ETGP is proposing to not permit the CO₂ Dehydrator Unit Vents as an emission point.

2.3.3.2. Dehydrator Unit Reboiler

A glycol reboiler, CO₂ Dehydrator Reboiler (EPN: 5-23B; EQT TBD), is proposed to be installed with the new TEG Dehydration System, which will supply heat to the system, allowing for the regeneration of the TEG. The CO₂ Dehydrator Reboiler will utilize a natural gas fuel and have a rated heat input of 1 MMBTU/hr.

For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup for the CO₂ Dehydrator Reboiler can be found in Appendix A of this application.

2.3.4. Storage Vessels

2.3.4.1. Produced Water Storage

With the Carbon Capture Project and as referenced in Section 2.1, ETGP proposes to install two new 750 barrel produced water storage vessels, Carbon Capture Produced Water Storage Tank (EPN: 6-23; EQT TBD) and Carbon Capture Produced Water Storage Tank (EPN: 7-23; EQT TBD). As previously referenced in Section 2.3.2.2, 200 BPD of liquids will be removed from the process and routed to the newly proposed produced water storage vessels.

For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup for the produced water storage vessels can be found in Appendix A of this application.

2.3.4.2. Miscellaneous Storage

With the Carbon Capture Project and as referenced in Section 2.1, ETGP proposes the installation of the following chemical tanks and totes:

- 1,000-gallon Carbon Capture Sump;
- 500-gallon Surfactant (S200) Storage Tank;
- 330-gallon TEG Storage Tank.

Per LAC 33:III.501.B.5, all aforementioned storage vessels will qualify as an IA as they are not subject to any federally enforceable emission limitation and will emit less than the minimum emission rate (MER) for all Louisiana Toxic Air Pollutants (LTAP) listed in LAC 33:III.5112, Table 51.1. For a detailed regulatory applicability analysis and EIQ refer to Section 4 and Section 6 of this application, respectively. A detailed PTE calculation backup for the proposed chemical tanks and totes can be found in Appendix A of this application.

2.3.5. Fugitive Emission Components

As referenced in Section 2.1 of this application, as part of the Carbon Capture Project, ETGP proposes to add various fugitive components associated with the construction and modification of the aforementioned processes. A summary of the increase in fugitive component counts, including service and component classification can be found in Table 2-2, below. For a detailed regulatory applicability analysis and EIQ associated with the Fugitive Emissions (EPN: FUG; FUG 0001) refer to Section 4 and Section 6, respectively. Additionally, a detailed PTE calculation backup can be found in Appendix A of this application.

Table 2-2. Fugitive Emission Components Summary

Component Classification	Service	Increase in Component Counts
Valves	Gas/Vapor	483
	Light Oil	15
	Heavy Oil	117
Pump Seal	Light Oil	4
	Heavy Oil	0
Connectors	Gas/Vapor	443
	Light Oil	0
	Heavy Oil	84
Other ¹	Gas/Vapor	52
	Light Oil	4
	Heavy Oil	0
Open-ended Lines	All	4

1: Other category includes compressors, sampling stations, and pressure relief devices

3. NSR APPLICABILITY

3.1. REGULATORY APPLICABILITY

The Ajax Amine Plant operates under Standard Industrial Classification (SIC) code 1389 and is not included as one of the twenty-seven listed source categories of 40 CFR 52.21(b)(1)(i)(a) and further codified via LAC 33:III.509.A. Therefore, the Prevention of Significant Deterioration (PSD) applicability threshold of 250 tons per year (TPY) applies to the Ajax Amine Plant for all PSD-regulated pollutants. As observed in Section 6 and Appendix A, the Ajax Amine Plant does not exceed 250 TPY for any PSD-regulated pollutant; therefore, the site is an existing minor source for purposes of PSD, and no further review is required.

Further, it should be noted that with the Carbon Capture Project and as previously referenced in Section 2, ETGP proposes to install a Valkyrie Redox system to recover elemental sulfur, which meets the definition of a sulfur recovery plant. Sulfur recovery plants are included in the twenty-seven listed source categories of 40 CFR 52.21(b)(1)(i)(a) and further codified via LAC 33:III.509.A. The sulfur recovery plant is a nested source within the Ajax Amine Plant and would be subject to PSD review as a standalone facility should the applicability threshold of 100 TPY of any PSD-regulated pollutant be exceeded. However, as observed in Section 6 and Appendix A, the Valkyrie Redox unit does not exceed 100 TPY of any PSD-regulated pollutant; therefore, PSD review does not apply to the Valkyrie Redox unit.

4. REGULATORY APPLICABILITY

4.1. REGULATORY APPLICABILITY BACKGROUND

Title 40 of the Code of Federal Regulations (40 CFR) and the LAC, Title 33 – Environmental Quality, Part III – Air Quality were reviewed to determine all applicable air regulations for all sources found to be affected due to the proposed Carbon Capture Project. Regulatory Tables 1, 2, 3, and 4, located in Section 22 of the AAEAP, found in Section 6 of this application, provide details of the applicability of federal and state regulations and compliance monitoring requirements. Specific details concerning the regulatory applicability can additionally be found below for those sources affected due to the Carbon Capture Project. For any existing source not referenced below, ETGP is not proposing to modify the regulatory applicability as found in the current effective operating permit.

4.2. NEW SOURCE PERFORMANCE STANDARDS - 40 CFR 60 (NSPS)

The NSPS were authorized by Section 111 of the Clean Air Act (CAA) and were developed as technology-based standards that apply to specific categories of stationary sources. The NSPS apply to new, modified, and reconstructed affected facilities (i.e., emission units) in specific source categories.

Each emissions source affected by the Carbon Capture Project and its applicability with an NSPS are shown in Table 4-1, below. In the subsections that follow, a detailed NSPS applicability analysis for each source can be found categorized by source type.

Table 4-1. Emissions Unit NSPS Summary

Source Type	TEMPO ID	Source ID	Description	Kb	KKK	JJJ	OOOa
Engine	EQT TBD	1-23	CAT G3608 Compressor Engine			X	
Engine	EQT TBD	2-23	CAT G3608 Compressor Engine			X	
Loading	EQT TBD	3-23	Sulfur Loading and Handling				
Dehydrator	EQT TBD	5-23B	CO ₂ Dehydrator Reboiler				
Tank	EQT TBD	6-23	Carbon Capture Produced Water Storage Tank				
Tank	EQT TBD	7-23	Carbon Capture Produced Water Storage Tank				
Loading	EQT TBD	8-23	Carbon Capture Produced Water Loading				
Fugitive	FUG 0001	FUG	Fugitive Emissions				X
IA	N/A	IA-11	Carbon Capture Sump				
IA	N/A	IA-12	Surfactant (S200) Storage Tank				
IA	N/A	IA-13	TEG Storage Tank				

4.2.1. Engines

This section includes the regulatory applicability analysis for all potentially applicable NSPS associated with the installation of the two reciprocating compressors, CAT G3608 Compressor Engine (EPN: 1-23; EQT TBD) and CAT G3608 Compressor Engine (EPN: 2-23; EQT TBD).

4.2.1.1. 40 CFR 60 Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines

The provisions of NSPS JJJJ are potentially applicable to owners or operators that commence construction (i.e., order) of a stationary spark ignition (SI) internal combustion engine (ICE) after June 12, 2006. The proposed CAT G3608 Compressor Engines will become subject to the provisions of NSPS JJJJ as they will commence construction after June 12, 2006. The proposed engines will be subject to the emission standards of NSPS JJJJ, as found in Table 1, for non-emergency SI natural gas fired engines with maximum power rating of greater than or equal to 500 HP. ETGP proposes to comply with the emission standards by purchasing a non-certified engine and complying with the provisions 40 CFR 60.4243(b)(2)(ii), that requires the development of a maintenance plan, recordkeeping of all conducted maintenance, initial performance testing, and subsequent performance testing every 8,760 hours or three years (whichever comes first).

4.2.1.2. 40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced after September 18, 2015

The provisions of NSPS OOOOa are applicable to reciprocating compressors, in natural gas service, not located at a well site, which commences construction, modification or reconstruction after September 18, 2015. The proposed reciprocating compressors will not be in natural gas service; therefore, the provisions of NSPS OOOOa do not apply.

4.2.2. Storage Vessels

This section includes the regulatory applicability analysis associated with the following affected storage vessels, found in Table 4-2, for all potentially applicable NSPS.

Table 4-2. Project Affected Storage Vessel Characteristics

TEMPO ID	Source ID	Description	Product	Construction Year ¹	Capacity (Gal)	Max True Vapor Pressure (psia)
EQT TBD	6-23	Carbon Capture Produced Water Storage Tank	Produced Water	Proposed 2024	31,500	0.50
EQT TBD	7-23	Carbon Capture Produced Water Storage Tank	Produced Water	Proposed 2024	31,500	0.50
IA	N/A	Carbon Capture Sump	Produced Water	Proposed 2024	1,000	0.50
IA	N/A	Surfactant (S200) Storage Tank	Surfactant	Proposed 2024	500	0.02
IA	N/A	TEG Storage Tank	TEG	Proposed 2024	330	<0.01

1: Year referenced represents the latest year of construction, reconstruction, or modification.

4.2.2.1. 40 CFR 60 Subpart Kb - Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984

The provisions of NSPS Kb are potentially applicable to storage vessels which commence construction, reconstruction, or modification after July 23, 1984. All storage vessels referenced in Table 4-2 commenced construction, reconstruction, or modification after July 23, 1984; therefore, NSPS Kb potentially applies to all storage vessels in Table 4-2.

Per 40 CFR 60.110b(a), and cited below, NSPS Kb only applies to storage vessels with a capacity greater than or equal to 19,813 gallons that is used to store volatile organic liquids (VOL).

Except as provided in paragraph (b) of this section, the affected facility to which this subpart applies is each storage vessel with a capacity greater than or equal to 75 cubic meters (m³) [19,813 gallons] that is used to store VOL for which construction, reconstruction, or modification is commenced after July 23, 1984.

Additionally, per 40 CFR 60.110b(b), and cited below, NSPS Kb does not apply to certain classifications of storage vessels determined by both storage capacity and maximum true vapor pressure (TVP).

This subpart does not apply to storage vessels with a capacity greater than or equal to 151 m³ [39,890 gallons] storing a liquid with a maximum true vapor pressure less than 3.5 kilopascals (kPa) [0.5 psia] or with a capacity greater than or equal to 75 m³ [19,813 gallons] but less than 151 m³ [39,890 gallons] storing a liquid with a maximum true vapor pressure less than 15.0 kPa [2.18 psia].

Capacity Less Than 19,813 Gallons

The miscellaneous chemical storage vessels, proposed to be permitted as an IA, all have a capacity less than 19,813 gallons; therefore, the provisions of NSPS Kb do not apply.

Capacity Greater Than 39,890 Gallons and Maximum TVP Less Than 0.5 psia

As observed from Table 4-2, the Carbon Capture Produced Water Storage Tanks have a capacity greater than 39,890 gallons and store a product with a maximum TVP less than 0.5 psia. Therefore, NSPS Kb does not apply to these storage vessels.

4.2.2.2. 40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced after September 18, 2015

The provisions of NSPS OOOOa are applicable to any storage vessel containing crude oil, condensate, intermediate hydrocarbon liquids, or produced water that has been constructed, reconstructed or modified after November 16, 2020, and has potential VOC emissions of equal to or greater than 6 TPY. All storage vessels identified in Table 4-2 have a potential VOC emission rate that is less than 6 TPY; therefore, the provisions of NSPS OOOOa do not apply.

4.2.3. Fugitive Emission Components

This section includes the regulatory applicability analysis associated with Fugitive Emissions (EPN: FUG; FUG 0001) for all potentially applicable NSPS.

4.2.3.1. 40 CFR 60 Subpart KKK - Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants for which Construction, Reconstruction, or Modification Commenced after January 20, 1984, and on or before August 3, 2011

The provisions of NSPS KKK are potentially applicable to the group of all "equipment" (i.e., fugitive emission components) located within a process unit and compressors located at natural gas processing plants which commenced construction, reconstruction, or modification after January 20, 1984, and on or before August 3, 2011. Per 40 CFR 60.630(e), because the Ajax Amine Plant is not a natural gas processing plant, the provisions of NSPS KKK do not apply.

4.2.3.2. 40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced after September 18, 2015

The provisions of NSPS OOOOa are potentially applicable to the group of all "equipment" (i.e., fugitive emission components) within a process unit located at an onshore natural gas processing plant, well site, or compressor station that commenced construction, modification, or reconstruction after September 18, 2015. The Ajax Amine Plant is classified as a compressor station; therefore, the provisions of NSPS OOOOa apply to all existing fugitive components. The Ajax Amine Plant will continue to comply with the provisions of NSPS OOOOa for all existing fugitive components and any new fugitive components associated with the Carbon Capture Project that have the potential to emit emissions of VOC.

4.3. NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS (NESHAP) - 40 CFR 61

The NESHAP standards were authorized under Section 112 of the CAA and were initially implemented as a risk-based standard, on a HAP-specific and activity basis. The Ajax Amine Plant does not engage in any of the HAP emitting activities defined by any underlying NESHAP. Further, no NESHAP will be triggered with the proposed construction and operation of the Carbon Capture Project; therefore, no further details regarding the applicability of an underlying NESHAP has been included in this application.

4.4. NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS FOR SOURCE CATEGORIES (MACT) - 40 CFR 63

The Environmental Protection Agency (EPA) shifted from the original conception of the NESHAP being developed on a risk-based approach to a technology-based approach with the development of the NESHAP promulgated with 40 CFR Part 63. The NESHAP promulgated with 40 CFR Part 63 are generally referred to as the Maximum Available Control Technology (MACT) standards and have been promulgated for specific source categories. The MACT rules, like the NESHAP codified under 40 CFR Part 61, define emission standards for HAP and are applicable to major and area sources of HAPs. A major source of HAP is defined as having potential emissions greater than 10 TPY for any individual HAP and 25 TPY for total HAPs. An area source is defined as a stationary source that is not a major source (i.e., emits less than 10 TPY of any individual HAP and less than 25 TPY for total HAPs). With the Carbon Capture Project, the Ajax Amine Plant will continue to emit less than 10 TPY of any single HAP and 25 TPY of total HAPs; therefore, the Ajax Amine Plant will continue to be considered an area source of HAP as observed in Section 6 and Appendix A.

Each emissions source affected by the Carbon Capture Project and its applicability with a MACT, considering the Ajax Amine Plant continues to be classified as an area source of HAP, can be found in Table 4-3, below. In the subsections that follow, a detailed MACT applicability analysis for each source can be found categorized by source

type.

Table 4-3. Emissions Unit MACT Summary

Source Type	TEMPO ID	Source ID	Description	HH	HHH	ZZZZ
Engine	EQT TBD	1-23	CAT G3608 Compressor Engine			X
Engine	EQT TBD	2-23	CAT G3608 Compressor Engine			X
Loading	EQT TBD	3-23	Sulfur Loading and Handling			
Dehydrator	EQT TBD	5-23B	CO ₂ Dehydrator Reboiler			
Tank	EQT TBD	6-23	Carbon Capture Produced Water Storage Tank			
Tank	EQT TBD	7-23	Carbon Capture Produced Water Storage Tank			
Loading	EQT TBD	8-23	Carbon Capture Produced Water Loading			
Fugitive	FUG 0001	FUG	Fugitive Emissions			
IA	N/A	IA-11	Carbon Capture Sump			
IA	N/A	IA-12	Surfactant (S200) Storage Tank			
IA	N/A	IA-13	TEG Storage Tank			

4.4.1. Engines

This section includes the regulatory applicability analysis for all potentially applicable MACT rules associated with the installation of the two reciprocating compressors, CAT G3608 Compressor Engine (EPN: 1-23; EQT TBD) and CAT G3608 Compressor Engine (EPN: 2-23; EQT TBD).

4.4.1.1. 40 CFR 63 Subpart HH - National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

The provisions of MACT HH apply to compressors in volatile HAP (VHAP) service located at a major source of HAP. The provisions of MACT HH do not apply to the two new proposed reciprocating compressors at the Ajax Amine Plant, since this site is an area source of HAP.

4.4.1.2. 40 CFR 63 Subpart ZZZZ - National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

The provisions of MACT ZZZZ are applicable to all stationary reciprocating internal combustion engines (RICE) located a major or area source of hazardous air pollutants (HAP). Further, the engines servicing the reciprocating compressors are classified as new, non-emergency, four stroke lean burn (4SLB), with a site rating of more than 500 HP, and are located at an area source of HAP. Therefore, per 40 CFR 63.6590(c)(1) the reciprocating compressors meet the provisions of MACT ZZZZ by meeting the provisions of NSPS JJJJ.

4.4.2. Dehydrators

This section includes the regulatory applicability analysis associated with the proposed CO₂ Dehydrator Unit for all potentially applicable MACT rules.

4.4.2.1. 40 CFR 63 Subpart HH - National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

The provisions of MACT HH apply to glycol dehydration units located at major and area sources of HAP. Per 40 CFR 63.761 a glycol dehydration unit is defined as follows:

means a device in which a liquid glycol (including, but not limited to, ethylene glycol, diethylene glycol, or triethylene glycol) absorbent directly contacts a natural gas stream and absorbs water in a contact tower or absorption column (absorber). The glycol contacts and absorbs water vapor and other gas stream constituents from the natural gas and becomes "rich" glycol. This glycol is then regenerated in the glycol dehydration unit reboiler. The "lean" glycol is then recycled.

While the CO₂ Dehydration Unit actively removes water from the process stream, the process stream does not qualify as natural gas, and further defined, per 40 CFR 63.761, as follows:

means a naturally occurring mixture of hydrocarbon and nonhydrocarbon gases found in geologic formations beneath the earth's surface. The principal hydrocarbon constituent is methane.

The process stream is primarily comprised CO₂ with only a minimal amount of methane being present. Therefore, the CO₂ Dehydration Unit is not subject to the provisions of MACT HH.

4.4.2.2. 40 CFR 63 Subpart HHH - National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities

The provisions of MACT HHH apply to glycol dehydration units found within the natural gas transmission and storage facilities located at major sources of HAP. The CO₂ Dehydration Unit is not subject to the provisions of MACT HHH as the Ajax Amine Plant is not considered a natural gas transmission or storage facility nor is it considered a major source of HAP.

4.4.3. Storage Vessels

This section includes the MACT regulatory applicability analysis associated with Produced Water Storage Tank (EPN: 6-23; EQT TBD) and Produced Water Tank (EPN: 7-23; EQT TBD).

4.4.3.1. 40 CFR 63 Subpart HH - National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

The provisions of MACT HH apply to storage vessels with the potential for flash emissions located at a major source of HAP. The provisions of MACT HH do not apply to the produced water storage tanks, as the Ajax Amine Plant is considered an area source of HAP.

4.4.4. Fugitive Emission Components

This section includes the regulatory applicability analysis associated with the Fugitive Emissions (EPN: FUG; FUG 0001) for all potentially applicable MACT rules.

4.4.4.1. 40 CFR 63 Subpart HH - National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

The provisions of MACT HH apply to all equipment (i.e., fugitive emission components) that are in VHAP service (≥ 10 weight percent VHAP) located at a natural gas processing plant that is a major source of HAP. The Ajax Amine Plant is not considered a natural gas processing plant nor is it considered a major source of HAP; therefore, the provisions of MACT HH do not apply.

4.5. COMPLIANCE ASSURANCE MONITORING

The Compliance Assurance Monitoring (CAM) rule applies to each pollutant-specific emission unit (PSEU) located at a major source that is required to obtain a Part 70 or 71 air permit. Applicability to the CAM rule is contingent on whether a unit is located at a major source, whether a unit is subject to an emission limitation or standard which is specified in a rule or regulation, whether a control device is used to achieve compliance with that limitation or standard, and whether potential uncontrolled emissions are equal to, or greater than, 100 percent of the major source threshold amount. The Major Source Threshold (MST) is defined as 100 TPY for each criteria pollutant, 10 TPY for any individual HAP, and 25 TPY for all combined HAPs.

Emission control devices subject to federally enforceable regulations promulgated after November 15, 1990, are exempt from additional regulation under the CAM rule as those rules already establish monitoring requirements to assure compliance. ETGP has previously conducted a comprehensive analysis associated with all existing PSEU and all newly proposed sources associated with the Carbon Capture Project referenced in this application and have determined that no CAM applicability will apply.

4.6. LOUISIANA STATE AIR QUALITY REGULATIONS

Each emissions source affected by the Carbon Capture Project and its applicability with the Louisiana State Air Quality regulations can be found in Table 4-4, below. In the subsections that follow, a detailed Louisiana State Air Quality regulation applicability analysis for each source can be found categorized by source type.

Table 4-4. Emissions Unit LAC Summary

Source Type	TEMPO ID	Source ID	Description	2103	2107	2111	2115	2116	2121	Ch. 11	Ch. 13	Ch. 15	Ch. 51
Engine	EQT TBD	1-23	CAT G3608 Compressor Engine								X		
Engine	EQT TBD	2-23	CAT G3608 Compressor Engine								X		
Loading	EQT TBD	3-23	Sulfur Loading and Handling								X		
Dehydrator	EQT TBD	5-23B	CO ₂ Dehydrator Reboiler								X		
Tank	EQT TBD	6-23	Carbon Capture Produced Water Storage Tank										
Tank	EQT TBD	7-23	Carbon Capture Produced Water Storage Tank										

Source Type	TEMPO ID	Source ID	Description	2103	2107	2111	2115	2116	2121	Ch. 11	Ch. 13	Ch. 15	Ch. 51
Loading	EQT TBD	8-23	Carbon Capture Produced Water Loading										
Fugitive	FUG 0001	FUG	Fugitive Emissions			X							
IA	N/A	IA-11	Carbon Capture Sump										
IA	N/A	IA-12	Surfactant (S200) Storage Tank										
IA	N/A	IA-13	TEG Storage Tank										

4.6.1. Engines

This section includes the regulatory applicability analysis for all potentially applicable Louisiana State Air Quality regulations associated with the installation of the two reciprocating compressors, CAT G3608 Compressor Engine (EPN: 1-23; EQT TBD) and CAT G3608 Compressor Engine (EPN: 2-23; EQT TBD).

4.6.1.1. LAC 33:III Chapter 11 - Control of Emissions of Smoke

LAC 33:III Chapter 11 establishes emission standards on smoke, with LAC 33:III.1101.B specifically establishing emission standards of smoke from fuel combustion equipment. LAC 33:III.1101.B requires that the combustion unit shall be controlled so that the shade or appearance of the emissions is not darker than 20 percent average opacity, except that such emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.

However, per LAC 33:III.1107.B.1, combustion units utilizing either natural gas and/or other gaseous fuels with a carbon to hydrogen molecular ratio of less than 0.34 are exempted from the provisions of LAC 33:III.1101.B. The reciprocating compressors will utilize natural gas; therefore, they are exempted from the provisions of LAC 33:III.1101.B.

4.6.1.2. LAC 33:III Chapter 13 - Emission Standards for Particulate Matter

The provisions of LAC 33:III Chapter 13 apply to fuel burning equipment with the intent to limit emissions of PM. LAC 33:III.1313.C requires that fuel burning equipment emit less than 0.6 pounds of PM per MMBTU. The reciprocating compressors are considered "fuel burning equipment"; therefore, the standards of LAC 33:III.1313.C apply.

4.6.1.3. LAC 33:III Chapter 15 - Emission Standards for Sulfur Dioxide

The provisions of LAC 33:III Chapter 15 apply to all single point sources, other than sulfuric acid plants or sulfur recovery plants (SRP), that emit or have the potential to emit 250 TPY or more of SO₂ into the atmosphere. LAC 33:III.1503.C limits concentration of SO₂ to less than 2,000 ppmv, on a 3-hour rolling average, at standard conditions, or any applicable NSPS or MACT limitation whichever is more stringent. The reciprocating compressors do not have the potential to emit in excess of 250 TPY of SO₂; therefore, the standards associated with LAC 33:III.1503.C do not apply.

4.6.2. Sulfur Loading and Handling

This section includes the regulatory applicability analysis associated with Sulfur Loading and Handling (EPN: 3-23; EQT TBD).

4.6.2.1. LAC 33:III Chapter 13 - Emission Standards for Particulate Matter

The provisions of LAC 33:III Chapter 13 apply to any operation, process, or activity from which particulate matter is emitted except for the wood pulping industry, aluminum industry, and processes involved in burning of fuel for indirect heating. The Ajax Amine Plant is not associated with the wood pulping or aluminum industry and the Sulfur Loading and Handling source is not engaged in the combustion of a fuel; therefore, the provisions of LAC 33:III Chapter 13 will apply. Specifically, the Sulfur Loading and Handling source will be subject to LAC 33:III.1311.C, limiting the source from exceeding 20 percent opacity, except for one six-minute period in any sixty consecutive minutes.

4.6.3. Glycol Dehydrators (CO₂ Dehydrator Unit Vents)

This section includes the Louisiana State Air Quality regulatory applicability analysis associated with the CO₂ Dehydrator Unit.

4.6.3.1. LAC 33:III.2116 - Glycol Dehydrators

The provisions of LAC 33:III.2116 apply to a glycol dehydrator that is not required to install controls according to LAC 33:III Chapter 51 or LAC 33:III.2115. The CO₂ Dehydration Unit is being proposed to remove moisture from a process stream that is primarily comprised of CO₂ with only trace quantities of VOC. While the LAC does not define the term *glycol dehydrator*, ETGP understands this term to be consistent with *glycol dehydration unit* as defined via MACT HH. The CO₂ Dehydration Unit is not defined as a *glycol dehydration unit* as previously referenced in Section 4.4.2.1; therefore, ETGP proposes that the provisions of LAC 33:III.2116 do not apply to the CO₂ Dehydration Unit.

4.6.4. Heaters (CO₂ Dehydrator Reboiler)

This section includes the Louisiana State Air Quality regulatory applicability analysis associated with the CO₂ Dehydrator Reboiler (EPN: 5-23B; EQT TBD).

4.6.4.1. LAC 33:III Chapter 11 - Control of Emissions of Smoke

LAC 33:III Chapter 11 establishes emission standards on smoke, with LAC 33:III.1101.B specifically establishing emission standards of smoke from fuel combustion equipment. LAC 33:III.1101.B requires that the combustion unit shall be controlled so that the shade or appearance of the emissions is not darker than 20 percent average opacity, except that such emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.

However, per LAC 33:III.1107.B.1, combustion units utilizing either natural gas and/or other gaseous fuels with a carbon to hydrogen molecular ratio of less than 0.34 are exempted from the provisions of LAC 33:III.1101.B. The CO₂ Dehydrator Reboiler will utilize natural gas; therefore, it is exempted from the provisions of LAC 33:III.1101.B.

4.6.4.2. LAC 33:III Chapter 13 - Emission Standards for Particulate Matter

The provisions of LAC 33:III Chapter 13 apply to fuel burning equipment with the intent to limit emissions of PM. LAC 33:III.1313.C requires that fuel burning equipment emit less than 0.6 pounds of PM per MMBTU. The CO₂ Dehydrator Reboiler is considered "fuel burning equipment"; therefore, the standards of LAC 33:III.1313.C apply.

4.6.4.3. LAC 33:III Chapter 15 - Emission Standards for Sulfur Dioxide

The provisions of LAC 33:III Chapter 15 apply to all single point sources, other than sulfuric acid plants or sulfur recovery plants (SRP), that emit or have the potential to emit 250 TPY or more of SO₂ into the atmosphere. LAC 33:III.1503.C limits concentration of SO₂ to less than 2,000 ppmv, on a 3-hour rolling average, at standard conditions, or any applicable NSPS or MACT limitation whichever is more stringent. The CO₂ Dehydrator Reboiler does not have the potential to emit in excess of 250 TPY of SO₂; therefore, the standards associated with LAC 33:III.1503.C do not apply.

4.6.5. Storage Vessels

This section includes the regulatory applicability analysis associated with the following storage vessels, found in Table 4-5, for all potentially applicable Louisiana State Air Quality regulations.

Table 4-5. Project Affected Storage Vessel Characteristics

TEMPO ID	Source ID	Description	Product	Construction Year ¹	Capacity (MMGal)	Max True Vapor Pressure (psia)
EQT TBD	6-23	Carbon Capture Produced Water Storage Tank	Produced Water	Proposed 2024	31,500	0.50
EQT TBD	7-23	Carbon Capture Produced Water Storage Tank	Produced Water	Proposed 2024	31,500	0.50
IA	N/A	Carbon Capture Sump	Produced Water	Proposed 2024	1,000	0.50
IA	N/A	Surfactant (S200) Storage Tank	Surfactant	Proposed 2024	500	0.02
IA	N/A	TEG Storage Tank	TEG	Proposed 2024	330	<0.01

1: Year referenced represents the latest year of construction, reconstruction, or modification.

4.6.5.1. LAC 33:III.2103 - Control of Emission of Organic Compounds - Storage of Volatile Organic Compounds

LAC 33:III.2103 requires that any storage vessel with a capacity of more than 250 gallons and less than 40,000 gallons storing a VOC having a maximum TVP of 1.5 psia or greater at storage conditions be equipped with a submerged fill pipe or vapor control system, except for pressure tanks capable of preventing emissions from venting to the atmosphere. Additionally, storage vessels of more than 40,000 gallons storing a VOC having a maximum TVP of 1.5 psia or greater at storage conditions be equipped with a submerged fill pipe and a vapor loss control device as defined in LAC 33:III.2103.C-E. No storage vessel, referenced in Table 4-5, has a maximum TVP in excess of 1.5 psia; therefore, the provisions of LAC 33:III.2103 do not apply.

4.6.6. Loading

This section includes the Louisiana State Air Quality regulatory applicability analysis associated with Carbon Capture Produced Water Loading (EPN: 8-23; EQT TBD).

4.6.6.1. LAC 33:III.2107 - Control of Emission of Organic Compounds - Volatile Organic Compounds - Loading

The provisions of LAC 33:III.2107 apply to loading facilities, servicing tanks, trucks, or trailers which have individual capacities of greater than 200 gallons and products having a TVP of 1.5 psia or greater during loading conditions. The loading sources represented in Table 4-3 do not service tanks, trucks, or trailers nor load products having a TVP in excess of 1.5 psia; therefore, the provisions of LAC 33:III.2107 do not apply.

4.6.7. Fugitive Emission Components

This section includes the regulatory applicability analysis associated with Fugitive Emissions (EPN: FUG; FUG 0001) for all potentially applicable Louisiana State Air Quality regulations.

4.6.7.1. LAC 33:III.2111 - Control of Emission of Organic Compounds (VOCs) - Pumps and Compressors

All rotary pumps and compressors handling VOCs having a TVP of 1.5 psia or greater at handling conditions are required to be equipped with mechanical seals or other equivalent equipment. ETGP operates various pumps and compressors throughout the facility that handle VOCs with a TVP of 1.5 psia or greater; therefore, these pumps and compressors are subject to the provisions of LAC 33:III.2111.

4.6.7.2. LAC 33:III.2121 - Control of Emission of Organic Compounds - Fugitive Emission Control

The provisions of LAC 33:III.2121 are applicable to each process unit at a natural gas processing facility that contains fugitive emission components that operate in VOC service for 300 hours or more during the calendar year. The provisions of LAC 33:III.2121 do not apply since the Ajax Amine Plant is not considered a natural gas processing facility.

4.7. LAC 33:III CHAPTER 51 - COMPREHENSIVE TOXIC AIR POLLUTANT EMISSION CONTROL PROGRAM

4.7.1. Louisiana MACT Applicability

The provisions of LAC 33:III Chapter 51 (LA MACT) apply to all major sources of LTAP, that is defined as any stationary source that has the potential to emit 10 TPY or more of any singular LTAP or 25 TPY or more of all aggregate LTAP, other than those sources of emissions that are exempted, per LAC 33:III.5105.B. The Ajax Amine Plant emits H₂S, a Class III LTAP, in excess of 10 TPY from sources that are not exempted, per LAC 33:III.5105.B; therefore, the Ajax Amine Plant is subject to the provisions of LAC 33:III Chapter 51. With the triggering of LA MACT, the Ajax Amine Plant will specifically be required to meet the following requirements:

- Reporting provisions of LAC 33:III.5107.A;
- The Emission Control and Reduction Requirements and Standards of LAC 33:III.5109; and,
- The air toxics permit application fee and air toxics annual emissions fee, per LAC 33:III Chapter 2.

4.7.2. LA MACT Reporting Requirements

The reporting requirements of LA MACT obligates the Ajax Amine Plant to report all LTAP listed in LAC 33:III.5112.A, Table 51.1 and Table 51.3 with the annual emissions inventory. Further, the Ajax Amine Plant is required to meet the discharge reporting requirements as defined in LAC 33:III.5107.B.

4.7.3. Emission Control and Reduction Requirements and Standards

The requirements of LAC 33:III.5109 consists of three main compliance requirements that includes:

- LA MACT Requirements;
- Ambient Air Standard (AAS) Requirements; and,
- Standard Operating Procedure (SOP) Requirements.

The subsections that follow detail the compliance of each three main compliance requirement as previously referenced.

4.7.3.1. LA MACT Requirements

The LA MACT requirements of LAC 33:III.5109.A apply to each Class I or Class II LTAP where the facility-wide emission rate exceeds the pollutant's respective Minimum Emission Rate (MER) as defined in Table 51.1. The requirements of LAC 33:III.5109.A apply to each emission source not other exempted in LAC 33:III.5105, which includes LTAP emissions generated via the combustion of Group 1 virgin fossil fuel (e.g., natural gas) and those emission sources subject to a federal MACT.

In review of the facility-wide emission rate for each Class I and Class II LTAP, ETGP has found that no pollutants exceed the listed MER.

4.7.3.2. AAS Requirements

Per LAC 33:III.5109.B, the AAS requirements apply to any Class I, Class II, or Class III LTAP that exceeds the pollutant's respective MER. ETGP conducted a thorough review of the facility-wide emission rate for each LTAP and found that H₂S, a Class III LTAP, exceeds its respective MER; therefore, the site is required to meet the AAS, as defined by Table 51.2. Based upon the magnitude of emissions associated with H₂S, it is assumed that the Ajax Amine Plant remains in compliance with the AAS for H₂S.

4.7.3.3. SOP Requirements

Per LAC 33:III.5109.C, the SOP requirements apply to any Class I, or Class III LTAP that exceeds the pollutant's, respective MER. As previously referenced, both H₂S and benzene exceed the pollutant's respective MER on a facility-wide basis; therefore, a SOP is required to be developed within 120 days of achieving compliance with the provisions of LA MACT. The SOP is required to detail all operating procedures or parameters established by ETGP to ensure that continued compliance is achieved with each of the aforementioned pollutants. The SOP is further required to be maintained onsite and available to be provided to LDEQ within 30 days upon request.

4.7.4. Air Toxics Fees

Per LAC 33:III.5101.D.1.c, ETGP is required to comply with the air permit application and air toxics annual emissions fees as identified in LAC 33:III Chapter 2. As observed in Section 6 and Appendix B, ETGP has included

the required air toxics fee in order to process this application. Further, ETGP will comply with the applicable air toxics annual emissions fee as a part of the annual emissions inventory.

5. SUMMARY OF PERMIT RECONCILIATIONS

5.1. RECONCILIATION BACKGROUND

In addition to authorizing the construction and operation of the proposed Carbon Capture Project, ETGP is requesting the following permit revisions.

5.2. PERMIT REVISION SUMMARY

5.2.1. SO₂ Calculation Methodology

Currently, the permitted natural gas combustion sources utilize emission factors from AP-42, Chapter 1.4 (e.g. 0.6 lb/MMscf). With this revision, ETGP proposes to revise the maximum hourly SO₂ basis utilizing 30 parts per million by volume (ppmv) sulfur content of the natural gas fuel for the sources identified in Table 5-1.

Table 5-1. Maximum Hourly SO₂ Revision

TEMPO ID	Source ID	Description
EQT 0002	1-22B	Plant 1 Amine Unit Hot Oil Heater
EQT 0004	2-22B	Plant 1 Glycol Dehydrator Reboiler
EQT 0006	3-22B	Plant 2 Amine Unit Hot Oil Heater
EQT 0008	4-22B	Plant 2 Glycol Dehydrator Reboiler
EQT 0009	5-22	Plant 1 Thermal Oxidizer
EQT 0010	6-22	Plant 2 Thermal Oxidizer
EQT 0011	7-22	CAT G3606 Compressor Engine
EQT 0012	8-22	CAT G3606 Compressor Engine
EQT 0013	9-22	CAT G3606 Compressor Engine
EQT 0014	10-22	CAT G3606 Compressor Engine
EQT 0023	19-22	Flare

For a revised EIQ and detailed calculation backup for each source identified in Table 5-1, refer to Section 6 and Appendix A, respectively.

5.2.2. Revision to Uncontrolled Vents

The Ajax Amine Plant operates multiple vents that are currently routed to thermal oxidation control during routine operations that include the following:

- Plant 1 Amine Unit Vent (EPN: 1-22A; EQT 0001);
- Plant 1 Glycol Dehy Unit Vent (EPN: 2-22A; EQT 0003);
- Plant 2 Amine Unit Vent (EPN: 3-22A; EQT 0005); and,
- Plant 2 Glycol Dehy Unit Vent (EPN: 4-22A; EQT 0007).

These vents are currently permitted to be vented to the atmosphere, for 720 hours per year (hr/yr), during thermal oxidizer downtime. Upon startup of the Carbon Capture Project, these vents will be routed to the front end of the Carbon Capture skid for further processing. In the event that the Carbon Capture skid is shutdown, there will be a period of time which the aforementioned vents will be routed to the atmosphere until the vents can be directed to the thermal oxidizer for control. Therefore, ETGP proposes to increase the number of hours that the vents can be routed to the atmosphere from 720 hr/yr to 1,200 hr/yr. A summary of the emission rate changes can be found in Table 5-2, with revised EIQ and detailed calculation backup for each source identified in Table 5-2, found in Section 6 and Appendix A, respectively.

Table 5-2. Emission Rate Changes to Uncontrolled Vents

Source	Pollutant	Current (TPY)	Proposed (TPY)	Delta (TPY)
Plant 1 Amine Unit Vent (EPN: 1-22A; EQT 0001)	VOC	0.01	0.02	+ 0.01
	H ₂ S	5.05	8.42	+ 3.37
	n-Hexane	<0.01	<0.01	-
Plant 1 Glycol Dehy Unit Vent (EPN: 2-22A; EQT 0003)	VOC	0.05	0.08	+ 0.03
	H ₂ S	-	-	-
	n-Hexane	0.03	0.06	+ 0.03
Plant 2 Amine Unit Vent (EPN: 3-22A; EQT 0005)	VOC	0.01	0.02	+ 0.01
	H ₂ S	5.05	8.42	+ 3.37
	n-Hexane	<0.01	<0.01	-
Plant 2 Glycol Dehy Unit Vent (EPN: 4-22A; EQT 0007)	VOC	0.05	0.08	+ 0.03
	H ₂ S	-	-	-
	n-Hexane	0.03	0.06	+ 0.03

5.2.3. Applicable Regulations and Specific Requirements Updates


5.2.3.1. Removal of Skid Drain Storage Tank from CRG 0004

The Skid Drain Storage Tank (EPN: 18-22; EQT 0022) has a vapor pressure less than 1.5 psia; therefore, is not subject to LAC 33:III.2103 and is proposed to be removed from CRG 0004. Refer to Section 6 for the requested changes to CRG 0004.

5.2.3.2. Modification to Specific Requirement 48

ETGP proposes to modify Specific Requirement (SR) 48 as portions of the SR have either been duplicated and can be found already included with the discreet source or references sources that do not exist at the facility. For specific details associated with the proposed modification of SR 48, refer to Section 6

**6. APPLICATION FOR APPROVAL OF EMISSIONS OF AIR POLLUTANTS FROM
PART 70 SOURCES (AAEAP)**

Department of Environmental Quality Office of Environmental Services Air Permits Division P.O. Box 4313 Baton Rouge, LA 70821-4313 (225) 219-3417	<h1 style="margin: 0;">LOUISIANA</h1> <h2 style="margin: 0;">Application for Approval of Emissions of Air Pollutants from Part 70 Sources</h2>	
--	--	---

PLEASE TYPE OR PRINT

1. Facility Information [LAC 33:III.517.D.1]

Facility Name or Process Unit Name (if any) Ajax Amine Plant		<input checked="" type="checkbox"/> All Process Units <input type="checkbox"/> Process Unit-specific Permit
Agency Interest Number (A.I. Number) 237065	Currently Effective Permit Number(s) 0760-01944-V0	
Company - Name of Owner ET Gathering & Processing LLC		
Company - Name of Operator (if different from Owner)		
Parent Company (if Company – Name of Owner given above is a division) Energy Transfer LP		
Federal Tax-ID 93-3058573		

- corporation, partnership, or sole proprietorship
 regulated utility
 municipal government
 state government
 federal government
 other, specify _____

**2. Physical Location and Process Description
[LAC 33:III.517.D.18, unless otherwise stated]**

What does this facility produce? Add more rows as necessary.

The Ajax Amine Plant is a natural gas amine treating and dehydration station.

What modifications/changes are proposed in this application? Add more rows as necessary.

Enable is submitting this minor modification application for the implementation of the Carbon Capture Project that will remove carbon dioxide (CO₂) from the inlet gas and produce a highly concentrated CO₂ stream for export.

Nearest town (in the same parish as the facility):	Parish(es) where facility is located:			
Pelican	DeSoto			
Distance To (mi):	<u>25</u> Texas	<u>80</u> Arkansas	<u>124</u> Mississippi	<u>294</u> Alabama
Latitude of Facility Front Gate:	<u>31</u> Deg	<u>51</u> Min	<u>10</u> Sec	<u>64</u> Hundredths
Longitude of Facility Front Gate:	<u>93</u> Deg	<u>26</u> Min	<u>57</u> Sec	<u>49</u> Hundredths
Distance from nearest Class I Area:	<u>496</u> kilometers			

Add physical address and description of location of the facility below. If the facility has no address, provide driving directions. Add more rows as necessary.

From Pleasant Hill, Louisiana drive east on Highway 714 for 4 miles until you reach Bowden Rd. Continue on Highway 174 for an additional 0.9 miles and the site is on the right.

- Map attached (required per LAC 33:III.517.D.1)
 Description of processes and products attached (required per LAC 33:III.517.D.2)
 Introduction/Description of the proposed project attached (required per LAC 33:III.517.D.5)

3. Confidentiality [LAC 33.I.Chapter 5]

Are you requesting confidentiality for any information except air pollutant emission rates? Yes No

If "yes," list the sections for which confidentiality is requested below. Add rows as necessary. Confidentiality requests require a submittal that is separate from this application. Information for which confidentiality is requested should not be submitted with this application. Consult instructions.

4. Type of Application [LAC 33:III.517.D]

Check all that apply.

<input type="checkbox"/> Renewal
Select one, if applicable:
<input type="checkbox"/> Entirely new facility
<input type="checkbox"/> Significant modification of existing facility (may also include reconciliations) [LAC 33:III.527]
<input checked="" type="checkbox"/> Minor modification of existing facility (may also include reconciliations) [LAC 33:III.525]
<input type="checkbox"/> Reconciliation only
NSR Analysis:
<input type="checkbox"/> Prevention of Significant Deterioration (PSD)
<input type="checkbox"/> Nonattainment New Source Review (NNSR)

Does this submittal update or replace an application currently under review? Yes No

If yes, provide date that the prior application was submitted: _____

Select one if this application is for an existing facility that does not have an air quality permit:

- Previously Grandfathered (LAC 33:III.501.B.6)
- Previously Exempted (e.g., Small Source Exemption; LAC 33:III.501.B.2.d)
- Previously Unpermitted

5. Fee Information [LAC 33:III.517.D.17]

Fee Parameter: If the fee code is based on an operational parameter (such as number of employees or capital cost), enter that parameter here. _____

Industrial Category: Enter the Standard Industrial Classification (SIC) and North American Industry Classification (NAICS) Codes that apply to the facility.

Primary SICC: 1389 **NAICS Code:** _____

Secondary SICC(s): _____

Project Fee Calculation: Enter fee code, permit type, production capacity/throughput, and fee amount pursuant to LAC 33:III.Chapter 2. Add rows to this table as needed. Include with the application the amount in the Grand Total blank as the permit application fee.

FEE CODE	TYPE	EXISTING CAPACITY	INCREMENTAL CAPACITY INCREASE	SURCHARGES				TOTAL AMOUNT
				MULTIPLIER	NSPS	PSD	AIR TOXICS	
1712	Minor		N/A	N/A	<input checked="" type="checkbox"/>	<input type="checkbox"/>	<input checked="" type="checkbox"/>	\$1,960.20
					<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>	\$
GRAND TOTAL								\$1,960.20

****Optional** Fee Explanation:** Use the space provided to give an explanation of the fee determination displayed above. Using this area will help to avoid confusion. See Appendix B for a detailed explanation of the Project Fee Calculation.

Electronic Fund Transfer (EFT): If paying the permit application fee using an Electronic Fund Transfer (EFT), please include the EFT Transaction Number, the Date that the EFT was made, and the total dollar amount submitted in the EFT. If not paying the permit application fee using EFT, leave blank.

EFT Transaction Number	Date of Submittal	Total Dollar Amount
N/A	N/A	\$N/A

6. Key Dates

Estimated date construction will commence: 2Q 2025 Estimated date operation will commence: 4Q 2026

7. Pending Permit Applications – For Process Unit-Specific Permits Only

[LAC 33:III.517.D.18]

List all other process units at this facility for which Part 70 permit applications have been submitted but have not been acted upon by LDEQ as of the date of submittal of this application. If none, state “none” in the table. ****It is not necessary to update this table during the permit review process, unless requested by LDEQ.****

Process Unit Name	Permit Number	Date Submitted

8. LAC 33:I.1701 Requirements – Answer all below for new sources and permit renewals - Yes No

Does the company or owner have federal or state environmental permits identical to, or of a similar nature to, the permit for which you are applying in Louisiana or other states? (This requirement applies to all individuals, partnerships, corporations, or other entities who own a controlling interest of 50% or more in your company, or who participate in the environmental management of the facility for an entity applying for the permit or an ownership interest in the permit.)

Yes No

If yes, list States: _____

Do you owe any outstanding fees or final penalties to the Department? Yes No

If yes, explain below. Add rows if necessary.

Is your company a corporation or limited liability company? Yes No

If yes, attach a copy of your company’s Certificate of Registration and/or Certificate of Good Standing from the Secretary of State. The appropriate certificate(s) should be attached to the end of this application as an appendix.

9. Permit Shield Request [LAC 33:III.517.E.7] - Yes No

If yes, check the appropriate boxes to indicate the type of permit shield being sought. Include the specific regulatory citation(s) for which the shield is being requested. Give an explanation of the circumstances that will justify the permit shield request. Attach additional pages if necessary. If additional pages are used, attach them directly behind this page and enter "See Attached Pages" into the Explanation field.

Type of Permit Shield request (check all that apply):

Non-applicability determination for:	Specific Citation(s)	Explanation
<input type="checkbox"/> 40 CFR 60		
<input type="checkbox"/> 40 CFR 61		
<input type="checkbox"/> 40 CFR 63		
<input type="checkbox"/> Prevention of Significant Deterioration		
<input type="checkbox"/> Nonattainment New Source Review		

Interpretation of monitoring, recordkeeping, and/or reporting requirements, and/or means of compliance for:	Specific Citation(s)	Explanation
<input type="checkbox"/> 40 CFR 60		
<input type="checkbox"/> 40 CFR 61		
<input type="checkbox"/> 40 CFR 63		
<input type="checkbox"/> Prevention of Significant Deterioration		
<input type="checkbox"/> Nonattainment New Source Review		
<input type="checkbox"/> State Implementation Plan (SIP) Regulation(s) referenced in 40 CFR 52 Subpart T		

10. Certification of Compliance With Applicable Requirements

Statement for Applicable Requirements for Which the Company and Facility Referenced In This Application Is In Compliance

Based on information and belief, formed after reasonable inquiry, the company and facility referenced in this application is in compliance with and will continue to comply with all applicable requirements pertaining to the sources covered by the permit application, as outlined in Tables 1 and 2 in the permit application. For requirements promulgated as of the date of this certification with compliance dates effective during the permit term, I further certify that the company and facility referenced in this application will comply with such requirements on a timely basis and will continue to comply with such requirements.


For corporations only: By signing this form, I certify that, in accordance with the definition of Responsible Official found in LAC 33:III.502, **(1)** I am a president, secretary, treasurer, or vice-president in charge of a principal business function, or other person who performs similar policy or decision-making functions; or **(2)** I am a duly authorized representative of such person; am responsible for the overall operation of one or more manufacturing, production, or operating facilities addressed in this permit application; and either the facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or the delegation of authority has been approved by LDEQ prior to this certification.*


CERTIFICATION: I certify, under provisions in Louisiana and United States law which provide criminal penalties for false statements, that based on information and belief formed after reasonable inquiry, the statements and information contained in this Application for Approval of Emissions of Air Pollutants from Part 70 Sources, including all attachments thereto and the compliance statement above, are true, accurate, and complete.

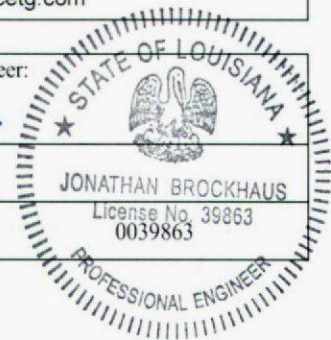
CERTIFICATION: I certify that the engineering calculations, drawings, and design are true and accurate to the best of my knowledge.

a. Responsible Official		
Name Joe Perez		
Title VP of Operations		
Company Energy Transfer LP		
Suite, mail drop, or division		
Street or P.O. Box 4550 Marlana Street		
City Bossier City	State LA	Zip 71111
Business phone (713) 989-7030		
Email Address Joe.Perez3@energytransfer.com		

b. Professional Engineer		
Name Jonathan D. Brockhaus		
Title Managing Director		
Company Alliance Technical Group		
Suite, mail drop, or division Suite 2050		
Street or P.O. Box 450 Laurel Street		
City Baton Rouge	State LA	Zip 70801
Business phone (281) 628-7851		
Email Address Jonathan.Brockhaus@alliancetg.com		

Signature of responsible official (See 40 CFR 70.2): 	
Date:	11/17/2024

Signature of Professional Engineer: 	
Date:	11/17/24



*Approval of a delegation of authority can be requested by completing a Duly Authorized Representative Designation Form (Form 7218) available on LDEQ's website at <http://deq.louisiana.gov/page/air-permit-applications>

11. Personnel [LAC 33:III.517.D.1]

a. Manager of Facility who is located at plant site		
Name John Woodard	<input type="checkbox"/> Primary contact	
Title Manager - Operations		
Company Energy Transfer LP		
Suite, mail drop, or division		
Street or P.O. Box 106 Old Highway 6		
City Natchitoches	State LA	Zip 71457
Business phone (318) 357-3614		
Email address John.Woodard@energytransfer.com		

b. On-site contact regarding air pollution control		
Name Anna Bufkin	<input type="checkbox"/> Primary contact	
Title Environmental Specialist		
Company Energy Transfer LP		
Suite, mail drop, or division		
Street or P.O. Box 4550 Marlena St.		
City Bossier City	State LA	Zip 71111
Business phone (318) 698-6509		
Email address Anna.Bufkin@energytransfer.com		

c. Person to contact with written correspondence		
Name Hanh Duong	<input checked="" type="checkbox"/> Primary contact	
Title Staff Engineer		
Company Energy Transfer LP		
Suite, mail drop, or division		
Street or P.O. Box 1300 Main Street		
City Houston	State TX	Zip 77002
Business phone (713) 989-7158		
Email address Hanh.Duong@energytransfer.com		

d. Person who prepared this report		
Name Eric Rucinski	<input type="checkbox"/> Primary contact	
Title Senior Project Manager		
Company Alliance Technical Group		
Suite, mail drop, or division Suite 2050		
Street or P.O. Box 450 Laurel Street		
City Baton Rouge	State LA	Zip 70801
Business phone (225) 400-3861		
Email address Eric.Rucinski@alliancetg.com		

e. Person to contact about Annual Maintenance Fees		<input type="checkbox"/> a <input type="checkbox"/> b <input checked="" type="checkbox"/> c <input type="checkbox"/> d <input type="checkbox"/> other (specify below)	
Name	<input type="checkbox"/> Primary contact	Suite, mail drop, or division	
Title		Street or P.O. Box	
Company		City	State Zip
Business Phone		Email Address	

12. Proposed Project Emissions [LAC 33:III.517.D.3]

List the total emissions following the proposed project for this facility or process unit (for process unit-specific permits). Speciate all criteria pollutants, TAP, and HAP for the proposed project.

Pollutant	Proposed Emission Rate (tons/yr)
Carbon Monoxide	108.02
Nitrogen Oxides	120.68
Particulate matter (PM10)	12.21
Particulate matter (PM2.5)	12.21
Sulfur Dioxide	233.99
Total VOC (including those listed below)	30.79
Acetaldehyde	1.73
Acrolein	1.065
Barium (and compounds)	<0.001
Benzene	0.16
Biphenyl	0.04
1,3-Butadiene	0.055
Carbon Tetrachloride	0.01
Chlorobenzene	0.006
Chloroform	0.01
Chromium VI (and compounds)	<0.001
1,4-Dichlorobenzene	<0.001
1,1-Dichloroethane	<0.01
1,2-Dichloroethane	0.002
1,2-Dichloropropane	<0.01
1,3-Dichloropropene	0.01
Ethyl benzene	0.07
Ethylene Dibromide	0.009
Formaldehyde	5.37
Hydrogen sulfide	19.29
Methanol	0.52
Methylene Chloride	<0.01
n-Hexane	2.28
Naphthalene (and Methyl-naphthalenes)	0.02
Nickel (and compounds)	<0.001
Phenol	<0.01
Polynuclear Aromatic Hydrocarbons	<0.001
Styrene	<0.01
Toluene	0.16
1,1,2,2-Tetrachloroethane	0.01
1,1,2-Trichloroethane	0.01
2,2,4-Trimethylpentane	0.05
Xylene (mixed isomers)	0.11
Vinyl Chloride	<0.01
Zinc (and compounds)	<0.001

13. History of Permitted Emissions [LAC 33:III.517.D.18]

List each of the following in chronological order:

- The Permit Number and Date Action Issued for each air quality permit that has been issued to this facility or process unit (for process unit-specific permits) within the last ten (10) years.
- All small source exemptions, authorizations to construct, administrative amendments, case-by-case insignificant activities, and changes of tank service that have been approved since the currently effective Title V Operating Permit or State Operating Permit was issued to this facility or process unit (for process unit-specific permits). It is not necessary to list any such activities issued prior to the issuance of the currently effective Title V Operating Permit or State Operating Permit if one exists.

Permit Number	Date Action Issued
0760-01944-V0	07/18/2023

14.a. Enforcement Actions [LAC 33:III.517.D.18] - Yes No

If yes, list all federal and state air quality enforcement actions, settlement agreements, and consent decrees received for this facility and/or process unit (for process unit-specific permits) since the issuance of the currently effective Title V Operating Permit or State Operating Permit. For each action, list the type of action (or its tracking number), the regulatory authority or authorities that issued the action, and the date that the action was issued. Summarize the conditions imposed by the enforcement action, settlement agreement, and consent decree in Section 22, Table 2. It is not necessary to submit a copy of the referenced action. Add rows to table as necessary.

Type of Action or Tracking Number	Issuing Authority	Date Action Issued	Summary of Conditions Included?
			<input type="checkbox"/> Yes <input type="checkbox"/> No
			<input type="checkbox"/> Yes <input type="checkbox"/> No

14.b. Schedule for Compliance [LAC 33:III.517.E.4] Yes No

If the facility or process unit for which application is being made is not in full compliance with all applicable regulations, give a description of how compliance will be achieved, including a schedule for compliance below. Add rows as necessary. See instructions.

15. Letters of Approval for Alternate Methods of Compliance - Yes No

If yes, list all correspondence with LDEQ, EPA, or other regulatory bodies that provides for or supports a request for alternate methods of compliance with any applicable regulations for this facility or process unit (for process unit-specific permits). List the date of issuance of the letter and the regulation referenced by the letter. **Attach as an appendix a copy of all documents referenced in this table.** Letters that are not included may not be incorporated into a final permit. Add rows to table as necessary.

Date Letter Issued	Issuing Authority	Referenced Regulation(s)	Copy of Letter Attached?
			<input type="checkbox"/> Yes <input type="checkbox"/> No
			<input type="checkbox"/> Yes <input type="checkbox"/> No
			<input type="checkbox"/> Yes <input type="checkbox"/> No
			<input type="checkbox"/> Yes <input type="checkbox"/> No

16. Initial Notifications and Performance Tests [LAC 33:III.517.D.18] - Yes No

If yes, list any initial notifications that have been submitted or one-time performance tests that have been performed for this facility or process unit (for process unit-specific permits) since the issuance of the currently effective Title V Operating Permit or State Operating Permit in order to satisfy regulatory requirements. Any initial notification or one-time performance test requirements that have not been satisfied should be listed in Section 22, Table 2 of this application. Any notifications or performance tests that recur periodically should also be properly noted in Section 22, Table 2 of this application. Add rows to table as necessary.

Initial Notification or One-time Performance Test?	Regulatory Citation Satisfied	Applicable Source(s)	Date Completed/Approved

17. Existing Prevention of Significant Deterioration or Nonattainment New Source Review Limitations [LAC 33:III.517.D.18]

Do one or more emissions sources represented in this permit application currently operate under one or more NSR permits?
 Yes No

If "yes," summarize the limitations from such permit(s) in the following table. Add rows to table as necessary. Be sure to note any annual emissions limitations from such permit(s) in Section 13 of this application.

Permit Number	Date Issued	Emission Point ID No.	Pollutant	BACT/LAER Limit ¹	Averaging Period	Description of Control Technology/Work Practice Standards

18. Air Quality Dispersion Modeling [LAC 33:III.517.D.15]

Was Air Quality Dispersion Modeling as required by LAC 33:III performed in support of this permit application? (Air Quality Dispersion Modeling is only required when applying for PSD permits and as requested by LDEQ.)

Yes No

Has Air Quality Dispersion Modeling completed in accordance with LAC 33:III ever been performed for this facility in support of an air permit application previously submitted for this facility or process unit (for process unit-specific permits) or as required by other regulations AND approved by LDEQ?

Yes No

If yes, enter the date the most recent Air Quality Dispersion Modeling results as required by LAC 33:III were submitted:

If the answer to either question above is "yes," enter a summary of the most recent results in the following table. If the answer to both questions is "no," enter "none" in the table. Add rows to table as necessary.

Pollutant	Time Period	Calculated Maximum Ground Level Concentration	Louisiana Toxic Air Pollutant Ambient Air Standard or (National Ambient Air Quality Standard {NAAQS})

19. General Condition XVII Activities- Yes No

Enter all activities that qualify as Louisiana Air Emissions Permit General Condition XVII Activities.

- Expand this table as necessary to include all such activities.
- See instructions to determine what qualifies as a General Condition XVII Activity.
- Do not include emissions from General Condition XVII Activities in the proposed emissions totals for the permit application.

Work Activity ¹	Schedule	Emission Rates – TPY					
		PM ₁₀	SO ₂	NO _x	CO	VOC	Other
[GCXVII – 1] Gas Sampling	Weekly					0.10	
[GCXVII – 2] Safety Inspections/Checks on Rupture Disks	Weekly					0.10	
[GCXVII – 3] Inspections on Control Devices	Daily					0.10	
[GCXVII – 4] Service Factors on Control Devices	Daily					0.10	
[GCXVII – 5] Removal of Tank Sludge	Annually					0.10	
[GCXVII – 6] Tank Preparation	Annually					0.10	
[GCXVII – 7] Instrument Maintenance	Monthly					0.10	
[GCXVII – 8] Tank Gauging	Weekly					0.10	
[GCXVII – 9] Nitrogen Blowing of Lines and Equipment	Annually					0.10	
[GCXVII – 10] Purging “Off-Spec” Material to Control Device	Weekly					0.10	
[GCXVII – 11] Compressor Maintenance	Monthly					0.10	
[GCXVII – 12] Valve Maintenance	Annually					0.10	
[GCXVII – 13] Draining Compressor Bottles	Annually					0.10	
[GCXVII – 14] Equipment/ Station Blowdowns	Monthly					3.00	
[GCXVII – 15] Startup and Shutdowns	-			<3.00	<3.00	<3.00	

1: Energy Transfer is not requesting any modification or addition to the GCXVII Activity listing associated with 0760-01944-V0.

21. Regulatory Applicability for Commonly Applicable Regulations – Answer all below [LAC 33:III.517.D.10]

Does this facility contain asbestos or asbestos containing materials? Yes No

If “yes,” the facility or any portion thereof may be subject to 40 CFR 61, Subpart M, LAC 33:III.Chapter 27, and/or LAC 33:III.5151, and this application must address compliance as stated in Section 22 of this application

Is the facility or process unit represented in this permit subject to 40 CFR 68, or is any other process unit located at the same facility as the process unit represented in this application subject to 40 CFR 68? Yes No

If “yes,” the entire facility is subject to 40 CFR 68 and LAC 33:III.Chapter 59, and this application must address compliance as stated in Section 22 of this application.

Is the facility listed in LAC 33:III.5611?

Table 5 Yes No

Table 6 Yes No

Table 7 Yes No

Does the applicant own or operate commercial refrigeration equipment normally containing more than 50 pounds of refrigerant at this facility or process unit? Yes No

If “yes,” the entire facility is subject to 40 CFR 82, Subpart F, and this application must address compliance as stated in Section 22 of this application.

22. Applicable Regulations, Air Pollution Control Measures, Monitoring, and Recordkeeping²

Important points for Table 1 [LAC 33:III.517.D.10]:

- List in Table 1, by Emission Point ID Number and Descriptive Name of the Equipment, state and federal pollution abatement programs and note the applicability or non-applicability of the regulations to each source.
- Adjust the headings for the columns in Table 1 as necessary to reflect all applicable regulations, in addition to any regulations that do not apply but require an explanation to substantiate this fact.
- For each piece of equipment, enter “1” for each regulation that applies. Enter “2” for each regulation that applies to this type of source, but from which this source of emissions is exempt. Enter “3” for equipment that is subject to a regulation, but does not have any applicable requirements. Also, enter “3” for each regulation that has applicable requirements that apply to the particular emission source, but the regulations currently do not apply due to meeting a specific criterion, such as it has not been constructed, modified, or reconstructed since the regulations have been in place.
- Leave the spaces blank when the regulations clearly would not apply under any circumstances to the source. For example, LAC 33:III.2103 – Storage of Volatile Organic Compounds would never apply to a steam generating boiler, no matter the circumstances.
- Consult instructions.

Important points for Table 2 [LAC 33:III.517.D.4; LAC 33:III.517.D.7; LAC 33:III.517.D.10]:

- For each piece of equipment listed in Table 2, include all applicable limitations, recordkeeping, reporting, monitoring, and testing requirements. Also, include any one-time notification or one-time performance test requirements that have not been fulfilled.
- Each of these regulatory aspects (limitations, recordkeeping, reporting, etc.) should be addressed for each regulation that is applicable to each emissions source or emissions point.
- For each regulation that provides a choice regarding the method of compliance, indicate the method of compliance that will be employed. It is not sufficient to state that all compliance options will be employed, though multiple compliance options may be approved as alternative operating scenarios.
- Consult instructions.

Important points for Table 3 [LAC 33:III.517.D.16]:

- Each time a 2 or a 3 is used to describe applicability of a source in Table 1, an entry should be made in Table 3 that explains the exemption or non-applicability status of the regulation to that source.
- Fill in all requested information in the table.
- The exact regulatory citation that provides for the specific exemption or non-applicability determination should be entered into the “Citation Providing for Exemption or Non-applicability” column.
- Consult Instructions.

Important points for Table 4 [LAC 33:III.517.D.18]

- List any single emission source that routes its emissions to another point where these emissions are commingled with the emissions of other sources before being released to the atmosphere. Do not list any single emission source in this table that does not route its emissions in this manner.
- List any and all emission sources that are routed as described above. This includes emission sources that do not otherwise appear in this permit application.
- Consult instructions.

2: The applicable regulations and specific requirements incorporated in the regulatory tables that follow are only associated with proposed modifications to 0760-01944-V0.

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Subject Item ID	Emission Point ID	Description	LAC 33:III.Chapter																				
			2	5	509	9	11	13	15	2103	2104	2107	2111	2113	2115	2116	2121	22	29*	51*	53*	56	59*
UNF 0001	-	Ajax Amine Plant	1	1		1	1	1					1							3	1		3
EQT 0001	1-22A	Plant 1 Amine Unit Vent																					
EQT 0002	1-22B	Plant 1 Amine, Hot Oil Heater					2	1	3														
EQT 0003	2-22A	Plant 1 Glycol Dehy Unit Vent													1								
EQT 0004	2-22B	Plant 1 Glycol Dehy Reboiler					2	1	3														
EQT 0005	3-22A	Plant 2 Amine Unit Vent																					
EQT 0006	3-22B	Plant 2 Amine Hot Oil Heater					2	1	3														
EQT 0007	4-22A	Plant 2 Glycol Dehy Unit Vent													1								
EQT 0008	4-22B	Plant 2 Glycol Dehy Reboiler					2	1	3														
EQT 0009	5-22	Plant 1 Thermal Oxidizer					1	1	1														
EQT 0010	6-22	Plant 2 Thermal Oxidizer					1	1	1														
EQT 0011	7-22	CAT G3606 Compressor Engine					2	1	3														
EQT 0012	8-22	CAT G3606 Compressor Engine					2	1	3														
EQT 0013	9-22	CAT G3606 Compressor Engine					2	1	3														
EQT 0014	10-22	CAT G3606 Compressor Engine					2	1	3														
EQT 0022	18-22	Skid Drain Storage Tank								4													
EQT 0023	19-22	Flare		1				1	3														
EQT TBD1	1-23	CAT G3608 Compressor Engine		1			2	1	3														
EQT TBD2	2-23	CAT G3608 Compressor Engine		1			2	1	3														
EQT TBD3	3-23	Sulfur Loading and Handling						1															
EQT TBD4	5-23B	CO ₂ Dehydrator Reboiler					2	1	3														
EQT TBD5	6-23	Carbon Capture Produced Water Storage Tank								3													
EQT TBD6	7-23	Carbon Capture Produced Water Storage Tank								3													
EQT TBD7	8-23	Carbon Capture Produced Water Loading									3												
FUG 0001	FUG	Fugitive Emissions											1				3						

KEY TO MATRIX

- 1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.
- 2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.
- 3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.

Blank – The regulations clearly do not apply to this type of emission source.

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Subject Item ID	Emission Point ID	Description	40 CFR 60 NSPS									40 CFR 61			40 CFR 63 NESHAP					40 CFR			
			A	K	Ka	Kb	KKK	Db	Dc	LLL	JJJJ	OOOa	A	J	V	A	HH	HHH	4Y	ZZZ	64	68	
UNF 0001	-	Ajax Amine Plant	1													1							3
EQT 0001	1-22A	Plant 1 Amine Unit Vent													1								
EQT 0002	1-22B	Plant 1 Amine Hot Oil Heater						1															
EQT 0003	2-22A	Plant 1 Glycol Dehy Unit Vent															1	3					
EQT 0004	2-22B	Plant 1 Glycol Dehy Reboiler																					
EQT 0005	3-22A	Plant 2 Amine Unit Vent													1								
EQT 0006	3-22B	Plant 2 Amine Hot Oil Heater						1															
EQT 0007	4-22A	Plant 2 Glycol Dehy Unit Vent															1	3					
EQT 0008	4-22B	Plant 2 Glycol Dehy Reboiler																					
EQT 0009	5-22	Plant 1 Thermal Oxidizer																					
EQT 0010	6-22	Plant 2 Thermal Oxidizer																					
EQT 0011	7-22	CAT G3606 Compressor Engine										1	1									1	
EQT 0012	8-22	CAT G3606 Compressor Engine										1	1									1	
EQT 0013	9-22	CAT G3606 Compressor Engine										1	1									1	
EQT 0014	10-22	CAT G3606 Compressor Engine										1	1									1	
EQT 0022	18-22	Skid Drain Storage Tank				3							3										
EQT 0023	19-22	Flare																					
EQT TBD1	1-23	CAT G3608 Compressor Engine										1	3									1	
EQT TBD2	2-23	CAT G3608 Compressor Engine										1	3									1	
EQT TBD3	3-23	Sulfur Loading and Handling																					
EQT TBD4	5-23B	CO ₂ Dehydrator Reboiler																					
EQT TBD5	6-23	Carbon Capture Produced Water Storage Tank				3							3										
EQT TBD6	7-23	Carbon Capture Produced Water Storage Tank				3							3										
EQT TBD7	8-23	Carbon Capture Produced Water Loading																					
FUG 0001	FUG	Fugitive Emissions					3						1										

KEY TO MATRIX

1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.

2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.

3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.

Blank – The regulations clearly do not apply to this type of emission source.

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
CRG 0001 - CAT G3606 Compressor Engines EQT 0011, EQT 0012, EQT 0013, EQT 0014	40 CFR 60 Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	Requirements that limit emissions or operations - (Excluding formaldehyde) VOC, Total <= 0.7 g/BHP-hr (0.00154 lb/HP-hr; 60 ppmv at 15% O2). Subpart JJJJ. [40 CFR 60.4233(e)]	40 CFR 60.4233(e) Current Permit SR 1	Which Months: All Year Statistical Basis: None Specified	
		Requirements that limit emissions or operations - Carbon monoxide <= 2.0 g/BHP-hr (0.0044 lb/HP-hr; 270 ppmv at 15% O2). Subpart JJJJ. [40 CFR 60.4233(e)]	40 CFR 60.4233(e) Current Permit SR 2	Which Months: All Year Statistical Basis: None Specified	
		Requirements that limit emissions or operations - Nitrogen oxides <= 1.0 g/BHP-hr (0.0022 lb/HP-hr; 82 ppmv at 15% O2). Subpart JJJJ. [40 CFR 60.4233(e)]	40 CFR 60.4233(e) Current Permit SR 3	Which Months: All Year Statistical Basis: None Specified	
		Requirements that limit emissions or operations - Operate and maintain stationary SI ICE to achieve the emission standards as required in 40 CFR 60.4233 over the entire life of the engine. Subpart JJJJ.	40 CFR 60.4234 Current Permit SR 4		
		Requirements that specify performance testing - Conduct an initial performance test. For engines greater than 500 HP, conduct subsequent performance testing every 8,760 hours or 3 years, whichever comes first, thereafter to demonstrate compliance. Subpart JJJJ. [40 CFR 60.4243(b)(2)]	40 CFR 60.4243(b)(2) Current Permit SR 5		
		Requirements that limit emissions or operations - Demonstrate compliance according to the emission standards specified in 40 CFR 60.4233(e), the requirements specified in 40 CFR 60.4244, as applicable, and the requirements specified in 40 CFR 60.4243(b)(2)(i) and (b)(2)(ii), as applicable. Subpart JJJJ. [40 CFR 60.4243(b)(2)]	40 CFR 60.4243(b)(2) Current Permit SR 6		
		Requirements that limit emissions or operations - Ensure that the engine is maintained and operated to the extent practicable in a manner consistent with good air pollution control practice for minimizing emissions. Subpart JJJJ. [40 CFR 60.4243(b)(2)]	40 CFR 60.4243(b)(2) Current Permit SR 7		
		Requirements that specify performance testing - Perform initial performance testing as indicated in 40 CFR 60.4243, if the engine is either non-certified or is not operated or maintained, along with the control device, according to the manufacturer's written emission-related instructions. Conduct subsequent performance testing, if the engine is rebuilt or undergoes major repair or maintenance. Subpart JJJJ. [40 CFR 60.4243(f)]	40 CFR 60.4243(f) Current Permit SR 8		
		Requirements that limit emissions or operations - Air-to-fuel ratio controller. Maintain and operate appropriately in order to ensure proper operation of the engine and control device to minimize emissions at all times. Subpart JJJJ. [40 CFR 60.4243(g)]	40 CFR 60.4243(g) Current Permit SR 9		
		Requirements that specify performance testing - Conduct performance tests by following the procedures in 40 CFR 60.4244(a) through (g). Subpart JJJJ.	40 CFR 60.4244 Current Permit SR 10		
		Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data recordkeeping by electronic or hard copy at the approved frequency. Keep records of the information in 40 CFR 60.4245(a)(1) through (a)(4). Subpart JJJJ. [40 CFR 60.4245(a)]	40 CFR 60.4245(a) Current Permit SR 11		
		Requirements that specify reports to be submitted - Submit an initial notification as required in 40 CFR 60.7(a)(1). Include the information in 40 CFR 60.4245(e)(1) through (c)(5). Subpart JJJJ. [40 CFR 60.4245(c)]	40 CFR 60.4245(c) Current Permit SR 12		
		Requirements that specify reports to be submitted - Submit performance test results. Due within 60 days after each test conducted according to 40 CFR 60.4244 has been completed. Subpart JJJJ. [40 CFR 60.4245(d)]	40 CFR 60.4245(d) Current Permit SR 13		

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
CRG 0001 - CAT G3606 Compressor Engines EQT 0011, EQT 0012, EQT 0013, EQT 0014	40 CFR 60 Subpart OOOO - Standards of Performance for Crude Oil and Natural Gas Facilities for Which Construction, Modification, or Reconstruction Commenced After August 23, 2011, and on or Before September 18, 2015	Requirements that specify performance testing - Perform the reporting as required by § 60.5420a(b)(1) and (4) and the recordkeeping as required by § 60.5420a(c)(3), (6) through (9), and (17), as applicable.	40 CFR 60.5385a(d) Current Permit SR 14		
	40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Requirements that limit emissions or operations - Reduce VOC emissions by complying with one of the following three options: 1) Replace the reciprocating compressor rod packing on or before the compressor has operated for 26,000 hours, 2) replace the reciprocating compressor rod packing prior to 36 months from the date of the most recent rod packing replacement, or 36 months from the date of startup for a new reciprocating compressor for which the rod packing has not yet been replaced, or 3) collect the VOC emissions from the rod packing using a rod packing emissions collection system that operates under negative pressure and route the rod packing emissions to a process through a closed vent system that meets the requirements of 40 CFR 60.5411a(a) and (d). If complying with the first option, continuously monitor the number of hours of operation beginning upon initial startup, August 2, 2016, or the date of the most recent reciprocating compressor rod packing replacement, whichever is later. Subpart OOOOa. [40 CFR 60.5385a(a)]	40 CFR 60.5385a(a) Current Permit SR 15		
		Requirements that specify reports to be submitted - Submit initial annual report as specified in 60.5420a(b)(1) and (4).	40 CFR 60.5410a(c)(3) Current Permit SR 16	Which Months: All Year Statistical Basis: None Specified	
		Requirements that specify monitoring - Equipment/operational data monitored by technically sound method continuously. During the initial compliance period, continuously monitor the number of hours of operation or track the number of months since initial startup, since August 2, 2016, or since the last rod packing replacement, whichever is latest. Subpart OOOOa. [40 CFR 60.5410a(c)(1)]	40 CFR 60.5410a(c)(1) Current Permit SR 17	Which Months: All Year Statistical Basis: None Specified	
		Requirements that limit emissions or operations - Replace the reciprocating compressor rod packing on or before the total number of hours of operation reaches 26,000 hours or the number of months since the most recent rod packing replacement reaches 36 months	40 CFR 60.5415a(c)(3) Current Permit SR 18		
		Requirements that specify monitoring - Equipment/operational data monitored by technically sound method continuously. Demonstrate continuous compliance by continuously monitoring the number of hours of operation or tracking the number of months since initial startup, since August 2, 2016, or since the date of the most recent reciprocating compressor rod packing replacement, whichever is later. Subpart OOOOa. [40 CFR 60.5415a(c)(1)]	40 CFR 60.5415a(c)(1) Current Permit SR 19		
		40 CFR 63 Subpart ZZZZ - National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines	Requirements that limit emissions or operations - Meet the requirements of 40 CFR 60 Subpart JJJJ for spark ignition engines.	40 CFR 63.6590(c) Current Permit SR 20	
	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes. (Complies by using sweet natural gas as fuel).	LAC 33-III.1311.C Current Permit SR 21	Which Months: All Year Statistical Basis: Six-minute average	
CRG 0002 - Amine Hot Oil Heaters EQT 0002, EQT 0006	40 CFR 60 Subpart De - Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units	Requirements that specify records to be kept and requirements that specify record retention time - Shall submit notification of the date of construction or reconstruction and actual startup, as provided by 40 CFR 60.7.	40 CFR 60.48c(a)(1) - (4) Current Permit SR 22		
		Requirements that specify records to be kept and requirements that specify record retention time - Fuel rate recordkeeping by electronic or hard copy monthly. Keep records of the amount of each fuel combusted during each calendar month. Subpart De.	40 CFR 60.48c(g)(2) Current Permit SR 23		
		Requirements that specify records to be kept and requirements that specify record retention time - All records required under this section shall be maintained by the owner or operator of the affected facility for a period of two years following the date of such record.	40 CFR 60.48c(i) Current Permit SR 24		
	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Total suspended particulate <= 0.6 lb/MMBTU of heat input (Complies by using sweet natural gas as fuel).	LAC 33-III.1313.C Current Permit SR 25	Which Months: All Year Statistical Basis: None Specified	
CRG 0003 - Glycol Dehy Unit Vents EQT 0003, EQT 0007	40 CFR 63 - Subpart HH - National Emission Standards for Hazardous Air Pollutants From Oil and Natural Gas Production Facilities	Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data recordkeeping by electronic or hard copy at the approved frequency. Keep records of the information specified in 40 CFR 63.774(d)(i)(i) or (d)(i)(ii), as applicable. Subpart HH. (40 CFR 63.774(d))	40 CFR 63.774(d) Current Permit SR 26		
	LAC 33-III Chapter 21 - Control of Emissions of Organic Compounds	Requirements that specify records to be kept and requirements that specify record retention time - Throughput recordkeeping by electronic or hard copy daily. Keep records of the actual throughput per day and the glycol circulation rate.	LAC 33-III.2116.F.4 b Current Permit SR 27		

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
CRG 0004 - Tanks EQT 0020, EQT 0021, EQT-0022	LAC 33:III Chapter 21 - Control of Emissions of Organic Compounds	Requirements that limit emissions or operations - Equip with a submerged fill pipe.	LAC 33:III.2103.A Current Permit SR 28		
		Requirements that limit emissions or operations - Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-c.	LAC 33:III.2103.H.3 Current Permit SR 29		
		Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Keep records of the information specified in LAC 33:III.2103.I.1 through I.7, as applicable. Maintain records for at least two years.	LAC 33:III.2103.I Current Permit SR 30		
CRG TBD - CAT G3608 Compressor Engines EQT TBD1, EQT TBD2	40 CFR 60 Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	Requirements that limit emissions or operations - Operate and maintain stationary SI ICE to achieve the emission standards as required in 40 CFR 60.4233 over the entire life of the engine.	40 CFR 60.4234 Proposed SR		
		Requirements that limit emissions or operations - If you are an owner or operator of a stationary SI internal combustion engine that is manufactured after July 1, 2008, and must comply with the emission standards specified in § 60.4233(a) through (c), you must comply by purchasing an engine certified to the emission standards in § 60.4231(a) through (c), as applicable, for the same engine class and maximum engine power.	40 CFR 60.4243(a) Proposed SR		
		Requirements that limit emissions or operations - If you operate and maintain the certified stationary SI internal combustion engine and control device according to the manufacturer's emission-related written instructions, you must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required if you are an owner or operator. You must also meet the requirements as specified in 40 CFR part 1068, subparts A through D, as they apply to you. If you adjust engine settings according to and consistent with the manufacturer's instructions, your stationary SI internal combustion engine will not be considered out of compliance.	40 CFR 60.4243(a)(1) Proposed SR		
		Requirements that limit emissions or operations - Purchasing an engine certified according to procedures specified in this subpart, for the same model year and demonstrating compliance according to one of the methods specified in paragraph (a) of this section.	40 CFR 60.4243(b)(1) Proposed SR		
		Requirements that specify monitoring - Owners and operators of stationary SI natural gas fired engines may operate their engines using propane for a maximum of 100 hours per year as an alternative fuel solely during emergency operations, but must keep records of such use. If propane is used for more than 100 hours per year in an engine that is not certified to the emission standards when using propane, the owners and operators are required to conduct a performance test to demonstrate compliance with the emission standards of § 60.4233.	40 CFR 60.4243(e) Proposed SR		
		Requirements that specify monitoring - It is expected that air-to-fuel ratio controllers will be used with the operation of three-way catalysts/non-selective catalytic reduction. The air-to-fuel ratio controller must be maintained and operated appropriately in order to ensure proper operation of the engine and control device to minimize emissions at all times.	40 CFR 60.4243(g) Proposed SR		
		Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data recordkeeping by electronic or hard copy at the approved frequency. Keep records of the information in 40 CFR 60.4245(a)(1) through (a)(4).	40 CFR 60.4245(a) Proposed SR		
		Requirements that specify reports to be submitted - Submit an initial notification as required in 40 CFR 60.7(a)(1). Include the information in 40 CFR 60.4245(c)(1)	40 CFR 60.4245(c) Proposed SR		
		Requirements that limit emissions or operations - Meet the requirements of 40 CFR 60 Subpart IIII for compression ignition engines or 40 CFR 60 Subpart JJJJ for spark ignition engines.	40 CFR 63.6590(c) Proposed SR		
		LAC 33:III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes	LAC 33:III.1311.C Proposed SR	Which Months: All Year Statistical Basis: Six minute average
EQT TBD3 - Sulfur Loading and Handling	LAC 33:III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - All reasonable precautions shall be taken to prevent particulate matter from becoming airborne. Those precautions shall include, but not be limited to those specified in LAC 33:III.1305.1-7	LAC 33:III.1305 Proposed SR	Which Months: All Year Statistical Basis: None Specified	
EQT TBD4 - CO ₂ Dehydrator Reboiler	LAC 33:III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Total suspended particulate <= 0.6 lb/MMBTU of heat input.	LAC 33:III.1313.C Proposed SR	Which Months: All Year Statistical Basis: None Specified	

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
<u>EQT 0001 - Plant 1 Amine Unit Vent</u>	40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Requirements that specify records to be kept and requirements that specify record retention time - To certify that a facility is exempt from the control requirements of these standards, for each facility with a design capacity less than 2 LT/D of H2S in the acid gas (expressed as sulfur) you must keep, for the life of the facility, an analysis demonstrating that the facility's design capacity is less than 2 LT/D of H2S expressed as sulfur.	40 CFR 60.5423a(c) Current Permit SR 31		
<u>EQT 0004 - Plant 1 Glycol Dehy Reboiler</u>	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Total suspended particulate <= 0.6 lb/MMBTU of heat input.	LAC 33-111.1313 C Current Permit SR 32	Which Months: All Year Statistical Basis: None Specified	
<u>EQT 0005 - Plant 2 Amine Unit Vent</u>	40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Requirements that specify records to be kept and requirements that specify record retention time - To certify that a facility is exempt from the control requirements of these standards, for each facility with a design capacity less than 2 LT/D of H2S in the acid gas (expressed as sulfur) you must keep, for the life of the facility, an analysis demonstrating that the facility's design capacity is less than 2 LT/D of H2S expressed as sulfur.	40 CFR 60.5423a(c) Current Permit SR 33		
<u>EQT 0008 - Plant 2 Glycol Dehy Reboiler</u>	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that specify monitoring - Total suspended particulate <= 0.6 lb/MMBTU of heat input.	LAC 33-111.1313 C Current Permit SR 34	Which Months: All Year Statistical Basis: None Specified	
<u>EQT 0009 - Plant 1 Thermal Oxidizer</u>	LAC 33-III Chapter 11 - Control of Emissions of Smoke	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33-III.1101 B Current Permit SR 35	Which Months: All Year Statistical Basis: None Specified	
	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33-III.1311 C Current Permit SR 36	Which Months: All Year Statistical Basis: Six-minute average	
	LAC 33-III Chapter 15 - Emission Standards for Sulfur Dioxide	Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data record keeping by electronic or hard copy once initially and annually. Record and retain at the site sufficient data to show annual potential sulfur dioxide emissions.	LAC 33-III.1513 C Current Permit SR 37		
<u>EQT 0010 - Plant 2 Thermal Oxidizer</u>	LAC 33-III Chapter 11 - Control of Emissions of Smoke	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33-III.1101 B Current Permit SR 38	Which Months: All Year Statistical Basis: None Specified	
	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33-III.1311 C Current Permit SR 39	Which Months: All Year Statistical Basis: Six-minute average	
	LAC 33-III Chapter 15 - Emission Standards for Sulfur Dioxide	Requirements that specify records to be kept and requirements that specify record retention time - Equipment/operational data recordkeeping by electronic or hard copy once initially and annually. Record and retain at the site sufficient data to show annual potential sulfur dioxide emissions.	LAC 33-III.1513 C Current Permit SR 40		
<u>EQT 0023 - Flare</u>	LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Opacity <= 20 percent, except for emissions that have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33-III.1311 C Current Permit SR 41	Which Months: All Year Statistical Basis: Six-minute average	
	LAC 33-III Chapter 5 - Permit Procedures	Requirements that limit emissions or operations - Develop a corrective action plan for re-lighting the flare. Keep plan readily available for immediate implementation in the event the flare needs to be re-lit. Requirements that specify monitoring - Presence of a flame monitored by visual inspection/determination daily.	LAC 33-III.501.C.6 Current Permit SR 42 LAC 33-III.507.H.1.a Current Permit SR 43	Which Months: All Year Statistical Basis: None Specified	
		Requirements that specify records to be kept and requirements that specify record retention time - Presence of a flame recordkeeping by electronic or hard copy daily.	LAC 33-III.507.H.1.a Current Permit SR 44		
<u>FUG 0001 - Fugitive Emissions</u>	40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Requirements that limit emissions or operations - In accordance with EPA's Questions and Answers document titled "Congressional Review Act Resolution to Disapprove EPA's 2020 Oil and Gas Policy Rule," dated June 30, 2021, the permittee shall comply with the methane standards of 40 CFR 60 Subpart OOOOa as promulgated on June 3, 2016 (81 FR 35898) and amended on March 12, 2018 (83 FR 10638) and with the VOC standards of 40 CFR 60 Subpart OOOOa as amended on	40 CFR 60.5497a Current Permit SR 45		
	LAC 33-III Chapter 21 - Control of Emissions of Organic Compounds	Requirements that limit emissions or operations - Equip all rotary pumps and compressors handling volatile organic compounds having a true vapor pressure of 1.5 psia or greater at handling conditions with mechanical seals or other equivalent equipment.	LAC 33-III.2111 Current Permit SR 46		

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
LNF 0001 - Ajax Amine Plant	40 CFR 60 Subpart OOOOa - Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Requirements that limit emissions or operations - At all times, including periods of startup, shutdown, and malfunction, owners and operators shall maintain and operate any affected facility including associated air pollution control equipment in a manner consistent with good air pollution control practice for minimizing emissions.	40 CFR 60.5370a(b) Current Permit SR 47		
		Requirements that specify reports to be submitted - Submit annual report. Due initially no later than 90 days after the end of the initial compliance period, as determined according to 40 CFR 60.5410a. Submit subsequent annual reports no later than the same date each year as the initial annual report. Include the general information specified in 40 CFR 60.5420a(b)(1)(i) through (b)(1)(iv). Include the applicable information specified in 40 CFR 60.5420a(b)(2)(i) through (b)(2)(sv) as specified in 40 CFR 60.5420a(b)(2), for a well affected facility. Include the information specified in 40 CFR 60.5420a(b)(3)(i) through (b)(3)(v), for a centrifugal compressor affected facility. Include the information specified in 40 CFR 60.5420a(b)(4)(i) and (b)(4)(iii), for a reciprocating compressor affected facility. Include the information specified in 40 CFR 60.5420a(b)(5)(i) through (b)(5)(iii), for a pneumatic controller affected facility. Include the information specified in 40 CFR 60.5420a(b)(6)(i) through (b)(6)(ix), for a storage vessel affected facility. Include the information specified in 40 CFR 60.5420a(b)(7)(i) through (b)(7)(iii), as applicable, for a collection of fugitive emissions components at each well site and a collection of fugitive emissions components at each compressor station. Include the information specified in 40 CFR 60.5420a(b)(8)(i) through (b)(8)(iv), for a pneumatic pump affected facility. Include performance test reports as specified in 40 CFR 60.5420a(b)(9) or (b)(10), if applicable. Follow the procedure specified in 40 CFR 60.5420a(b)(11). One report may be submitted for multiple affected facilities, provided the report contains all of the information required as specified in 40 CFR 60.5420a(b)(1) through (b)(8) and (b)(12). Annual reports may coincide with title V reports, as long as all the required elements of the annual report are included. The facility may arrange with LDEQ a common schedule on which reports required by 40 CFR 60 may be submitted, as long as the schedule does not extend the reporting period. Subpart OOOOa. Submit the certification signed by the qualified professional engineer or in-house engineer according to 40 CFR 60.5411a(d) for each closed vent system routing to a control device or process, as specified in 40 CFR 60.5420a(b)(12), [40 CFR 60.5420a(b)]	40 CFR 60.5420a(b) Current Permit SR 48		
		Requirements that specify records to be kept and requirements that specify record retention time - Maintain all records required by 40 CFR 60 Subpart OOOOa either onsite or at the nearest local field office for at least 5 years. Any records required to be maintained by 40 CFR 60 Subpart OOOOa that are submitted electronically via the EPA's CDX may be maintained in electronic format. Subpart OOOOa. [40 CFR 60.5420a(c)]	40 CFR 60.5420a(c) Current Permit SR 49		
40 CFR 60 Subpart A - General Provisions	Requirements that limit emissions or operations - All affected facilities shall comply with all applicable provisions in 40 CFR 60 Subpart A.	40 CFR 60. Current Permit SR 50			
40 CFR 63 Subpart HH - National Emission Standards for Hazardous Air Pollutants From Oil and Natural Gas Production Facilities	Requirements that limit emissions or operations - All affected facilities shall comply with all applicable provisions in 40 CFR 63 Subpart A as delineated in Table 2 of 40 CFR 63 Subpart HH.	40 CFR 63. Current Permit SR 51			
LAC 33-III Chapter 11 - Control of Emissions of Smoke	Requirements that limit emissions or operations - Emissions of smoke which pass onto or across a public road and create a traffic hazard by impairment of visibility as defined in LAC 33-III.111 or intensifies an existing traffic hazard condition are prohibited.	LAC 33-III.1103 Current Permit SR 52			
	Requirements that limit emissions or operations - Outdoor burning of waste material or other combustible material is prohibited.	LAC 33-III.1109 B Current Permit SR 53			
LAC 33-III Chapter 13 - Emission Standards for Particulate Matter	Requirements that limit emissions or operations - Emissions of particulate matter which pass onto or across a public road and create a traffic hazard by impairment of visibility or intensify an existing traffic hazard condition are prohibited.	LAC 33-III.1303 B Current Permit SR 54			
LAC 33-III Chapter 21 - Control of Emissions of Organic Compounds	Requirements that limit emissions or operations - Maintain best practical housekeeping and maintenance practices at the highest possible standards to reduce the quantity of organic compounds emissions. Good housekeeping includes, but is not limited to, the practices listed in LAC 33-III.2113 A. 1 through A. 5.	LAC 33-III.2113 A Current Permit SR 55			
LAC 33-III Chapter 2 - Rules and Regulations for the Fee System of the Air Quality Control Programs	Requirements that limit emissions or operations - Failure to pay the prescribed application fee or annual fee as provided herein, within 90 days after the due date, will constitute a violation of these regulations and shall subject the person to applicable enforcement actions under the Louisiana Environmental Quality Act including, but not limited to, revocation or suspension of the applicable permit, license, registration, or variance.	LAC 33-III.219 Current Permit SR 56			
LAC 33-III Chapter 5 - Permit Procedures	Requirements that specify monitoring - Monitor and record the date/time and duration of downtime for each thermal oxidizer (EQT 9 and EQT 10) while Plant 1 and 2 amine units are in operation. Planned outages of both thermal oxidizers (EQT 9 and EQT 10) while Plant 1 and 2 amine units are in operation shall not occur simultaneously.	LAC 33-III.501 C.6 Current Permit SR 57			

TABLE 2. STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/Frequency	State Only Requirement
UNF 0001 - Ajax Amine Plant	LAC 33:III Chapter 5 - Permit Procedures	Requirements that limit emissions or operations - Comply with the Part 70 General Conditions as set forth in LAC 33:III.535 and the Louisiana General Conditions as set forth in LAC 33:III.537. [LAC 33:III.535, LAC 33:III.537]	LAC 33:III.535 Current Permit SR 58		
	LAC 33:III Chapter 56 - Prevention of Air Pollution Emergency Episodes	Requirements that specify reports to be submitted - Submit standby plan for the reduction or elimination of emissions during an Air Pollution Alert, Air Pollution Warning, or Air Pollution Emergency. Due within 30 days after requested by DEQ.	LAC 33:III.5611.A Current Permit SR 59		
		Requirements that limit emissions or operations - During an Air Pollution Alert, Air Pollution Warning or Air Pollution Emergency, make the standby plan available on the premises to any person authorized by DEQ to enforce these regulations.	LAC 33:III.5611.B Current Permit SR 60		
LAC 33:III Chapter 9 - General Regulations on Control of Emissions and Emission Standards	Requirements that specify monitoring - Install air pollution control facilities whenever practically, economically, and technologically feasible, except as specified in LAC 33:III.905.B. When facilities have been installed on a property, use and diligently maintain in proper working order whenever any emissions are being made which can be controlled by the facilities, even though the ambient air quality standards in affected areas are not exceeded.	LAC 33:III.905 Current Permit SR 61			
	Requirements that specify reports to be submitted - Submit Emission Inventory (EI)/Annual Emissions Statement. Due annually, by the 30th of April to the Office of Environmental Assessment, for the reporting period of the previous calendar year that coincides with period of ownership or operatorship, until released from reporting, in writing, by DEQ. Submit both an emissions inventory and the certification statement required by LAC 33:III.919.F.1.c, separately for each AI, in a format specified by DEQ.	LAC 33:III.919 Current Permit SR 62			
	Requirements that specify reports to be submitted - Report the unauthorized discharge of any air pollutant into the atmosphere in accordance with LAC 33:III.Chapter 39, Notification Regulations and Procedures for Unauthorized Discharges. Submit written reports to DEQ pursuant to LAC 33:III.3925. Submit timely and appropriate follow-up reports detailing methods and procedures to be used to prevent similar atmospheric releases.	LAC 33:III.927 Current Permit SR 63			
LAC 33:III Chapter 51 - Comprehensive Toxic Air Pollutant Emission Control Program	Requirements that limit emissions or operations - Do not cause a violation of any ambient air standard listed in LAC 33:III.5112, Table 51.2, unless operating in accordance with LAC 33:III.5109.B.	LAC 33:III.5105.A.2 Proposed SR			
	Requirements that specify reports to be submitted - Include a certification statement with the annual emission report and revisions to any emission report that attests that the information contained in the emission report is true, accurate, and complete, and that is signed by a responsible official, as defined in LAC 33:III.502. Include the full name of the responsible official, title, signature, date of signature and phone number of the responsible official.	LAC 33:III.5107.A.2 Proposed SR			
	Requirements that specify reports to be submitted - Submit Annual Emissions Report. Due annually, by the 30th of April unless otherwise directed by DEQ, to the Office of Environmental Services in a format specified by DEQ. Identify the quantity of emissions in the previous calendar year for any toxic air pollutant listed in Table 51.1 or Table 51.3.	LAC 33:III.5107.A Proposed SR			
	Requirements that specify reports to be submitted - Submit notification. Due to the Department of Public Safety 24-hour Louisiana Emergency Hazardous Materials Hotline in accordance with LAC 33:III.3915.A, after any discharge of a toxic air pollutant into the atmosphere that results or threatens to result in an emergency condition, as defined in LAC 33:III.3905.A.	LAC 33:III.5107.B.1 Proposed SR			
	Requirements that specify reports to be submitted - Submit notification. Due to SPOC, except as provided in LAC 33:III.5107.B.4, immediately, but in no case later than 24 hours after any unauthorized discharge of a toxic air pollutant into the atmosphere that does not cause an emergency condition, the rate or quantity of which is in excess of that allowed by permit, compliance schedule, or variance, or for upset events that exceed the reportable quantity in LAC 33:III.3931. Submit notification in the manner provided in LAC 33:III.3923.	LAC 33:III.5107.B.2 Proposed SR			
	Requirements that specify reports to be submitted - Submit written report. Due by certified mail to SPOC within seven calendar days of learning of any such discharge or equipment bypass as referred to in LAC 33:III.5107.B.1 and B.2. Include the information specified in LAC 33:III.5107.B.3.a.i through B.3.a.viii.	LAC 33:III.5107.B.3 Proposed SR			
	Requirements that specify reports to be submitted - Develop a standard operating procedure (SOP) within 120 days after achieving or demonstrating compliance with the standards specified in LAC 33:III.Chapter 51. Detail in the SOP all operating procedures or parameters established to ensure that compliance with the applicable standards is maintained and address operating procedures for any monitoring systems in place, specifying procedures to ensure compliance with LAC 33:III.5113.C.5. Make a written copy of the SOP available on site or at any alternate approved location for inspection by DEQ. Provide a copy of the SOSP within 30 days upon request by DEQ.	LAC 33:III.5109.C.2 Proposed SR			

Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana

TABLE 3. EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
UNF 0001 - Ajax Amine Plant	Chemical Accident Prevention Provisions 40 CFR 68	Does Not Apply	Plant does not produce, handle, process, or store substances listed in 40 CFR 68.130, Table 59.0 of LAC 33:III.5907, or Table 59.1 of LAC 33:III.5913 in quantities greater than the listed thresholds.	40 CFR 68 LAC 33:III.Chapter 59
	Chemical Accident Prevention and Minimization of Consequences LAC 33:III.Chapter 59			
	Comprehensive Toxic Air Pollutant Emission Control Program LAC 33:III.Chapter 51	Does Not Apply	Facility is not a major source of TAPs.	LAC 33:III.5101.A
EQT 0003 - Plant 1 Glycol Dehy Unit Vent, EQT 0007 - Plant 2 Glycol Dehy Unit Vent	Glycol Dehydrators LAC 33:III.2116	Exempt	The total uncontrolled VOC emissions from the glycol dehydrators do not exceed nine (9) tons per year per glycol dehydrator.	LAC 33:III.2116.C.2
	National Emission Standards for Hazardous Air Pollutants From Natural Gas Transmission and Storage Facilities 40 CFR 63 Subpart HHHH	Does Not Apply	The facility is not a natural gas transmission or storage facility	40 CFR 63.1270(a)
EQT 0002 - Plant 1 Amine Hot Oil Heater, EQT 0004 - Plant 1 Glycol Dehy Reboiler, EQT 0006 - Plant 2 Amine Hot Oil Heater, EQT 0008 - Plant 2 Glycol Dehy Reboiler, EQT 0011 - CAT G3606 Compressor Engine, EQT 0012 - CAT G3606 Compressor Engine, EQT 0013 - CAT G3606 Compressor Engine, EQT 0014 - CAT G3606 Compressor Engine,	Control of Emissions of Smoke LAC 33:III.1101	Exempt	These units only combust natural gas.	LAC 33:III.1107.B.1
	Emission Standards for Sulfur Dioxide LAC 33:III.Chapter 15	Does Not Apply	Potential SO ₂ emissions < 5 TPY.	LAC 33:III.1502.A.3
EQT TBD4 - CO ₂ Dehydrator Reboiler				

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 3. EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
EQT TBD1 - CAT G3608 Compressor Engine, EQT TBD2 - CAT G3608 Compressor Engine	Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution for which Construction, Modification or Reconstruction Commenced After September 18, 2015. 40 CFR 60 Subpart OOOOa	Does Not Apply	Compressors are not in natural gas service	40 CFR 60.5430a
	Control Emissions of Smoke LAC 33:III.Chapter 11	Exempt	The opacity standards set forth in LAC 33:III.1101 do not apply to combustion units when combusting only natural gas, carbon monoxide, hydrogen, and/or other gaseous fuels with a carbon to hydrogen molecular ratio of less than 0.34.	LAC 33:III.1107.B.1
	Emission Standard for Sulfur Dioxide LAC 33:III.Chapter 15	Does Not Apply	Single point sources have the potential to emit less than 5 tons per year of sulfur dioxide.	LAC 33:III.1502.A.3
EQT 0022 - Skid Drain Storage Tank, EQT TBD5 - Carbon Capture Produced Water Storage Tank, EQT TBD6 - Carbon Capture Produced Water Storage Tank	Control of Organic Compound Emissions, Storage of Volatile Organic Compounds LAC 33:III.2103	Does Not Apply	The maximum true vapor pressure of the volatile organic liquid stored is less than 1.5 psia.	LAC 33:III.2103.A
	Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984) 40 CFR 60 Subpart Kb	Does Not Apply	Vessels have a design capacity less than or equal to 1,589.874 m ³ and are used for petroleum or condensate stored, processed, or treated prior to custody transfer.	40 CFR 60.110b(d)(4)
	Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution for which Construction, Modification or Reconstruction Commenced After August 23, 2011, and on or before September 15, 2015. 40 CFR 60 Subpart OOOO	Does Not Apply	The potential VOC emissions from each single storage vessel located at the facility are less than six tons per year.	40 CFR 60.5365(e)
	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015 40 CFR 60 Subpart OOOOa	Does Not Apply	VOC emissions from each of these sources is less than 6 tpy.	40 CFR 60.5365a(e)(2)

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 3. EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
EQT TBD7 - Carbon Capture Produced Water Loading	Control of Emissions of Organic Compounds from VOC Loading LAC 33:III.2107	Does Not Apply	The facility does not have a throughput of more than 20,000 gallons per day.	LAC 33:III.2107.A.1
EQT 0023 - Flare	Emission Standards for Sulfur Dioxide LAC 33:III.Chapter 15	Does Not Apply	Potential SO2 emissions < 5 TPY.	LAC 33:III.1502.A.3
FUG 0001 - Fugitive Emissions	Standards of Performance for Equipment Leaks of VOC From Onshore Natural Gas Processing Plants for which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011 40 CFR 60 Subpart KKK	Does Not Apply	The facility is not an onshore natural gas processing plant.	40 CFR 60.630(a)(1)
	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015 40 CFR 60 Subpart OOOOa	Does Not Apply	Facility is not classified as a natural gas processing plant.	40 CFR 60.5430a
	Fugitive Emission Control LAC 33:III.2121	Does Not Apply	The facility is not a petroleum refinery, natural gas processing plant, synthetic organic chemical manufacturing industry facility, methyl tertiary butyl ether manufacturing facility, or polymer manufacturing facility.	LAC 33:III.2121.A

**Ajax Amine Plant
ET Gathering & Processing LLC
Pelican, DeSoto Parish, Louisiana**

TABLE 4. EQUIPMENT LIST

Enter each single emission point that routes its emissions to another source (i.e., a control device) or a common stack, or is part of an Emissions Cap. List the emissions source to which each single emission point is routed or the Cap of which the source is a member, if applicable. Consult instructions.

Subject Item ID No:	Emission Point ID No:	Description	Construction Date	Routes to:	Operating Rate/Volume	Applicable Requirement(s)?	
						Yes	No
EQT 0001	1-22A	Plant 1 Amine Unit Vent		EQT 0009 (5-22 - Plant 1 Thermal Oxidizer)	150 MM scf/day		
EQT 0003	2-22A	Plant 1 Glycol Dehy Unit Vent		EQT 0009 (5-22 - Plant 1 Thermal Oxidizer)	150 MM scf/day		
EQT 0005	3-22A	Plant 2 Amine Unit Vent		EQT 0010 (6-22 - Plant 2 Thermal Oxidizer)	150 MM scf/day		
EQT 0007	4-22A	Plant 2 Glycol Dehy Unit Vent		EQT 0010 (6-22 - Plant 2 Thermal Oxidizer)	150 MM scf/day		
EQT 0015	11-22	Produced Water Tank		EQT 0023 (19-22 - Flare)	210,000 gallons/yr		
EQT 0016	12-22	Produced Water Tank		EQT 0023 (19-22 - Flare)	210,000 gallons/yr		
EQT 0017	13-22	Produced Water Tank		EQT 0023 (19-22 - Flare)	210,000 gallons/yr		
EQT 0018	14-22	Produced Water Tank		EQT 0023 (19-22 - Flare)	210,000 gallons/yr		

23. Emissions Inventory Questionnaire (EIQ) Forms [LAC 33:III.517.D.3; 517.D.6]³

Complete one (1) EIQ for:

- Each emission source. If two emission sources have a common stack, the applicant may submit one EIQ sheet for the common emissions point. Note any emissions sources that route to this common point in Table 4 of the application.
- Each emissions CAP that is proposed, including each source that is part of the CAP.
- Each alternate operating scenario that a source may operate under. Some common scenarios are:
 1. Sources that combust multiple fuels
 2. Sources that have startup/shutdown max lb/hr emission rates higher than the max lb/hr for normal operating conditions would need a separate EIQ addressing the startup/shutdown emission rates
- Fugitive emissions releases. One (1) EIQ should be completed for each of the following types of fugitive emissions sources or emissions points:
 1. Equipment leaks.
 2. Non-equipment leaks (i.e., road dust, settling ponds, etc).

For each EIQ:

- Fill in all requested information.
- Speciate all Toxic Air Pollutants and Hazardous Air Pollutants emitted by the source.
- Use appropriate significant figures.
- Consult instructions.

The EIQ is in Microsoft Word Excel. Visit the following website to get to the EIQ form.

<http://deq.louisiana.gov/page/air-permit-applications>

3: The included EIQ are only associated with those sources incorporated in 0760-01944-V0.

State of Louisiana								Date of submittal			
Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Jan 2024			
Emission Point ID No. (Designation)		Descriptive Name of the Emissions Source (Alt. Name)			Approximate Location of Stack or Vent (see instructions)						
1-22A		Plant 1 Amine Unit Vent			Method 18, "Interpolation - Map"			Datum WGS84			
Tempo Subject Item ID No.					UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN		
EQT 0001					Latitude 31°		51'		2" 65 hundredths		
					Longitude 93°		26'		54" 68 hundredths		
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	0.25 ft ft ²	10 ft	0.54 ft/sec	2 ft ³ /min	120 °F	1200 hr/yr	Jun 15 2023	25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel	Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description			
a				150		150		MM scf/day			
b				150				MM scf/day			
c								Design Capacity/Volume/Cylinder Displacement			
Notes These emissions are uncontrolled amine unit flash vent and acid gas vent during thermal oxidizer's planned/scheduled outage				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof		<input type="checkbox"/> Floating Roof		<input type="checkbox"/> External		<input type="checkbox"/> Internal	
				Date Engine Ordered				Engine Model Year			
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn		<input type="checkbox"/> Lean Burn		<input type="checkbox"/> 2 Stroke		<input type="checkbox"/> 4 Stroke	
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Total VOC (including those listed below)				0.04	0.04	0.02	0.01	C		ppm by vol	
Hydrogen sulfide			07783-06-4	14.03	14.03	8.42	5.05	C		ppm by vol	
n-Hexane			00110-54-3	0.01	0.01	<0.01	<0.01	U		ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal			
								Jan	2024		
Emission Point ID No. (Designation)	Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)						
1-22B	Plant 1 Amine Hot Oil Heater				Method <u>18, "Interpolation - Map"</u> Datum <u>WGS84</u>						
Tempo Subject Item ID No. EQT 0002					UTM Zone <u>15</u>	Horizontal <u>457565.87</u> mE	Vertical <u>3523978.64</u> mN				
					Latitude <u>31</u> °	<u>51</u> ' <u>2</u> "	<u>65</u> hundredths				
					Longitude <u>93</u> °	<u>26</u> ' <u>54</u> "	<u>68</u> hundredths				
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	<u>1</u> ft ft ²	<u>25</u> ft	<u>4.25</u> ft/sec	<u>200</u> ft ³ /min	<u>700</u> °F	<u>8760</u> hr/yr	Jun 15 2023	25%	25%	25%	25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
	a	Type of Fuel	Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter		Description			
		Natural Gas	85	85		85		MM BTU/hr			
				85		85		MM BTU/hr			
				Design Capacity/Volume/Cylinder Displacement							
				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof		<input type="checkbox"/> Floating Roof		<input type="checkbox"/> External		<input type="checkbox"/> Internal	
				Date Engine Ordered		Engine Model Year					
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn		<input type="checkbox"/> Lean Burn		<input type="checkbox"/> 2 Stroke		<input type="checkbox"/> 4 Stroke	
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
1-22B				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Pollutant											
Carbon monoxide				7.00	7.00	30.66	30.66	U		ppm by vol	
Nitrogen oxides				5.48	5.48	24.01	24.01	U		ppm by vol	
Particulate matter (PM ₁₀)				0.63	0.63	2.77	2.77	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.63	0.63	2.77	2.77	U		gr/std ft ³	
Sulfur dioxide				0.42	0.42	1.82	0.22	C		ppm by vol	
Total VOC (including those listed below)				0.46	0.46	2.01	2.01	U		ppm by vol	
Benzene			00071-43-2	<0.001	<0.001	<0.01	<0.01	U		ppm by vol	
Formaldehyde			00050-00-0	0.01	0.01	0.03	0.03	U		ppm by vol	

Emission Point ID No. (Designation) 1-22B	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
n-Hexane			00110-54-3	0.15	0.15	0.66	0.66	U		ppm by vol
Toluene			00108-88-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol

State of Louisiana

Emissions Inventory Questionnaire (EIQ) for Air Pollutants

Date of submittal
Jan | 2024

Emission Point ID No. (Designation) 2-22A	Descriptive Name of the Emissions Source (Alt. Name) Plant 1 Glycol Dehy Unit Vent	Approximate Location of Stack or Vent (see instructions)					
Tempo Subject Item ID No. EQT 0003		Method	18, "Interpolation - Map"		Datum	WGS84	
		UTM Zone	15	Horizontal	457565.87 mE	Vertical	3523978.64 mN
		Latitude	31 °		51 ' 2 "		65 hundredths
		Longitude	93 °		26 ' 54 "	68 hundredths	

Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft²) 0.25 ft ft ²	Height of Stack Above Grade (ft) 10 ft	Stack Gas Exit Velocity 0.54 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft³/min) 2 ft ³ /min	Stack Gas Exit Temperature (°F) 120 °F	Normal Operating Time (hours per year) 1200 hr/yr	Date of Construction or Modification Jun 15 2023	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
								25%	25%	25%	25%

Fuel	Type of Fuel Used and Heat Input (see instructions)	
	Type of Fuel	Heat Input (MMBTU/hr)
	a	
	b	
c		
Notes		
These emissions are uncontrolled glycol dehydration unit flash vent and BTEX vent during thermal oxidizer's planned/scheduled outage		

Operating Parameters (include units)		
	Parameter	Description
	Normal Operating Rate/Throughput	150 MM scf/day
	Maximum Operating Rate/Throughput	150 MM scf/day
	Design Capacity/Volume/Cylinder Displacement	
	Shell Height (ft)	
	Tank Diameter (ft)	
Tanks:	<input type="checkbox"/> Fixed Roof	<input type="checkbox"/> Floating Roof
	<input type="checkbox"/> External	<input type="checkbox"/> Internal
Date Engine Ordered		Engine Model Year
Date Engine Was Built by Manufacturer		
SI Engines:	<input type="checkbox"/> Rich Burn	<input type="checkbox"/> Lean Burn
	<input type="checkbox"/> 2 Stroke	<input type="checkbox"/> 4 Stroke

Emission Point ID No. (Designation) 2-22A	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Total VOC (including those listed below)				0.13	0.13	0.08	0.05	C		ppm by vol
n-Hexane			00110-54-3	0.10	0.10	0.06	0.03	C		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal			
								Jan	2024		
Emission Point ID No. (Designation)	Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)						
2-22B	Plant 1 Glycol Dehy Reboiler				Method 18, "Interpolation - Map" Datum WGS84						
Tempo Subject Item ID No.					UTM Zone 15	Horizontal 457565.87 mE	Vertical 3523978.64 mN				
EQT 0004					Latitude 31° 51' 2"	65 hundredths					
					Longitude 93° 26' 54"	68 hundredths					
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	1 ft	15 ft	4.25 ft/sec	200 ft ³ /min	700 °F	8760 hr/yr		25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)					Operating Parameters (include units)						
Fuel	Type of Fuel	Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter	Description				
	a	Natural Gas	5		Maximum Operating Rate/Throughput		5	MM BTU/hr			
	b				Design Capacity/Volume/Cylinder Displacement						
	c				Shell Height (ft)						
Notes				Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal					
				Date Engine Ordered		Engine Model Year					
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
2-22B				0.41	0.41	1.80	1.80	U		ppm by vol	
Carbon monoxide				0.32	0.32	1.41	1.41	U		ppm by vol	
Nitrogen oxides				0.04	0.04	0.16	0.16	U		gr/std ft ³	
Particulate matter (PM ₁₀)				0.04	0.04	0.16	0.16	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.02	0.02	0.11	0.01	C		ppm by vol	
Sulfur dioxide				0.03	0.03	0.12	0.12	U		ppm by vol	
Total VOC (including those listed below)				<0.001	<0.001	<0.01	0.01	U		ppm by vol	
Formaldehyde			00050-00-0	0.01	0.01	0.04	0.04	U		ppm by vol	
n-Hexane			00110-54-3							ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024			
Emission Point ID No. (Designation) 3-22A		Descriptive Name of the Emissions Source (Alt. Name) Plant 2 Amine Unit Vent			Approximate Location of Stack or Vent (see instructions)						
Tempo Subject Item ID No. EQT 0005					Method <u>18,"Interpolation - Map"</u> Datum <u>WGS84</u>		UTM Zone <u>15</u> Horizontal <u>457565.87</u> mE Vertical <u>3523978.64</u> mN		Latitude <u>31</u> ° <u>51</u> ' <u>2</u> " <u>65</u> hundredths		
		Longitude <u>93</u> ° <u>26</u> ' <u>54</u> " <u>68</u> hundredths									
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
<u>no</u>	<u>0.25</u> ft <u> </u> ft ²	<u>10</u> ft	<u>0.54</u> ft/sec	<u>2</u> ft ³ /min	<u>120</u> °F	<u>1200</u> hr/yr	Jun 15 2023	25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)								
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Parameter			Description			
	a				Normal Operating Rate/Throughput			150 MM scf/day			
	b				Maximum Operating Rate/Throughput			150 MM scf/day			
	c				Design Capacity/Volume/Cylinder Displacement						
Notes											
These emissions are uncontrolled amine unit flash vent and acid gas vent during thermal oxidizer's planned/scheduled outage											
			Shell Height (ft)								
			Tank Diameter (ft)								
			Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal								
			Date Engine Ordered						Engine Model Year		
			Date Engine Was Built by Manufacturer								
			SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke								
Emission Point ID No. (Designation) 3-22A		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Total VOC (including those listed below)					0.04	0.04	0.02	0.01	U		ppm by vol
Hydrogen sulfide				07783-06-4	14.03	14.03	8.42	5.05	C		ppm by vol
n-Hexane				00110-54-3	0.01	0.01	<0.01	<0.01	U		ppm by vol

State of Louisiana								Date of submittal						
Emissions Inventory Questionnaire (EIQ) for Air Pollutants												Jan 2024		
Emission Point ID No. (Designation)		Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)								
3-22B		Plant 2 Amine Hot Oil Heater				Method 18, "Interpolation - Map"			Datum WGS84					
Tempo Subject Item ID No.		Diameter (ft) or Stack Discharge Area (ft ²)		Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification		Percent of Annual Throughput Through This Emission Point			
EQT 0006		1 ft ft ²		25 ft	4.25 ft/sec	200 ft ³ /min	700 °F	8760 hr/yr	Jun 15 2023		Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no											25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)										
Fuel	Type of Fuel	Heat Input (MMBTU/hr)		Parameter				Description						
a	Natural Gas	85		Normal Operating Rate/Throughput				85 MM BTU/hr						
b				Maximum Operating Rate/Throughput				85 MM BTU/hr						
c				Design Capacity/Volume/Cylinder Displacement										
Notes				Shell Height (ft)										
				Tank Diameter (ft)										
				Tanks: <input type="checkbox"/> Fixed Roof		<input type="checkbox"/> Floating Roof		<input type="checkbox"/> External		<input type="checkbox"/> Internal				
				Date Engine Ordered				Engine Model Year						
				Date Engine Was Built by Manufacturer										
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke										
Emission Point ID No. (Designation)		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack			
3-22B					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)						
Pollutant														
Carbon monoxide					7.00	7.00	30.66	30.66	U	ppm by vol				
Nitrogen oxides					5.48	5.48	24.01	24.01	U	ppm by vol				
Particulate matter (PM ₁₀)					0.63	0.63	2.77	2.77	U	gr/std ft ³				
Particulate matter (PM _{2.5})					0.63	0.63	2.77	2.77	U	gr/std ft ³				
Sulfur dioxide					0.42	0.42	1.82	0.22	C	ppm by vol				
Total VOC (including those listed below)					0.46	0.46	2.01	2.01	U	ppm by vol				
Benzene				00071-43-2	<0.001	<0.001	<0.01	<0.01	U	ppm by vol				
Formaldehyde				00050-00-0	0.01	0.01	0.03	0.03	U	ppm by vol				

Emission Point ID No. (Designation) 3-22B	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
n-Hexane			00110-54-3	0.15	0.15	0.66	0.66	U		ppm by vol
Toluene			00108-88-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal Jan 2024	
Emission Point ID No. (Designation) 4-22A		Descriptive Name of the Emissions Source (Alt. Name) Plant 2 Glycol Dehy Unit Vent				Approximate Location of Stack or Vent (see instructions)					
Tempo Subject Item ID No. EQT 0007						Method 18, "Interpolation - Map"		Datum WGS84			
						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
						Latitude 31 °		51'		2" 65 hundredths	
						Longitude 93 °		26'		54" 68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 0.25 ft	Height of Stack Above Grade (ft) 10 ft	Stack Gas Exit Velocity 0.54 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft ³ /min) 2 ft ³ /min	Stack Gas Exit Temperature (°F) 120 °F	Normal Operating Time (hours per year) 1200 hr/yr	Date of Construction or Modification Jun 15 2023	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar 25%	Apr-Jun 25%	Jul-Sep 25%	Oct-Dec 25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description		
	a				150				MM scf/day		
	b				150				MM scf/day		
	c				Design Capacity/Volume/Cylinder Displacement						
Notes These emissions are uncontrolled glycol dehydration unit flash vent and BTEX vent during thermal oxidizer's planned/scheduled outage				Shell Height (ft)		Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal			
				Date Engine Ordered		Engine Model Year		Date Engine Was Built by Manufacturer			
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation) 4-22A		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current) Annual (tons/yr)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Total VOC (including those listed below)					0.13	0.13	0.08	0.05	C		ppm by vol
n-Hexane				00110-54-3	0.10	0.10	0.06	0.03	C		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024				
Emission Point ID No. (Designation) 4-22B		Descriptive Name of the Emissions Source (Alt. Name) Plant 2 Glycol Dehy Reboiler			Approximate Location of Stack or Vent (see instructions)							
Tempo Subject Item ID No. EQT 0008					Method	18, "Interpolation - Map"		Datum NAD83				
					UTM Zone	15	Horizontal	457565.87 mE	Vertical	3523978.64 mN		
					Latitude	31 °	51 '	2 "	65 hundredths			
					Longitude	93 °	26 '	54 "	68 hundredths			
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point				
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec	
no	1 ft	15 ft	4.25 ft/sec	200 ft ³ /min	700 °F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%	
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)								
	a	b	c	Type of Fuel	Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description			
				Natural Gas	5	5		5	MM BTU/hr			
						Maximum Operating Rate/Throughput			MM BTU/hr			
						Design Capacity/Volume/Cylinder Displacement						
						Shell Height (ft)						
						Tank Diameter (ft)						
						Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal						
						Date Engine Ordered			Engine Model Year			
						Date Engine Was Built by Manufacturer						
						SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke						
Emission Point ID No. (Designation)		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)					Annual (tons/yr)
4-22B												
Carbon monoxide					0.41	0.41	1.80	1.80	U		ppm by vol	
Nitrogen oxides					0.32	0.32	1.41	1.41	U		ppm by vol	
Particulate matter (PM ₁₀)					0.04	0.04	0.16	0.16	U		gr/std ft ³	
Particulate matter (PM _{2.5})					0.04	0.04	0.16	0.16	U		gr/std ft ³	
Sulfur dioxide					0.02	0.02	0.11	0.01	C		ppm by vol	
Total VOC (including those listed below)					0.03	0.03	0.12	0.12	U		ppm by vol	
Formaldehyde				00050-00-0	<0.001	<0.001	<0.01	0.01	U		ppm by vol	
n-Hexane				00110-54-3	0.01	0.01	0.04	0.04	U		ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal	
										Jan	2024
Emission Point ID No. (Designation) 5-22		Descriptive Name of the Emissions Source (Alt. Name) Plant 1 Thermal Oxidizer				Approximate Location of Stack or Vent (see instructions)					
Tempo Subject Item ID No. EQT 0009						Method 18, "Interpolation - Map"		Datum WGS84			
						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
						Latitude 31° 51' 2"		Longitude 93° 26' 54"		65 hundredths 68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 3 ft	Height of Stack Above Grade (ft) 48 ft	Stack Gas Exit Velocity 21.61 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft ³ /min) 9,160 ft ³ /min	Stack Gas Exit Temperature (°F) 1,500 °F	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification Jun 15 2023	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
								25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput			Parameter		Description	
	a		33					33		MM BTU/hr	
	b				Maximum Operating Rate/Throughput			33		MM BTU/hr	
	c				Design Capacity/Volume/Cylinder Displacement						
Notes				Shell Height (ft)			Tank Diameter (ft)				
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal			Date Engine Ordered		Engine Model Year		
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation) 5-22		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Carbon monoxide					2.72	2.72	11.9	11.90	U		ppm by vol
Nitrogen oxides					2.13	2.13	9.32	9.32	U		ppm by vol
Particulate matter (PM ₁₀)					0.25	0.25	1.08	1.08	U		gr/std ft ³
Particulate matter (PM _{2.5})					0.25	0.25	1.08	1.08	U		gr/std ft ³
Sulfur dioxide					26.04	26.04	114.05	113.42	C		ppm by vol
Total VOC (including those listed below)					0.18	0.18	0.79	0.79	U		ppm by vol
Hydrogen sulfide				07783-06-4	0.28	0.28	1.23	1.23	U		ppm by vol
n-Hexane				00110-54-3	0.06	0.06	0.26	0.26	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal			
								Jan	2024		
Emission Point ID No. (Designation)	Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)						
6-22	Plant 2 Thermal Oxidizer				Method <u>18,"Interpolation - Map"</u> Datum <u>WGS84</u> UTM Zone <u>15</u> Horizontal <u>457565.87</u> mE Vertical <u>3523978.64</u> mN Latitude <u>31</u> ° <u>51</u> ' <u>2</u> " <u>65</u> hundredths Longitude <u>93</u> ° <u>26</u> ' <u>54</u> " <u>68</u> hundredths						
Tempo Subject Item ID No.	EQT 0010										
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	3 ft ft ²	48 ft	21.61 ft/sec	9,160 ft ³ /min	1,500 °F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
	Type of Fuel	Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description			
a		33		33		33		MM BTU/hr			
b				33		33		MM BTU/hr			
c				Design Capacity/Volume/Cylinder Displacement							
Notes				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal							
				Date Engine Ordered				Engine Model Year			
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				2.72	2.72	11.9	11.90	U		ppm by vol	
Nitrogen oxides				2.13	2.13	9.32	9.32	U		ppm by vol	
Particulate matter (PM ₁₀)				0.25	0.25	1.08	1.08	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.25	0.25	1.08	1.08	U		gr/std ft ³	
Sulfur dioxide				26.04	26.04	114.05	113.42	C		ppm by vol	
Total VOC (including those listed below)				0.18	0.18	0.79	0.79	U		ppm by vol	
Hydrogen sulfide			07783-06-4	0.28	0.28	1.23	1.23	U		ppm by vol	
n-Hexane			00110-54-3	0.06	0.06	0.26	0.26	U		ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal Jan 2024	
Emission Point ID No. (Designation) 7-22		Descriptive Name of the Emissions Source (Alt. Name) CAT G3606 Compressor Engine				Approximate Location of Stack or Vent (see instructions)					
Tempo Subject Item ID No. EQT 0011						Method 18,"Interpolation - Map"		Datum WGS84			
		UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN		Latitude 31° 51' 2"		Longitude 93° 26' 54"	
		65 hundredths		68 hundredths							
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 1.67 ft	Height of Stack Above Grade (ft) 29 ft	Stack Gas Exit Velocity 90.17 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft ³ /min) 11,803 ft ³ /min	Stack Gas Exit Temperature (°F) 835 °F	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification Jun 15 2023	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar 25%	Apr-Jun 25%	Jul-Sep 25%	Oct-Dec 25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
	Type of Fuel		Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description				
	a		Natural Gas	1875		1875	HP				
	b										
c					Design Capacity/Volume/Cylinder Displacement						
Notes											
			Shell Height (ft)		Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal				
			Date Engine Ordered		Engine Model Year		Date Engine Was Built by Manufacturer				
			SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke								
Emission Point ID No. (Designation) 7-22		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current) Annual (tons/yr)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Carbon monoxide					0.64	0.64	2.79	2.79	U	ppm by vol	
Nitrogen oxides					2.07	2.07	9.05	9.05	U		
Particulate matter (PM ₁₀)					0.14	0.14	0.62	0.62	U	gr/std ft ³	
Particulate matter (PM _{2.5})					0.14	0.14	0.62	0.62	U	gr/std ft ³	
Sulfur dioxide					0.07	0.07	0.3	0.04	C	ppm by vol	
Total VOC (including those listed below)					0.85	0.85	3.71	3.71	U	ppm by vol	
1,1,2,2-Tetrachloroethane				00079-34-5	<0.001	<0.001	<0.01	<0.01	U	ppm by vol	
1,1,2-Trichloroethane				00079-00-5	<0.001	<0.001	<0.01	<0.01	U	ppm by vol	
1,2-Dibromoethane				00106-93-4	<0.001	<0.001	<0.01	<0.01	U	ppm by vol	

Emission Point ID No. (Designation) 7-22	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
1,3-Butadiene			00106-99-0	0.002	0.002	0.01	0.01	U		ppm by vol
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	<0.01	<0.01	U		ppm by vol
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Acetaldehyde			00075-07-0	0.06	0.06	0.26	0.26	U		ppm by vol
Acrolein			00107-02-8	0.036	0.04	0.16	0.16	U		ppm by vol
Benzene			00071-43-2	0.003	0.003	0.01	0.01	U		ppm by vol
Biphenyl			00092-52-4	0.002	0.002	0.01	0.01	U		ppm by vol
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chloroform			00067-66-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Formaldehyde			00050-00-0	0.25	0.25	1.09	1.09	U		ppm by vol
Methanol			00067-56-1	0.02	0.02	0.08	0.08	U		ppm by vol
n-Hexane			00110-54-3	0.01	0.01	0.04	0.03	U		ppm by vol
Naphthalene			00091-20-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Styrene			00100-42-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Toluene			00108-88-3	0.003	0.003	0.01	0.01	U		ppm by vol
Xylene (mixed isomers)			01330-20-7	0.001	0.001	0.01	0.01	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal	
										Jan	2024
Emission Point ID No. (Designation)		Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)					
8-22		CAT G3606 Compressor Engine				Method 18, "Interpolation - Map"		Datum WGS84			
Tempo Subject Item ID No.						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
EQT 0012						Latitude 31° 51' 2"		Longitude 93° 26' 54"		65 hundredths	
										68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	1.67 ft	29 ft	90.17 ft/sec	11,803 ft ³ /min	835 °F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel	Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description			
a	Natural Gas			1875		1875		HP			
b								HP			
c				Design Capacity/Volume/Cylinder Displacement							
Notes				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal							
				Date Engine Ordered				Engine Model Year			
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
8-22				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				0.64	0.64	2.79	2.79	U		ppm by vol	
Nitrogen oxides				2.07	2.07	9.05	9.05	U		ppm by vol	
Particulate matter (PM ₁₀)				0.14	0.14	0.62	0.62	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.14	0.14	0.62	0.62	U		gr/std ft ³	
Sulfur dioxide				0.07	0.07	0.3	0.04	C		ppm by vol	
Total VOC (including those listed below)				0.85	0.85	3.71	3.71	U		ppm by vol	
1,1,2,2-Tetrachloroethane			00079-34-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol	
1,1,2-Trichloroethane			00079-00-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol	

Emission Point ID No. (Designation) 8-22	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
1,2-Dibromoethane			00106-93-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
1,3-Butadiene			00106-99-0	0.002	0.002	0.01	0.01	U		ppm by vol
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	<0.01	<0.01	U		ppm by vol
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Acetaldehyde			00075-07-0	0.06	0.06	0.26	0.26	U		ppm by vol
Acrolein			00107-02-8	0.036	0.04	0.16	0.16	U		ppm by vol
Benzene			00071-43-2	0.003	0.003	0.01	0.01	U		ppm by vol
Biphenyl			00092-52-4	0.002	0.002	0.01	0.01	U		ppm by vol
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chloroform			00067-66-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Formaldehyde			00050-00-0	0.25	0.25	1.09	1.09	U		ppm by vol
Methanol			00067-56-1	0.02	0.02	0.08	0.08	U		ppm by vol
n-Hexane			00110-54-3	0.01	0.01	0.04	0.03	U		ppm by vol
Naphthalene			00091-20-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Styrene			00100-42-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Toluene			00108-88-3	0.003	0.003	0.01	0.01	U		ppm by vol
Xylene (mixed isomers)			01330-20-7	0.001	0.001	0.01	0.01	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024				
Emission Point ID No. (Designation) 9-22		Descriptive Name of the Emissions Source (Alt. Name) CAT G3606 Compressor Engine			Approximate Location of Stack or Vent (see instructions)							
Tempo Subject Item ID No. EQT 0013					Method	18, "Interpolation - Map"		Datum WGS84				
					UTM Zone	15	Horizontal	457565.87	mE	Vertical	3523978.64	mN
					Latitude	31°		51'		2"	65	hundredths
					Longitude	93°		26'		54"	68	hundredths
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point				
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec	
no	1.67 ft	29 ft	90.17 ft/sec	11,803 ft ³ /min	835 °F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%	
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)								
		Type of Fuel	Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description					
	a	Natural Gas		1875		1875	HP					
	b											
c												
Notes				Shell Height (ft)		Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal				
				Date Engine Ordered		Engine Model Year		Date Engine Was Built by Manufacturer				
				SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke								
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack		
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)					
Carbon monoxide				0.64	0.64	2.79	2.79	U		ppm by vol		
Nitrogen oxides				2.07	2.07	9.05	9.05	U		ppm by vol		
Particulate matter (PM ₁₀)				0.14	0.14	0.62	0.62	U		gr/std ft ³		
Particulate matter (PM _{2.5})				0.14	0.14	0.62	0.62	U		gr/std ft ³		
Sulfur dioxide				0.07	0.07	0.3	0.04	C		ppm by vol		
Total VOC (including those listed below)				0.85	0.85	3.71	3.71	U		ppm by vol		
1,1,2,2-Tetrachloroethane			00079-34-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol		
1,1,2-Trichloroethane			00079-00-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol		

Emission Point ID No. (Designation) 9-22	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
1,2-Dibromoethane			00106-93-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
1,3-Butadiene			00106-99-0	0.002	0.002	0.01	0.01	U		ppm by vol
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	<0.01	<0.01	U		ppm by vol
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Acetaldehyde			00075-07-0	0.06	0.06	0.26	0.26	U		ppm by vol
Acrolein			00107-02-8	0.036	0.04	0.16	0.16	U		ppm by vol
Benzene			00071-43-2	0.003	0.003	0.01	0.01	U		ppm by vol
Biphenyl			00092-52-4	0.002	0.002	0.01	0.01	U		ppm by vol
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chloroform			00067-66-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Formaldehyde			00050-00-0	0.25	0.25	1.09	1.09	U		ppm by vol
Methanol			00067-56-1	0.02	0.02	0.08	0.08	U		ppm by vol
n-Hexane			00110-54-3	0.01	0.01	0.04	0.03	U		ppm by vol
Naphthalene			00091-20-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Styrene			00100-42-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Toluene			00108-88-3	0.003	0.003	0.01	0.01	U		ppm by vol
Xylene (mixed isomers)			01330-20-7	0.001	0.001	0.01	0.01	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal Jan 2024	
Emission Point ID No. (Designation) 10-22		Descriptive Name of the Emissions Source (Alt. Name) CAT G3606 Compressor Engine				Approximate Location of Stack or Vent (see instructions)					
Tempo Subject Item ID No. EQT 0014						Method 18, "Interpolation - Map"		Datum WGS84			
						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
						Latitude 31° 51' 2"		Longitude 93° 26' 54"			
						Longitude 93° 26' 54"					
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 1.67 ft	Height of Stack Above Grade (ft) 29 ft	Stack Gas Exit Velocity 90.17 ft/sec	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min) 11,803 ft ³ /min	Stack Gas Exit Temperature (°F) 835 °F	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification Jun 15 2023	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
							25%	25%	25%	25%	
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description		
	a	Natural Gas			1875		1875		HP		
	b								HP		
	c										
Notes				Design Capacity/Volume/Cylinder Displacement		Shell Height (ft)		Tank Diameter (ft)			
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal		Date Engine Ordered		Engine Model Year			
				Date Engine Was Built by Manufacturer		SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke					
Emission Point ID No. (Designation) 10-22	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				0.64	0.64	2.79	2.79	U		ppm by vol	
Nitrogen oxides				2.07	2.07	9.05	9.05	U		ppm by vol	
Particulate matter (PM ₁₀)				0.14	0.14	0.62	0.62	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.14	0.14	0.62	0.62	U		gr/std ft ³	
Sulfur dioxide				0.07	0.07	0.3	0.04	C		ppm by vol	
Total VOC (including those listed below)				0.85	0.85	3.71	3.71	U		ppm by vol	
1,1,2,2-Tetrachloroethane			00079-34-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol	
1,1,2-Trichloroethane			00079-00-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol	

Emission Point ID No. (Designation) 10-22	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
1,2-Dibromoethane			00106-93-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
1,3-Butadiene			00106-99-0	0.002	0.002	0.01	0.01	U		ppm by vol
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	<0.01	<0.01	U		ppm by vol
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Acetaldehyde			00075-07-0	0.06	0.06	0.26	0.26	U		ppm by vol
Acrolein			00107-02-8	0.036	0.04	0.16	0.16	U		ppm by vol
Benzene			00071-43-2	0.003	0.003	0.01	0.01	U		ppm by vol
Biphenyl			00092-52-4	0.002	0.002	0.01	0.01	U		ppm by vol
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Chloroform			00067-66-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Formaldehyde			00050-00-0	0.25	0.25	1.09	1.09	U		ppm by vol
Methanol			00067-56-1	0.02	0.02	0.08	0.08	U		ppm by vol
n-Hexane			00110-54-3	0.01	0.01	0.04	0.03	U		ppm by vol
Naphthalene			00091-20-3	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Styrene			00100-42-5	<0.001	<0.001	<0.01	<0.01	U		ppm by vol
Toluene			00108-88-3	0.003	0.003	0.01	0.01	U		ppm by vol
Xylene (mixed isomers)			01330-20-7	0.001	0.001	0.01	0.01	U		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal	
										Jan	2024
Emission Point ID No. (Designation)		Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)					
19-22		Flare				Method 18, "Interpolation - Map" Datum WGS84					
Tempo Subject Item ID No.						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
EQT 0023						Latitude 31° 51' 10"		Longitude 93° 26' 54"		11 hundredths 68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	6.8 ft	45 ft	66.00 ft/sec	ft ³ /min	1,832 °F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description		
	a				17.3		17.3		MM BTU/hr		
	b								MM BTU/hr		
	c										
Notes				Shell Height (ft)		Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal		Date Engine Ordered	
				Date Engine Was Built by Manufacturer		SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke		Engine Model Year			
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				0.01	1.42	0.04	0.04	U		ppm by vol	
Nitrogen oxides				0.01	1.69	0.05	0.05	U		ppm by vol	
Particulate matter (PM ₁₀)				0.001	0.13	<0.01	<0.01	U		gr/std ft ³	
Particulate matter (PM _{2.5})				0.001	0.13	<0.01	<0.01	U		gr/std ft ³	
Sulfur dioxide				0.001	0.08	<0.01	<0.01	C		ppm by vol	
Total VOC (including those listed below)				0.001	0.09	<0.01	<0.01	U		ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024			
Emission Point ID No. (Designation) FUG		Descriptive Name of the Emissions Source (Alt. Name) Fugitive Emissions			Approximate Location of Stack or Vent (see instructions)						
Tempo Subject Item ID No. FUG 0001					Method 28,"GPS-Unspecified" Datum NAD83		UTM Zone 15 Horizontal 457565.87 mE Vertical 3523978.64 mN				
					Latitude 31° 51' 2" 65 hundredths		Longitude 93° 26' 5254" 68 hundredths				
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	ft	ft	ft/sec	ft ³ /min	°F	8760 hr/yr	Jun 15 2023	25%	25%	25%	25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
	Type of Fuel		Heat Input (MMBTU/hr)	Parameter		Description					
	a			Normal Operating Rate/Throughput							
	b			Maximum Operating Rate/Throughput							
c			Design Capacity/Volume/Cylinder Displacement								
Notes											
Shell Height (ft)											
Tank Diameter (ft)											
Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal											
Date Engine Ordered _____ Engine Model Year _____											
Date Engine Was Built by Manufacturer _____											
SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke											
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Total VOC (including those listed below)				0.31	0.31	1.35	4.69	C		ppm by vol	
Benzene			00071-43-2	0.01	0.01	0.07		A		ppm by vol	
Ethyl benzene			00100-41-4	0.01	0.01	0.07		A		ppm by vol	
Hydrogen sulfide			07783-06-4	<0.001	<0.001	<0.01		A		ppm by vol	
Toluene			00108-88-3	0.02	0.02	0.07		A		ppm by vol	
Xylene (mixed isomers)			01330-20-7	0.02	0.02	0.07		A		ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal			
								Jan	2024		
Emission Point ID No. (Designation) 1-23		Descriptive Name of the Emissions Source (Alt. Name) Caterpillar G3608A4 (w/ Oxidation Catalyst)			Approximate Location of Stack or Vent (see instructions)						
Tempo Subject Item ID No. EQT TBD1					Method 18, "Interpolation - Map"		Datum WGS84				
					UTM Zone 15	Horizontal 457565.87 mE	Vertical 3523978.64 mN				
					Latitude 31° 51' 2"	Longitude 93° 26' 54"		65 hundredths 68 hundredths			
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft²) 0 ft ft ²	Height of Stack Above Grade (ft) 0 ft	Stack Gas Exit Velocity 0.00 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft³/min) ft ³ /min	Stack Gas Exit Temperature (°F) °F	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification proposed	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar 25%	Apr-Jun 25%	Jul-Sep 25%	Oct-Dec 25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
	a	Type of Fuel	Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description				
b	Natural Gas		2500		2500	HP					
c			2500			HP					
Notes				Design Capacity/Volume/Cylinder Displacement							
				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal							
				Date Engine Ordered		Engine Model Year					
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation) 1-23	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				0.88	0.88	3.86		A		ppm by vol	
Nitrogen oxides				1.65	1.65	7.24		A		ppm by vol	
Particulate matter (PM ₁₀)				0.19	0.19	0.83		A		gr/std ft ³	
Particulate matter (PM _{2.5})				0.19	0.19	0.83		A		gr/std ft ³	
Sulfur dioxide				0.09	0.09	0.41		A		ppm by vol	
Total VOC (including those listed below)				0.50	0.50	2.17		A		ppm by vol	
1,1,2,2-Tetrachloroethane			00079-34-5	<0.001	<0.001	<0.01		A		ppm by vol	
1,1,2-Trichloroethane			00079-00-5	<0.001	<0.001	<0.01		A		ppm by vol	

Emission Point ID No. (Designation) 1-23	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
Pollutant										
1,1-Dichloroethane			00075-34-3	<0.001	<0.001	<0.01		A		ppm by vol
1,2-Dibromoethane			00106-93-4	<0.001	<0.001	<0.01		A		ppm by vol
1,2-Dichloroethane			00107-06-2	<0.001	<0.001	<0.01		A		ppm by vol
1,2-Dichloropropane			00078-87-5	<0.001	<0.001	<0.01		A		ppm by vol
1,3-Butadiene			00106-99-0	0.003	0.003	0.01		A		ppm by vol
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01		A		ppm by vol
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	0.01		A		ppm by vol
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01		A		ppm by vol
Acetaldehyde			00075-07-0	0.08	0.08	0.35		A		ppm by vol
Acrolein			00107-02-8	0.049	0.05	0.213		A		ppm by vol
Benzene			00071-43-2	0.004	0.004	0.02		A		ppm by vol
Biphenyl			00092-52-4	0.002	0.002	0.01		A		ppm by vol
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01		A		ppm by vol
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01		A		ppm by vol
Chloroform			00067-66-3	<0.001	<0.001	<0.01		A		ppm by vol
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01		A		ppm by vol
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01		A		ppm by vol
Formaldehyde			00050-00-0	0.11	0.11	0.48		A		ppm by vol
Methanol			00067-56-1	0.02	0.02	0.10		A		ppm by vol
n-Hexane			00110-54-3	0.01	0.01	0.05		A		ppm by vol
Naphthalene			00091-20-3	<0.001	<0.001	<0.01		A		ppm by vol
Styrene			00100-42-5	<0.001	<0.001	<0.01		A		ppm by vol
Toluene			00108-88-3	0.004	0.004	0.01		A		ppm by vol
Vinyl chloride			00075-01-4	<0.001	<0.001	<0.01		A		ppm by vol
Xylene (mixed isomers)			01330-20-7	0.002	0.002	0.01		A		ppm by vol

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024			
Emission Point ID No. (Designation) 2-23		Descriptive Name of the Emissions Source (Alt. Name) Caterpillar G3608A4 (w/ Oxidation Catalyst)			Approximate Location of Stack or Vent (see instructions)						
Tempo Subject Item ID No. EQT TBD2					Method 18, "Interpolation - Map"		Datum WGS84				
					UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN		
					Latitude 31°		51'		2" 65 hundredths		
					Longitude 93°		26'		54" 68 hundredths		
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 0 ft	Height of Stack Above Grade (ft) 0 ft	Stack Gas Exit Velocity 0.00 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification proposed	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar 25%	Apr-Jun 25%	Jul-Sep 25%	Oct-Dec 25%
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)							
		Type of Fuel	Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description				
	a	Natural Gas		2500			HP				
	b			2500			HP				
c			Design Capacity/Volume/Cylinder Displacement								
Notes				Shell Height (ft)							
				Tank Diameter (ft)							
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal							
				Date Engine Ordered		Engine Model Year					
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input checked="" type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input checked="" type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation) 2-23	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack	
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)				
Carbon monoxide				0.88	0.88	3.86		A		ppm by vol	
Nitrogen oxides				1.65	1.65	7.24		A		ppm by vol	
Particulate matter (PM ₁₀)				0.19	0.19	0.83		A		gr/std ft ³	
Particulate matter (PM _{2.5})				0.19	0.19	0.83		A		gr/std ft ³	
Sulfur dioxide				0.09	0.09	0.41		A		ppm by vol	
Total VOC (including those listed below)				0.50	0.50	2.17		A		ppm by vol	
1,1,2,2-Tetrachloroethane			00079-34-5	<0.001	<0.001	<0.01		A		ppm by vol	
1,1,2-Trichloroethane			00079-00-5	<0.001	<0.001	<0.01		A		ppm by vol	

Emission Point ID No. (Designation) 2-23	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
1,1-Dichloroethane			00075-34-3	<0.001	<0.001	<0.01		A	ppm by vol	
1,2-Dibromoethane			00106-93-4	<0.001	<0.001	<0.01		A	ppm by vol	
1,2-Dichloroethane			00107-06-2	<0.001	<0.001	<0.01		A	ppm by vol	
1,2-Dichloropropane			00078-87-5	<0.001	<0.001	<0.01		A	ppm by vol	
1,3-Butadiene			00106-99-0	0.003	0.003	0.01		A	ppm by vol	
1,3-Dichloropropene			00542-75-6	<0.001	<0.001	<0.01		A	ppm by vol	
2,2,4-Trimethylpentane			00540-84-1	0.002	0.002	0.01		A	ppm by vol	
2-Methylnaphthalene			00091-57-6	<0.001	<0.001	<0.01		A	ppm by vol	
Acetaldehyde			00075-07-0	0.08	0.08	0.35		A	ppm by vol	
Acrolein			00107-02-8	0.049	0.05	0.21		A	ppm by vol	
Benzene			00071-43-2	0.004	0.004	0.02		A	ppm by vol	
Biphenyl			00092-52-4	0.002	0.002	0.01		A	ppm by vol	
Carbon tetrachloride			00056-23-5	<0.001	<0.001	<0.01		A	ppm by vol	
Chlorobenzene			00108-90-7	<0.001	<0.001	<0.01		A	ppm by vol	
Chloroform			00067-66-3	<0.001	<0.001	<0.01		A	ppm by vol	
Dichloromethane			00075-09-2	<0.001	<0.001	<0.01		A	ppm by vol	
Ethyl benzene			00100-41-4	<0.001	<0.001	<0.01		A	ppm by vol	
Formaldehyde			00050-00-0	0.11	0.11	0.48		A	ppm by vol	
Methanol			00067-56-1	0.02	0.02	0.10		A	ppm by vol	
n-Hexane			00110-54-3	0.01	0.01	0.05		A	ppm by vol	
Naphthalene			00091-20-3	<0.001	<0.001	<0.01		A	ppm by vol	
Styrene			00100-42-5	<0.001	<0.001	<0.01		A	ppm by vol	
Toluene			00108-88-3	0.004	0.004	0.01		A	ppm by vol	
Vinyl chloride			00075-01-4	<0.001	<0.001	<0.01		A	ppm by vol	
Xylene (mixed isomers)			01330-20-7	0.002	0.002	0.01		A	ppm by vol	

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024				
Emission Point ID No. (Designation) 3-23		Descriptive Name of the Emissions Source (Alt. Name) Sulfur Loading and Handling			Approximate Location of Stack or Vent (see instructions)							
Tempo Subject Item ID No. EQT TBD3					Method 18,"Interpolation - Map" Datum WGS84		UTM Zone 15 Horizontal 457565.87 mE Vertical 3523978.64 mN		Latitude 31 ° 51 ' 2 " 65 hundredths		Longitude 93 ° 26 ' 54 " 68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, <u>not</u> at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point				
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec	
no	0 ft	0 ft	0.00 ft/sec	ft ³ /min	°F	8760 hr/yr	proposed	25%	25%	25%	25%	
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)								
	Type of Fuel	Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description				
a				182.5		182.5		tons/yr				
b								tons/yr				
c				Design Capacity/Volume/Cylinder Displacement								
Notes				Shell Height (ft)								
				Tank Diameter (ft)								
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal								
				Date Engine Ordered		Engine Model Year						
				Date Engine Was Built by Manufacturer								
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke								
Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack		
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)					
Particulate matter (PM ₁₀)				<0.01	<0.01	<0.01		A		gr/std ft ³		
Particulate matter (PM _{2.5})				<0.01	<0.01	<0.01		A		gr/std ft ³		

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants								Date of submittal Jan 2024			
Emission Point ID No. (Designation) 5-23B		Descriptive Name of the Emissions Source (Alt. Name) CO2 Dehydrator Reboiler			Approximate Location of Stack or Vent (see instructions)						
Tempo Subject Item ID No. EQT TBD4					Method 18, "Interpolation - Map"		Datum WGS84				
					UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN		
					Latitude 31 °		51'		2"		
					Longitude 93 °		26'		54"		
Stack and Discharge Physical Characteristics Change? (yes or no) no	Diameter (ft) or Stack Discharge Area (ft ²) 0 ft	Height of Stack Above Grade (ft) 0 ft	Stack Gas Exit Velocity 0.00 ft/sec	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year) 8760 hr/yr	Date of Construction or Modification proposed	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar 25%	Apr-Jun 25%	Jul-Sep 25%	Oct-Dec 25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description		
	a	Natural Gas	1		1		1		MM BTU/hr		
	b								MM BTU/hr		
c											
Notes				Design Capacity/Volume/Cylinder Displacement Shell Height (ft) Tank Diameter (ft) Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal Date Engine Ordered _____ Engine Model Year _____ Date Engine Was Built by Manufacturer _____ SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation) 5-23B		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current) Annual (tons/yr)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Carbon monoxide					0.08	0.08	0.36		A	ppm by vol	
Nitrogen oxides					0.1	0.10	0.43		A	ppm by vol	
Particulate matter (PM ₁₀)					0.01	0.01	0.03		A	gr/std ft ³	
Particulate matter (PM _{2.5})					0.01	0.01	0.03		A	gr/std ft ³	
Sulfur dioxide					<0.01	<0.01	0.02		A	ppm by vol	
Total VOC (including those listed below)					0.01	0.01	0.02		A	ppm by vol	
n-Hexane				00110-54-3	0.002	0.002	0.01		A	ppm by vol	

State of Louisiana										Date of submittal			
Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Jan 2024			
Emission Point ID No. (Designation) 6-23		Descriptive Name of the Emissions Source (Alt. Name) Carbon Capture Produced Water Storage Tank: 750 bbl				Approximate Location of Stack or Vent (see instructions)							
Tempo Subject Item ID No. EQT TBD5						Method 18, "Interpolation - Map" Datum WGS84				UTM Zone 15 Horizontal 457565.87 mE Vertical 3523978.64 mN			
						Latitude 31° 51' 2"		Longitude 93° 26' 54"		65 hundredths		68 hundredths	
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point					
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec		
no	0 ft	0 ft	0.00 ft/sec	ft ³ /min	°F	8760 hr/yr	proposed	25%	25%	25%	25%		
Fuel	Type of Fuel Used and Heat Input (see instructions)			Operating Parameters (include units)									
	Type of Fuel		Heat Input (MMBTU/hr)	Normal Operating Rate/Throughput		Parameter	Description						
	a			3076920		3076920	gal/yr						
	b			3076920		750	gal/yr						
Notes				Design Capacity/Volume/Cylinder Displacement		22.06	ft						
				Shell Height (ft)		18	ft						
				Tank Diameter (ft)		Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal							
				Date Engine Ordered		Date Engine Was Built by Manufacturer		Engine Model Year					
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke									
Emission Point ID No. (Designation) 6-23		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack		
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)						Annual (tons/yr)
Total VOC (including those listed below)					0.04	0.04	0.18		A	ppm by vol			

Emission Point ID No. (Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)			
6-23										

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal Jan 2024											
Emission Point ID No. (Designation) 7-23		Descriptive Name of the Emissions Source (Alt. Name) Carbon Capture Produced Water Storage Tank: 750 bbl				Approximate Location of Stack or Vent (see instructions)															
Tempo Subject Item ID No. EQT TBD6						Method 18, "Interpolation - Map"		Datum WGS84													
						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN											
						Latitude 31 °		51'		2"											
						Longitude 93 °		26'		54"											
Stack and Discharge Physical Characteristics Change? (yes or no) no		Diameter (ft) or Stack Discharge Area (ft ²) 0 ft		Height of Stack Above Grade (ft) 0 ft		Stack Gas Exit Velocity 0.00 ft/sec		Stack Gas Flow at Conditions, not at Standard (ft ³ /min)		Stack Gas Exit Temperature (°F)		Normal Operating Time (hours per year) 8760 hr/yr		Date of Construction or Modification 		Percent of Annual Throughput Through This Emission Point					
												proposed		Jan-Mar 25%		Apr-Jun 25%		Jul-Sep 25%		Oct-Dec 25%	
Type of Fuel Used and Heat Input (see instructions)										Operating Parameters (include units)											
Fuel		Type of Fuel				Heat Input (MMBTU/hr)				Normal Operating Rate/Throughput		Parameter		Description							
a										3076920				gal/yr							
b										3076920				gal/yr							
c										750				bbl							
Notes										Design Capacity/Volume/Cylinder Displacement		22.06		ft							
										Shell Height (ft)		18		ft							
										Tank Diameter (ft)											
										Tanks: <input type="checkbox"/> Fixed Roof		<input type="checkbox"/> Floating Roof		<input type="checkbox"/> External		<input type="checkbox"/> Internal					
										Date Engine Ordered				Engine Model Year							
										Date Engine Was Built by Manufacturer											
										SI Engines: <input type="checkbox"/> Rich Burn		<input type="checkbox"/> Lean Burn		<input type="checkbox"/> 2 Stroke		<input type="checkbox"/> 4 Stroke					
Emission Point ID No. (Designation) 7-23		Control Equipment Code		Control Equipment Efficiency		HAP / TAP CAS Number		Proposed Emission Rates			Permitted Emission Rate (Current)		Add, Change, Delete, or Unchanged		Continuous Compliance Method		Concentration in Gases Exiting at Stack				
Pollutant								Average (lb/hr)			Annual (tons/yr)										
Total VOC (including those listed below)								0.04			0.04		0.18		A		ppm by vol				

State of Louisiana Emissions Inventory Questionnaire (EIQ) for Air Pollutants										Date of submittal	
										Jan	2024
Emission Point ID No. (Designation)		Descriptive Name of the Emissions Source (Alt. Name)				Approximate Location of Stack or Vent (see instructions)					
8-23		Carbon Capture Produced Water Loading				Method 18, "Interpolation - Map" Datum WGS84					
Tempo Subject Item ID No. EQT TBD7						UTM Zone 15		Horizontal 457565.87 mE		Vertical 3523978.64 mN	
		Longitude 93° 26' 54"				68 hundredths					
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (ft) or Stack Discharge Area (ft ²)	Height of Stack Above Grade (ft)	Stack Gas Exit Velocity	Stack Gas Flow at Conditions, not at Standard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Operating Time (hours per year)	Date of Construction or Modification	Percent of Annual Throughput Through This Emission Point			
								Jan-Mar	Apr-Jun	Jul-Sep	Oct-Dec
no	0 ft	0 ft	0.00 ft/sec			8760 hr/yr	proposed	25%	25%	25%	25%
Type of Fuel Used and Heat Input (see instructions)				Operating Parameters (include units)							
Fuel	Type of Fuel		Heat Input (MMBTU/hr)		Normal Operating Rate/Throughput		Parameter		Description		
	a				3066000		3066000		gal/yr		
	b						3066000		gal/yr		
	c										
Notes				Design Capacity/Volume/Cylinder Displacement		Shell Height (ft)		Tank Diameter (ft)			
				Tanks: <input type="checkbox"/> Fixed Roof <input type="checkbox"/> Floating Roof <input type="checkbox"/> External <input type="checkbox"/> Internal		Date Engine Ordered		Engine Model Year			
				Date Engine Was Built by Manufacturer							
				SI Engines: <input type="checkbox"/> Rich Burn <input type="checkbox"/> Lean Burn <input type="checkbox"/> 2 Stroke <input type="checkbox"/> 4 Stroke							
Emission Point ID No. (Designation)		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Proposed Emission Rates			Permitted Emission Rate (Current)	Add, Change, Delete, or Unchanged	Continuous Compliance Method	Concentration in Gases Exiting at Stack
8-23					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)				
Pollutant					0.09	0.09	0.02		A		ppm by vol
Total VOC (including those listed below)											

24. NSR Applicability Summary [LAC 33:III.504 and LAC 33:III.509] N/A

This section consists of seven subsections, A-G, and is applicable only to new and existing major stationary sources (as defined in LAC 33:III.504 or in LAC 33:III.509) proposing to permit a physical change or change in the method of operation. It would also apply to existing minor stationary sources proposing a physical change or change in the method of operation where the change would be a major source in and of itself. Add rows to each table as necessary. Provide a written explanation of the information summarized in these tables. Consult instructions.

6: Refer to Section 3 and Appendix A for a detailed narrative describing the NSR analysis methodology and associated project increases.

24.A. Project Summary

Emission Point ID	Description	A New, Modified, Affected, or Unaffected*	B Pre-Project Allowables (TPY)	C Baseline Actual Emissions (over 24-month period)	D Projected Actual Emissions (TPY)	E Post-Project Potential to Emit (TPY)	F Change
PM_{2.5}	24-Month Period: MM/DD/YYYY – MM/DD/YYYY						
						PM_{2.5} Change:	
PM₁₀	24-Month Period: MM/DD/YYYY – MM/DD/YYYY						
						PM₁₀ Change:	
SO₂	24-Month Period: MM/DD/YYYY – MM/DD/YYYY						
						SO₂ Change:	
NO_x	24-Month Period: MM/DD/YYYY – MM/DD/YYYY						

							NOx Change:	
CO	24-Month Period: MM/DD/YYYY – MM/DD/YYYY							
							CO Change:	
VOC	24-Month Period: MM/DD/YYYY – MM/DD/YYYY							
							VOC Change:	
CO2e	24-Month Period: MM/DD/YYYY – MM/DD/YYYY							
							CO2e Change:	

* Unaffected emissions units are not required to be listed individually. By choosing not to list unaffected emissions units, the applicant asserts that all emissions units not listed in Table 24.A will not be modified or experience an increase in actual annual emissions as part of the proposed project.

24.B. Creditable Contemporaneous Changes

Contemporaneous Period: MM/DD/YYYY – MM/DD/YYYY							
		A	B	C	D	E	F
Emission Point ID	Description	Date of Modification	Pre-Project Allowables (TPY)	Baseline Actual Emissions (over 24-month period)	24-Month Period	Post-Project Potential to Emit (TPY)	Change
PM2.5							

24.B. Creditable Contemporaneous Changes

							PM_{2.5} Change:		
PM₁₀									
							PM₁₀ Change:		
SO₂									
							SO₂ Change:		
NO_x									
							NO_x Change:		
CO									
							CO Change:		
VOC									
							VOC Change:		

24.B. Creditable Contemporaneous Changes

CO₂e								
							CO₂e Change:	

For each source identified as "New" or "Modified" in Section 24.A, complete the following table for each pollutant that will trigger NSR. If LAER is not required per LAC 33:III.504.D.3, indicate such.

24.C. BACT/LAER Summary

Emission Point ID	Pollutant	BACT/LAER	Limitation	Averaging Period	Description of Control Technology/Work Practice Standard(s)

24.D. PSD Air Quality Analyses Summary

	A	B	C	D	E	F	G	H	I	
Pollutant	Averaging Period	Preliminary Screening Concentration (µg/m ³)	Level of Significant Impact (µg/m ³)	Significant Monitoring Concentration (µg/m ³)	Background (µg/m ³)	Maximum Modeled Concentration (µg/m ³)	Modeled + Background Concentration (µg/m ³)	NAAQS (µg/m ³)	Modeled PSD Increment Consumption (µg/m ³)	Allowable Class II PSD Increment (µg/m ³)
PM _{2.5}	24-hour		1.2	4				35		-
	Annual		0.3	-				12		-
PM ₁₀	24-hour		5	10				150		30
	Annual		1	-				50		17
SO ₂	1-hour		7.8	-				195		-
	3-hour		25	-				1300		512
	24-hour		5	13				365		91
	Annual		1	-				80		20
NO _x	1-hour		7.5	-				189		-
	Annual		1	14				100		25
CO	1-hour		2000	-				40,000	-	-
	8-hour		500	575				10,000	-	-
Lead	3-month		-	0.1				1.5	-	-

24.E Nonattainment New Source Review Offsets [LAC 33:III.517.D.16, LAC 33:III.504.D.4 & 5] N/A

Complete this section only if the proposed project triggers Nonattainment New Source Review (NNSR).

This project triggers NNSR review for: NO_x VOC SO₂

NO_x:

Is the applicant proposing to use internal offsets? Yes No

If not, identify the source of the offsets. **Company:** _____

Facility/Unit: _____

Permit No.: _____

Is an ERC Bank Application included with this application, or has an application already been submitted to LDEQ?

Yes No

If the ERC application has already been submitted, give the date: _____

Identify the emissions units from which the offsets will be obtained (reference specific Emission Point ID numbers).

VOC:

Is the applicant proposing to use internal offsets? Yes No

If not, identify the source of the offsets. **Company:** _____

Facility/Unit: _____

Permit No.: _____

Is an ERC Bank Application included with this application, or has an application already been submitted to LDEQ?

Yes No

If the ERC application has already been submitted, give the date: _____

Identify the emissions units from which the offsets will be obtained (reference specific Emission Point ID numbers).

SO₂:

Is the applicant proposing to use internal offsets? Yes No

If not, identify the source of the offsets. **Company:** _____

Facility/Unit: _____

Permit No.: _____

Is an ERC Bank Application included with this application, or has an application already been submitted to LDEQ?

Yes No

If the ERC application has already been submitted, give the date: _____

Identify the emissions units from which the offsets will be obtained (reference specific Emission Point ID numbers).

In order to expedite processing, please be sure the ERC Bank Application is completed properly. In the case of NO_x, the document should clearly differentiate between ozone season and non-ozone season actual emissions during the baseline period. Be sure to indicate if a portion of the reductions are no longer surplus (e.g., due to new or revised federal or state regulations, use in a netting analysis, etc.).

24.F. Economic Impact

Answer the following questions.

How many temporary jobs will be added as a result of this project? N/A

How many permanent jobs will be added as a result of this project? N/A

24.G Notification of Federal Land Manager [LAC 33:III.504.E.1, LAC 33:III.509.P.1] N/A

Complete this section only if the proposed project triggers NNSR or PSD.

a. Is the proposed facility or modification located within 100 kilometers of a Class I Area? Yes No
 If Yes, determination of Q/d is not required; skip to the next question. If No, complete the Q/d equation below:

$$Q/d = \frac{PM_{10(NEI)} + SO_{2(NEI)} + NO_{X(NEI)} + H_2SO_{4(NEI)}}{\text{Class I km}}$$

where:

- PM_{10(NEI)} = net emissions increase of PM₁₀^{1,2}
- SO_{2(NEI)} = net emissions increase of SO₂^{1,2}
- NO_{X(NEI)} = net emissions increase of NO_X^{1,2}
- H₂SO_{4(NEI)} = net emissions increase of H₂SO₄^{1,2}
- Class I km = distance to nearest Class I Area³

Q/d = _____

Per Federal Land Manager guidance, Q values should reflect annual emissions (in tons per year, based on 24-hour maximum allowable emissions). If Q/d < 10, proceed to Section 25. If Q/d ≥ 10, complete the remainder of this Section.

- b. Has the applicant provided a copy of the application to the Federal Land Manager? Yes No
- c. Does the application contain modeling that demonstrates no adverse impact on Air Quality Related Values (AQRVs) in the Class I Area? Yes No
- d. If Yes, indicate the model used: VISCREEN PLUVUE II CALPUFF Other:⁴ _____
- e. Has the Federal Land Manager concurred that the proposed project will not adversely impact any AQRVs?
 Yes No If Yes, please attach correspondence.

¹If the net emissions increase of any pollutant is negative, enter "0."
²If the project did not trigger a netting analysis, use the project increase. In this case, the value will be less than the pollutant's significance level.
³In kilometers.
⁴Model must be approved by LDEQ and the Federal Land Manager.

25. Environmental Assessment Statement (EAS or "IT" Question Responses)

[La. R.S. 30:2018] Yes No

**** This section is required when applying for new Part 70 operating permits and/or major modifications. Any applications for these permit types that do not include answers to these questions will not be considered to be administratively complete. ****

For new Part 70 operating permits and/or major modifications, answers to these questions must be provided by the applicant to the local governmental authority and the designated public library at no additional costs to these entities. Consult instructions to determine what is considered to be a "local governmental authority" and a "designated public library." Indicate the name and address of the local governmental authority and the designated public library to which the answers to these questions were sent:

Name of Local Governing Authority			Name of Designated Public Library		
Street or P.O. Box			Street or P.O. Box		
City	State	ZIP	City	State	ZIP

Answer the following five questions on separate pages using full and complete answers. Include as many pages as necessary in order to provide full and complete answers. This information is required per Louisiana Revised Statutes 30:2018 (La. R.S. 30:2018).

Question 1: Have the potential and real adverse environmental effects of the proposed facility been avoided to the maximum extent possible?

Question 2: Does a cost benefit analysis of the environmental impact costs balanced against the social and economic benefits of the proposed facility demonstrate that the latter outweighs the former?

Question 3: Are there alternative projects which would offer more protection to the environment than the proposed facility without unduly curtailing non-environmental benefits?

Question 4: Are there alternative sites which would offer more protection to the environment than the proposed facility site without unduly curtailing non-environmental benefits?

Question 5: Are there mitigating measures which would offer more protection to the environment than the facility as proposed without unduly curtailing non-environmental benefits?

PART 70 OPERATING PERMIT APPLICATION COMPLETENESS CHECKLIST

Instructions: Complete this checklist and submit with the completed air permit application.

LAC 33:III.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
517.A Timely Submittal	Was a Copy of the Application Also Submitted to EPA?	X			N/A
517.B.1,2 Certification	Does the Application include a Certification by a Responsible Official?	X			Section 6
517.B.3 Certification	Does the Application Include Certification by a Professional Engineer or their Designee:	X			Section 6
517.D.1 Identifying Information	Does the Application Include:				
	1. Company Name, Physical and Mailing Address of Facility?	X			Section 1 & 6
	2. Map showing Location of the Facility?	X			Section 1
	3. Owner and Operator Names and Agent?	X			Section 6
	4. Name and Telephone Number of Plant Manager or Contact?	X			Section 6
517.D.2 SIC Codes, Source Categories	Does the Application Include a Description of the Source's Processes and Products?	X			Section 1 & 6
	Does the Application Include the Source's SIC Code?	X			Section 6
	Does the Application Include EPA Source Category of HAPs if applicable?	X			Section 6
517.D.3.6 EIQ Sheets	Has an EIQ Sheet been Completed for each Emission Point whether an Area or Point Source?	X			Section 6
517.D.4 Monitoring Devices	Does the Application Include Identification and Description of Compliance Monitoring Devices or Activities?	X			Section 6
517.D.5 Revisions and Modifications Only	For Revisions or Modifications, Does the Application include a Description of the Proposed Change and any Resulting Change in Emissions?	X			Section 2
517.D.7 General Information	Does the Application Include Information Regarding Fuels, Fuel Use, Raw Materials, Production Rates, and Operating Schedules as necessary to substantiate emission rates?	X			Section 1 & 6
517 D.8 Operating Limitations	Has Information Regarding any Limitations on Source Operation or any Applicable Work Practice Standards been Identified?	X			Section 6
517.D.9 Calculations	Are Emission Calculations Provided?	X			Appendix A
517.D.10 Regulatory Review	Does the Application Include a Citation and Description of Applicable Louisiana and Federal Air Quality Requirements and Standards?	X			Section 4 & 6

LAC 33:III.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
517.D.11 Test Methods	Has a Description of or a Reference to Applicable Test Methods Used to Determine Compliance with Standards been Provided?	X			Section 6
517.D.12 Major Sources of TAPs	Does the Application include Information Regarding the Compliance History of Sources Owned or Operated by the Applicant (per LAC 33.III.5111)?	X			Section 6
517.D.13 Major Sources of TAPs	Does the Application include a Demonstration to show that the Source Meets all Applicable MACT and Ambient Air Standard Requirements?			X	N/A
517.D.14 PSD Sources Only	If Required by DEQ, Does the Application Include Information Regarding the Ambient Air Impact for Criteria Pollutants as Required for the Source Impact Analysis per LAC 33:III.509.K, L, and M?			X	N/A
517 D.15 PSD Sources Only	If Required by DEQ, Does the Application Include a Detailed Ambient Air Analysis?			X	N/A
517.D.16, 18	Has any Additional Information been Provided?			X	N/A
517.D.17 Fees	Has the Fee Code been Identified?	X			Section 6 & Appendix B
	Is the Applicable Fee Included with the Application?	X			Section 6
517.E.1 Additional Part 70 Requirements	Does the Certification Statement Include a Description of the Compliance Status of Each Emission Point in the Source with All Applicable Requirements?	X			Section 6
517E.2 Additional Part 70 Requirements	Does the Certification Statement Include a Statement that the Source will continue to Comply with All Applicable Requirements with which the Source is in Compliance?	X			Section 6
517.E.3 Additional Part 70 Requirements	Does the Certification Statement Include a Statement that the Source will, on a timely basis, meet All Applicable Requirements that will Become Effective During the Permit Term?	X			Section 6
517.E.4 Additional Part 70 Requirements	Are there Applicable Requirements for which the Source is not in Compliance at the Time of Submittal?		X		N/A
	Does the Application include a Compliance Plan Schedule?			X	N/A
	Does the Schedule Include Milestone Dates for which Significant Actions will occur?			X	N/A
	Does the Schedule Include Submittal Dates for Certified Progress Reports?			X	N/A
517.E.5 Additional Part 70 Requirements Acid Rain	Is this Source Covered by the Federal Acid Rain Program?		X		N/A

LAC 33:III.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
	Are the Requirements of LAC 33:III.517.E 1-4 included in the Acid Rain Portion of the Compliance Plan?			X	N/A
517.E.6 Additional Part 70 Requirements	Have any Exemptions from any Applicable Requirements been Requested?	X			Section 6
	Is the List and explanations Provided?	X			Section 6
517.E.7 Additional Part 70 Requirements	Does the Application Include a Request for a Permit Shield?		X		
	Does the Request List those Federally Applicable Requirements for which the Shield is Requested along with the Corresponding Draft Permit Terms and conditions which are Proposed to Maintain Compliance?			X	N/A
517.E.8 Additional Part 70 Requirements	Does the Application Identify and Reasonably Anticipated Alternative Operating Scenarios?		X		
	Does the Application include Sufficient Information to Develop permit Terms and Conditions for Each Scenario, Including Source Process and Emissions Data?			X	N/A
517.F Confidentiality	Does the Application Include a Request for Non-Disclosure (Confidentiality)?		X		
525.B. Minor Permit Modifications	Does the Application Include a Listing of New Requirements Resulting for the Change?	X			Section 6
	Does the Application Include Certification by the Responsible Official that the Proposed Action Fits the Definition of a Minor Modification as per LAC 33:III.525.A.	X			Section 6
	Does the Certification also Request that Minor Modification Procedures be Used?	X			Section 1 & 6
	Does the Application, for Part 70 Sources, Include the Owner's Suggested Draft Permit and Completed Forms for the Permitting Authority to Use to Notify Affected States?	X			Section 6
La. R.S. 30:2018 – PSD/NNSR only	Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the local governing authority at no cost to the local governing authority?			X	N/A
	Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the designated public library at no cost to the designated public library?			X	N/A

APPENDIX A: PTE CALCULATION DOCUMENTATION

Summary of Emissions

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Criteria		Criteria		Criteria		Criteria		Criteria		Criteria		Criteria		Class III	
		NO _x		VOC		CO		PM		PM ₁₀		PM _{2.5}		SO ₂		H ₂ S	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Existing/Unchanged Sources																	
EQT0019	Produced Water Loading	--	--	3.63	0.18	--	--	--	--	--	--	--	--	--	--	--	--
EQT0020	Amine Storage Tank	--	--	0.41	1.81	--	--	--	--	--	--	--	--	--	--	--	--
EQT0021	Amine Storage Tank	--	--	0.41	1.81	--	--	--	--	--	--	--	--	--	--	--	--
EQT0022	Skid Drain Storage Tank	--	--	0.00	0.01	--	--	--	--	--	--	--	--	--	--	--	--
--	Insignificant Activities	--	--	--	<0.001	--	--	--	--	--	--	--	--	--	--	--	--
--	General Condition XVII Activities	--	3.00	--	7.30	--	3.00	--	--	--	--	--	--	--	--	--	--
Existing/Changed Sources																	
EQT0001	Plant 1 Amine Unit Vent	--	--	0.04	0.02	--	--	--	--	--	--	--	--	--	--	14.03	8.42
EQT0002	Plant 1 Amine Hot Oil Heater	5.48	24.01	0.46	2.01	7.00	30.66	0.63	2.77	0.63	2.77	0.63	2.77	0.42	1.82	--	--
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	0.13	0.08	--	--	--	--	--	--	--	--	--	--	<0.001	<0.001
EQT0004	Plant 1 Glycol Dehy Reboiler	0.32	1.41	0.03	0.12	0.41	1.80	0.04	0.16	0.04	0.16	0.04	0.16	0.02	0.11	--	--
EQT0005	Plant 2 Amine Unit Vent	--	--	0.04	0.02	--	--	--	--	--	--	--	--	--	--	14.03	8.42
EQT0006	Plant 2 Amine Hot Oil Heater	5.48	24.01	0.46	2.01	7.00	30.66	0.63	2.77	0.63	2.77	0.63	2.77	0.42	1.82	--	--
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	0.13	0.08	--	--	--	--	--	--	--	--	--	--	<0.001	<0.001
EQT0008	Plant 2 Glycol Dehy Reboiler	0.32	1.41	0.03	0.12	0.41	1.80	0.04	0.16	0.04	0.16	0.04	0.16	0.02	0.11	--	--
EQT0009	Plant 1 Thermal Oxidizer	2.13	9.32	0.18	0.79	2.72	11.90	0.25	1.08	0.25	1.08	0.25	1.08	26.04	114.05	0.28	1.23
EQT0010	Plant 2 Thermal Oxidizer	2.13	9.32	0.18	0.79	2.72	11.90	0.25	1.08	0.25	1.08	0.25	1.08	26.04	114.05	0.28	1.23
EQT0011	CAT G3606 Compressor Engine	2.07	9.05	0.85	3.71	0.64	2.79	0.14	0.62	0.14	0.62	0.14	0.62	0.07	0.30	--	--
EQT0012	CAT G3606 Compressor Engine	2.07	9.05	0.85	3.71	0.64	2.79	0.14	0.62	0.14	0.62	0.14	0.62	0.07	0.30	--	--
EQT0013	CAT G3606 Compressor Engine	2.07	9.05	0.85	3.71	0.64	2.79	0.14	0.62	0.14	0.62	0.14	0.62	0.07	0.30	--	--
EQT0014	CAT G3606 Compressor Engine	2.07	9.05	0.85	3.71	0.64	2.79	0.14	0.62	0.14	0.62	0.14	0.62	0.07	0.30	--	--
EQT0023	Flare	0.01	0.05	0.00	<0.001	0.01	0.04	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	--	--
FUG0001	Fugitive Emissions	--	--	0.31	1.35	--	--	--	--	--	--	--	--	--	--	<0.001	<0.001
New Sources																	
1-23	CAT G3608 Compressor Engine	1.65	7.24	0.50	2.17	0.88	3.86	0.19	0.83	0.19	0.83	0.19	0.83	0.09	0.41	--	--
2-23	CAT G3608 Compressor Engine	1.65	7.24	0.50	2.17	0.88	3.86	0.19	0.83	0.19	0.83	0.19	0.83	0.09	0.41	--	--
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	0.001	0.005	0.001	0.005	0.001	0.005	--	--	--	--
5-23B	CO ₂ Dehydrator Reboiler	0.10	0.43	0.01	0.02	0.08	0.36	0.01	0.03	0.01	0.03	0.01	0.03	0.005	0.02	--	--
6-23	Carbon Capture Produced Water Storage Tank	--	--	0.04	0.18	--	--	--	--	--	--	--	--	--	--	--	--
7-23	Carbon Capture Produced Water Storage Tank	--	--	0.04	0.18	--	--	--	--	--	--	--	--	--	--	--	--
8-23	Carbon Capture Produced Water Loading	--	--	0.09	0.02	--	--	--	--	--	--	--	--	--	--	--	--
Project Total Emissions		27.55	120.68	6.54	26.99	24.66	108.02	2.79	12.21	2.79	12.21	2.79	12.21	53.42	233.99	28.62	19.29
Existing Source Emissions		<0.001	<0.001	4.46	3.80	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		27.55	120.68	11.00	30.79	24.66	108.02	2.79	12.21	2.79	12.21	2.79	12.21	53.42	233.99	28.62	19.29

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Class I		Class II		Class II		Class III		Class III		Class I		Class III		Class II	
		Formaldehyde		Acetaldehyde		Acrolein		Methanol		n-Hexane		Benzene		Toluene		Ethylbenzene	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Existing/Unchanged Sources																	
EQT0019	Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0020	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0021	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0022	Skid Drain Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	Insignificant Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	General Condition XVII Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Existing/Changed Sources																	
EQT0001	Plant 1 Amine Unit Vent	--	--	--	--	--	--	--	--	0.01	0.00	--	--	--	--	--	--
EQT0002	Plant 1 Amine Hot Oil Heater	0.01	0.03	--	--	--	--	--	--	0.15	0.66	<0.001	0.00	<0.001	0.00	--	--
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	0.10	0.06	--	--	--	--	--	--
EQT0004	Plant 1 Glycol Dehy Reboiler	<0.001	0.00	--	--	--	--	--	--	0.01	0.04	--	--	--	--	--	--
EQT0005	Plant 2 Amine Unit Vent	--	--	--	--	--	--	--	--	0.01	0.00	--	--	--	--	--	--
EQT0006	Plant 2 Amine Hot Oil Heater	0.01	0.03	--	--	--	--	--	--	0.15	0.66	<0.001	0.00	<0.001	0.00	--	--
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	0.10	0.06	--	--	--	--	--	--
EQT0008	Plant 2 Glycol Dehy Reboiler	<0.001	0.00	--	--	--	--	--	--	0.01	0.04	--	--	--	--	--	--
EQT0009	Plant 1 Thermal Oxidizer	--	--	--	--	--	--	--	--	0.06	0.26	--	--	--	--	--	--
EQT0010	Plant 2 Thermal Oxidizer	--	--	--	--	--	--	--	--	0.06	0.26	--	--	--	--	--	--
EQT0011	CAT G3606 Compressor Engine	0.25	1.09	0.06	0.26	0.036	0.160	0.02	0.08	0.01	0.03	0.00	0.01	0.00	0.01	<0.001	0.00
EQT0012	CAT G3606 Compressor Engine	0.25	1.09	0.06	0.26	0.036	0.160	0.02	0.08	0.01	0.03	0.00	0.01	0.00	0.01	<0.001	0.00
EQT0013	CAT G3606 Compressor Engine	0.25	1.09	0.06	0.26	0.036	0.160	0.02	0.08	0.01	0.03	0.00	0.01	0.00	0.01	<0.001	0.00
EQT0014	CAT G3606 Compressor Engine	0.25	1.09	0.06	0.26	0.036	0.160	0.02	0.08	0.01	0.03	0.00	0.01	0.00	0.01	<0.001	0.00
EQT0023	Flare	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
FUG0001	Fugitive Emissions	--	--	--	--	--	--	--	--	--	--	0.01	0.07	0.02	0.07	0.01	0.07
New Sources																	
1-23	CAT G3608 Compressor Engine	0.11	0.48	0.08	0.35	0.049	0.213	0.02	0.10	0.01	0.05	0.00	0.02	0.00	0.02	<0.001	0.002
2-23	CAT G3608 Compressor Engine	0.11	0.48	0.08	0.35	0.049	0.213	0.02	0.10	0.01	0.05	0.00	0.02	0.00	0.02	<0.001	0.002
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
5-23B	CO ₂ Dehydrator Reboiler	--	--	--	--	--	--	--	--	0.002	0.01	--	--	--	--	--	--
6-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
7-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
8-23	Carbon Capture Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Project Total Emissions		1.23	5.37	0.40	1.73	0.24	1.06	0.12	0.52	0.70	2.28	0.04	0.16	0.04	0.16	0.02	0.07
Existing Source Emissions		<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		1.23	5.37	0.40	1.73	0.243	1.065	0.12	0.52	0.70	2.28	0.04	0.16	0.04	0.16	0.02	0.07

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Class II		Class II		Class II		Class II		Class II		Class II		Class II		Class I	
		Xylene		Barium		1,3-Butadiene		Biphenyl		Carbon Tetrachloride		Chlorobenzene		Chloroform		Chromium	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Existing/Unchanged Sources																	
EQT0019	Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0020	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0021	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0022	Skid Drain Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	Insignificant Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	General Condition XVII Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Existing/Changed Sources																	
EQT0001	Plant 1 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0002	Plant 1 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0004	Plant 1 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0005	Plant 2 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0006	Plant 2 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0008	Plant 2 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0009	Plant 1 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0010	Plant 2 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0011	CAT G3606 Compressor Engine	0.00	0.01	--	--	0.002	0.008	0.00	0.01	<0.001	0.00	<0.001	0.001	<0.001	0.00	--	--
EQT0012	CAT G3606 Compressor Engine	0.00	0.01	--	--	0.002	0.008	0.00	0.01	<0.001	0.00	<0.001	0.001	<0.001	0.00	--	--
EQT0013	CAT G3606 Compressor Engine	0.00	0.01	--	--	0.002	0.008	0.00	0.01	<0.001	0.00	<0.001	0.001	<0.001	0.00	--	--
EQT0014	CAT G3606 Compressor Engine	0.00	0.01	--	--	0.002	0.008	0.00	0.01	<0.001	0.00	<0.001	0.001	<0.001	0.00	--	--
EQT0023	Flare	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
FUG0001	Fugitive Emissions	0.02	0.07	--	--	--	--	--	--	--	--	--	--	--	--	--	--
New Sources																	
1-23	CAT G3608 Compressor Engine	0.00	0.01	--	--	0.003	0.011	0.00	0.01	<0.001	0.002	<0.001	0.001	<0.001	0.001	--	--
2-23	CAT G3608 Compressor Engine	0.00	0.01	--	--	0.003	0.011	0.00	0.01	<0.001	0.002	<0.001	0.001	<0.001	0.001	--	--
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
5-23B	CO ₂ Dehydrator Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
6-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
7-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
8-23	Carbon Capture Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Project Total Emissions		0.02	0.11	<0.001	<0.001	0.01	0.06	0.01	0.04	0.00	0.01	0.00	0.01	0.00	0.01	<0.001	<0.001
Existing Source Emissions		<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		0.02	0.11	<0.001	<0.001	0.013	0.055	0.01	0.04	0.00	0.01	0.001	0.006	0.00	0.01	<0.001	<0.001

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Class II		Supplemental		Class II		Class II		Class II		Class I		Class II	
		Dichlorobenzene		1,1-Dichloroethane		1,2-Dichloroethane		1,2-Dichloropropane		1,3-Dichloropropane		Ethylene Dibromide		Methylene Chloride	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Existing/Unchanged Sources															
EQT0019	Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0020	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0021	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0022	Skid Drain Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	Insignificant Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	General Condition XVII Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Existing/Changed Sources															
EQT0001	Plant 1 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0002	Plant 1 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0004	Plant 1 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0005	Plant 2 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0006	Plant 2 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0008	Plant 2 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0009	Plant 1 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0010	Plant 2 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0011	CAT G3606 Compressor Engine	--	--	--	--	--	--	--	--	<0.001	0.00	<0.001	0.001	<0.001	0.001
EQT0012	CAT G3606 Compressor Engine	--	--	--	--	--	--	--	--	<0.001	0.00	<0.001	0.001	<0.001	0.001
EQT0013	CAT G3606 Compressor Engine	--	--	--	--	--	--	--	--	<0.001	0.00	<0.001	0.001	<0.001	0.001
EQT0014	CAT G3606 Compressor Engine	--	--	--	--	--	--	--	--	<0.001	0.00	<0.001	0.001	<0.001	0.001
EQT0023	Flare	--	--	--	--	--	--	--	--	--	--	--	--	--	--
FUG0001	Fugitive Emissions	--	--	--	--	--	--	--	--	--	--	--	--	--	--
New Sources															
1-23	CAT G3608 Compressor Engine	--	--	<0.001	0.001	<0.001	0.001	<0.001	0.001	<0.001	0.001	<0.001	0.002	<0.001	0.001
2-23	CAT G3608 Compressor Engine	--	--	<0.001	0.001	<0.001	0.001	<0.001	0.001	<0.001	0.001	<0.001	0.002	<0.001	0.001
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	--	--	--	--	--	--	--	--
5-23B	CO ₂ Dehydrator Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
6-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
7-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
8-23	Carbon Capture Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Project Total Emissions		<0.001	<0.001	<0.001	0.00	<0.001	0.00	0.00	0.00	0.00	0.01	0.00	0.01	0.00	0.00
Existing Source Emissions		<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		<0.001	<0.001	<0.001	0.00	<0.001	0.002	0.00	0.00	0.00	0.01	0.002	0.009	0.00	0.00

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Class II		Class I		Class II		Class II		Class II		Class II		Class II	
		Naphthalene (and Methyl-naphthalenes)		Nickel		Phenol		PAH		Styrene		1,1,2,2-Tetrachloroethane		1,1,2-Trichloroethane	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Existing/Unchanged Sources															
EQT0019	Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0020	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0021	Amine Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0022	Skid Drain Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	Insignificant Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--
--	General Condition XVII Activities	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Existing/Changed Sources															
EQT0001	Plant 1 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0002	Plant 1 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0004	Plant 1 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0005	Plant 2 Amine Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0006	Plant 2 Amine Hot Oil Heater	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0008	Plant 2 Glycol Dehy Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0009	Plant 1 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0010	Plant 2 Thermal Oxidizer	--	--	--	--	--	--	--	--	--	--	--	--	--	--
EQT0011	CAT G3606 Compressor Engine	0.00	0.00	--	--	--	--	--	--	<0.001	0.00	<0.001	0.00	<0.001	0.00
EQT0012	CAT G3606 Compressor Engine	0.00	0.00	--	--	--	--	--	--	<0.001	0.00	<0.001	0.00	<0.001	0.00
EQT0013	CAT G3606 Compressor Engine	0.00	0.00	--	--	--	--	--	--	<0.001	0.00	<0.001	0.00	<0.001	0.00
EQT0014	CAT G3606 Compressor Engine	0.00	0.00	--	--	--	--	--	--	<0.001	0.00	<0.001	0.00	<0.001	0.00
EQT0023	Flare	--	--	--	--	--	--	--	--	--	--	--	--	--	--
FUG0001	Fugitive Emissions	--	--	--	--	--	--	--	--	--	--	--	--	--	--
New Sources															
1-23	CAT G3608 Compressor Engine	0.001	0.00	--	--	<0.001	0.00	--	--	<0.001	0.001	<0.001	0.002	<0.001	0.001
2-23	CAT G3608 Compressor Engine	0.001	0.00	--	--	<0.001	0.00	--	--	<0.001	0.001	<0.001	0.002	<0.001	0.001
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	--	--	--	--	--	--	--	--
5-23B	CO ₂ Dehydrator Reboiler	--	--	--	--	--	--	--	--	--	--	--	--	--	--
6-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
7-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	--	--	--	--	--	--	--	--
8-23	Carbon Capture Produced Water Loading	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Project Total Emissions		0.01	0.02	<0.001	<0.001	<0.001	0.00	<0.001	<0.001	0.00	0.00	0.00	0.01	0.00	0.01
Existing Source Emissions		<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		0.01	0.02	<0.001	<0.001	<0.001	0.00	<0.001	<0.001	0.00	0.00	0.00	0.01	0.00	0.01

Emissions Summary
 ET Gathering & Processing LLC
 Ajax Amine Plant

Source	Source Description	Supplemental		Class I		Class III		Total HAPs	
		2,2,4-Trimethylpentane		Vinyl Chloride		Zinc		lb/hr	tpy
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy		
Existing/Unchanged Sources									
EQT0019	Produced Water Loading	--	--	--	--	--	--	<0.001	<0.001
EQT0020	Amine Storage Tank	--	--	--	--	--	--	<0.001	<0.001
EQT0021	Amine Storage Tank	--	--	--	--	--	--	<0.001	<0.001
EQT0022	Skid Drain Storage Tank	--	--	--	--	--	--	<0.001	<0.001
--	Insignificant Activities	--	--	--	--	--	--	<0.001	<0.001
--	General Condition XVII Activities	--	--	--	--	--	--	<0.001	<0.001
Existing/Changed Sources									
EQT0001	Plant 1 Amine Unit Vent	--	--	--	--	--	--	0.01	0.00
EQT0002	Plant 1 Amine Hot Oil Heater	--	--	--	--	--	--	0.16	0.69
EQT0003	Plant 1 Glycol Dehy Unit Vent	--	--	--	--	--	--	0.10	0.06
EQT0004	Plant 1 Glycol Dehy Reboiler	--	--	--	--	--	--	0.01	0.04
EQT0005	Plant 2 Amine Unit Vent	--	--	--	--	--	--	0.01	0.00
EQT0006	Plant 2 Amine Hot Oil Heater	--	--	--	--	--	--	0.16	0.69
EQT0007	Plant 2 Glycol Dehy Unit Vent	--	--	--	--	--	--	0.10	0.06
EQT0008	Plant 2 Glycol Dehy Reboiler	--	--	--	--	--	--	0.01	0.04
EQT0009	Plant 1 Thermal Oxidizer	--	--	--	--	--	--	0.06	0.26
EQT0010	Plant 2 Thermal Oxidizer	--	--	--	--	--	--	0.06	0.26
EQT0011	CAT G3606 Compressor Engine	0.00	0.01	--	--	--	--	0.38	1.69
EQT0012	CAT G3606 Compressor Engine	0.00	0.01	--	--	--	--	0.38	1.69
EQT0013	CAT G3606 Compressor Engine	0.00	0.01	--	--	--	--	0.38	1.69
EQT0014	CAT G3606 Compressor Engine	0.00	0.01	--	--	--	--	0.38	1.69
EQT0023	Flare	--	--	--	--	--	--	<0.001	<0.001
FUG0001	Fugitive Emissions	--	--	--	--	--	--	0.06	0.27
New Sources									
1-23	CAT G3608 Compressor Engine	0.00	0.01	<0.001	0.001	--	--	0.29	1.29
2-23	CAT G3608 Compressor Engine	0.00	0.01	<0.001	0.001	--	--	0.29	1.29
3-23	Sulfur Loading and Handling	--	--	--	--	--	--	<0.001	<0.001
5-23B	CO ₂ Dehydrator Reboiler	--	--	--	--	--	--	0.00	0.01
6-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	<0.001	<0.001
7-23	Carbon Capture Produced Water Storage Tank	--	--	--	--	--	--	<0.001	<0.001
8-23	Carbon Capture Produced Water Loading	--	--	--	--	--	--	<0.001	<0.001
Project Total Emissions		0.01	0.05	<0.001	0.00	<0.001	<0.001	2.85	11.70
Existing Source Emissions		<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001	<0.001
Proposed Sitewide Emissions		0.01	0.05	<0.001	0.00	<0.001	<0.001	2.85	11.70

Engines Calculations

Engine Emissions

T Gathering & Processing LLC

Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3608 Compressor Engine				
TEMPO ID:	TBD	Construction Year:	2023	Regulation:	MACT ZZZZ; NSPS JJJJ
Source ID No:	1-23	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	2,500.00	HP	Engine Dataplate
Power Rating (avg):	1,865.67	KW	KW = HP / 1.34
Power Rating (max):	2,500.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	18.92	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.3000	g/bhp-hr	Vendor	
CO	0.1600	g/bhp-hr	Vendor	
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0900	g/bhp-hr	Vendor	
Hazardous Air Pollutant (HAP)				
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Biphenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1-Dichloroethane	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,2-Dichloroethane	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,2-Dichloropropane	1.35E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Formaldehyde	2.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH
Phenol	1.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Vinyl Chloride	7.45E-06	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Total Speciated VOCs	0.0297	lb/MMBTU		
Total Speciated TAP	0.0297	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0001	lb/MMBTU		

MISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	1.65	1.65	14,484.38	7.24	
CO	0.88	0.88	7,725.00	3.86	
PM ₁₀	0.19	0.19	1,655.25	0.83	
PM _{2.5}	0.19	0.19	1,655.25	0.83	
SO ₂	0.09	0.09	810.12	0.41	
VOC (Total)	0.50	0.50	4,345.31	2.17	
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	0.003	0.003	22.126	0.011	HAP, TAP, TRI
Acetaldehyde	0.079	0.079	692.790	0.346	HAP, TAP, TRI
Acrolein	0.049	0.049	425.950	0.213	HAP, TAP, TRI
Benzene	0.004	0.004	36.463	0.018	TAP, HAP, TRI
Biphenyl	0.002	0.002	17.568	0.009	HAP, TAP, TRI
Carbon Tetrachloride	0.000	0.000	3.041	0.002	HAP, TAP, TRI
Chlorobenzene	0.000	0.000	2.519	0.001	HAP, TAP, TRI
Chloroform	0.000	0.000	2.362	0.001	HAP, TAP, TRI
1,1-Dichloroethane	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,2-Dichloroethane	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,2-Dichloropropane	0.000	0.000	2.229	0.001	HAP, TAP, TRI
1,3-Dichloropropene	0.000	0.000	2.188	0.001	HAP, TAP, TRI
Ethylbenzene	0.000	0.000	3.290	0.002	HAP, TAP, TRI
Ethylene Dibromide	0.000	0.000	3.671	0.002	HAP, TAP, TRI
Formaldehyde	0.110	0.110	965.625	0.483	HAP, TAP, TRI
Methanol	0.024	0.024	207.174	0.104	HAP, TAP, TRI
Methylene Chloride	0.000	0.000	1.657	0.001	HAP, TAP, TRI
2-Methylnaphthalene	0.000	0.000	2.751	0.001	TAP
n-Hexane	0.011	0.011	91.985	0.046	HAP, TAP, TRI
Naphthalene	0.001	0.001	6.165	0.003	HAP, TRI, PAH
Phenol	0.000	0.000	1.989	0.001	HAP, TAP, TRI
Styrene	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	0.000	0.000	3.315	0.002	HAP, TAP, TRI
Toluene	0.004	0.004	33.811	0.017	TAP, TRI
1,1,2-Trichloroethane	0.000	0.000	2.635	0.001	HAP, TAP, TRI
2,2,4-Trimethylpentane	0.002	0.002	20.717	0.010	HAP, TAP, TRI
Vinyl Chloride	0.000	0.000	1.235	0.001	HAP, TAP, TRI
Xylenes	0.002	0.002	15.248	0.008	TAP, HAP, TRI
Total Speciated VOCs	0.294	0.294	2,576.972	1.288	
Total Speciated TAP	0.294	0.294	2,577.053	1.289	
Total Speciated PAH	0.000	0.000	2.238	0.001	
Total Naphthalenes	0.001	0.001	8.917	0.004	

Engine Emissions
ET Gathering & Processing LLC
Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3608 Compressor Engine				
TEMPO ID:	TBD	Construction Year:	2023	Regulation:	MACT ZZZZ; NSPS JJJ
Source ID No:	2-23	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	2,500.00	HP	Engine Dataplate
Power Rating (avg):	1,865.67	KW	KW = HP / 1.34
Power Rating (max):	2,500.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	18.92	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.3000	g/bhp-hr	Vendor	
CO	0.1600	g/bhp-hr	Vendor	
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0900	g/bhp-hr	Vendor	
Hazardous Air Pollutant (HAP)				
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Biphenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1-Dichloroethane	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,2-Dichloroethane	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,2-Dichloropropane	1.35E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Formaldehyde	2.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH
Phenol	1.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Vinyl Chloride	7.45E-06	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Total Speciated VOCs	0.0297	lb/MMBTU		
Total Speciated TAP	0.0297	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0001	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	1.65	1.65	14,484.38	7.24	
CO	0.88	0.88	7,725.00	3.86	
PM ₁₀	0.19	0.19	1,655.25	0.83	
PM _{2.5}	0.19	0.19	1,655.25	0.83	
SO ₂	0.09	0.09	810.12	0.41	
VOC (Total)	0.50	0.50	4,345.31	2.17	
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	0.003	0.003	22.126	0.011	HAP, TAP, TRI
Acetaldehyde	0.079	0.079	692.790	0.346	HAP, TAP, TRI
Acrolein	0.049	0.049	425.950	0.213	HAP, TAP, TRI
Benzene	0.004	0.004	36.463	0.018	TAP, HAP, TRI
Biphenyl	0.002	0.002	17.568	0.009	HAP, TAP, TRI
Carbon Tetrachloride	0.000	0.000	3.041	0.002	HAP, TAP, TRI
Chlorobenzene	0.000	0.000	2.519	0.001	HAP, TAP, TRI
Chloroform	0.000	0.000	2.362	0.001	HAP, TAP, TRI
1,1-Dichloroethane	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,2-Dichloroethane	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,2-Dichloropropane	0.000	0.000	2.229	0.001	HAP, TAP, TRI
1,3-Dichloropropene	0.000	0.000	2.188	0.001	HAP, TAP, TRI
Ethylbenzene	0.000	0.000	3.290	0.002	HAP, TAP, TRI
Ethylene Dibromide	0.000	0.000	3.671	0.002	HAP, TAP, TRI
Formaldehyde	0.110	0.110	965.625	0.483	HAP, TAP, TRI
Methanol	0.024	0.024	207.174	0.104	HAP, TAP, TRI
Methylene Chloride	0.000	0.000	1.657	0.001	HAP, TAP, TRI
2-Methylnaphthalene	0.000	0.000	2.751	0.001	TAP
n-Hexane	0.011	0.011	91.985	0.046	HAP, TAP, TRI
Naphthalene	0.001	0.001	6.165	0.003	HAP, TRI, PAH
Phenol	0.000	0.000	1.989	0.001	HAP, TAP, TRI
Styrene	0.000	0.000	1.956	0.001	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	0.000	0.000	3.315	0.002	HAP, TAP, TRI
Toluene	0.004	0.004	33.811	0.017	TAP, TRI
1,1,2-Trichloroethane	0.000	0.000	2.635	0.001	HAP, TAP, TRI
2,2,4-Trimethylpentane	0.002	0.002	20.717	0.010	HAP, TAP, TRI
Vinyl Chloride	0.000	0.000	1.235	0.001	HAP, TAP, TRI
Xylenes	0.002	0.002	15.248	0.008	TAP, HAP, TRI
Total Speciated VOCs	0.294	0.294	2,576.972	1.288	
Total Speciated TAP	0.294	0.294	2,577.053	1.289	
Total Speciated PAH	0.000	0.000	2.238	0.001	
Total Naphthalenes	0.001	0.001	8.917	0.004	

Engine Emissions
 ET Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3606 Compressor Engine				
TEMPO ID:	EQT0011	Construction Year:	2022	Regulation:	MACT ZZZZ; NSPS JJJJ
Source ID No:	7-22	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	1,875.00	HP	Engine Dataplate
Power Rating (avg):	1,399.25	KW	KW = HP / 1.34
Power Rating (max):	1,875.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	14.19	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS					
Pollutant	Value	Unit	Basis	Notes	
Criteria					
NOx	0.5000	g/bhp-hr	Vendor		
CO	0.1540	g/bhp-hr	Vendor		
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable	
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance		
VOC (Total)	0.2050	g/bhp-hr	Vendor		
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI	
B-phenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Formaldehyde	6.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI	
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP	
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH	
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI	
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI	
Total Speciated VOCs	0.0697	lb/MMBTU			
Total Speciated TAP	0.0697	lb/MMBTU			
Total Speciated PAH	0.0000	lb/MMBTU			
Total Naphthalenes	0.0001	lb/MMBTU			

MISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.07	2.07	18,105.48	9.05	
CO	0.64	0.64	5,576.49	2.79	
PM ₁₀	0.14	0.14	1,241.44	0.62	
PM _{2.5}	0.14	0.14	1,241.44	0.62	
SO ₂	0.07	0.07	607.59	0.30	
VOC (Total)	0.85	0.85	7,423.25	3.71	
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	0.002	0.002	16.595	0.008	HAP, TAP, TRI
Acetaldehyde	0.059	0.059	519.592	0.260	HAP, TAP, TRI
Acrolein	0.036	0.036	319.462	0.160	HAP, TAP, TRI
Benzene	0.003	0.003	27.347	0.014	TAP, HAP, TRI
Biphenyl	0.002	0.002	13.176	0.007	HAP, TAP, TRI
Carbon Tetrachloride	0.000	0.000	2.281	0.001	HAP, TAP, TRI
Chlorobenzene	0.000	0.000	1.889	0.001	HAP, TAP, TRI
Chloroform	0.000	0.000	1.771	0.001	HAP, TAP, TRI
1,3-Dichloropropene	0.000	0.000	1.641	0.001	HAP, TAP, TRI
Ethylbenzene	0.000	0.000	2.467	0.001	HAP, TAP, TRI
Ethylene Dibromide	0.000	0.000	2.753	0.001	HAP, TAP, TRI
Formaldehyde	0.248	0.248	2,172.657	1.086	HAP, TAP, TRI
Methanol	0.018	0.018	155.381	0.078	HAP, TAP, TRI
Methylene Chloride	0.000	0.000	1.243	0.001	HAP, TAP, TRI
2-Methylnaphthalene	0.000	0.000	2.063	0.001	TAP
n-Hexane	0.008	0.008	68.989	0.034	HAP, TAP, TRI
Naphthalene	0.001	0.001	4.624	0.002	HAP, TRI, PAH
Styrene	0.000	0.000	1.467	0.001	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	0.000	0.000	2.486	0.001	HAP, TAP, TRI
Toluene	0.003	0.003	25.358	0.013	TAP, TRI
1,1,2-Trichloroethane	0.000	0.000	1.976	0.001	HAP, TAP, TRI
2,2,4-Trimethylpentane	0.002	0.002	15.538	0.008	HAP, TAP, TRI
Xylenes	0.001	0.001	11.436	0.006	TAP, HAP, TRI
Total Speciated VOCs	0.386	0.386	3,381.167	1.691	
Total Speciated TAP	0.386	0.386	3,381.228	1.691	
Total Speciated PAH	0.000	0.000	1.679	0.001	
Total Naphthalenes	0.001	0.001	6.688	0.003	

Engine Emissions
 T Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3606 Compressor Engine				
TEMPO ID:	EQT0012	Construction Year:	2022	Regulation:	MACT ZZZZ; NSPS JJJJ
Source ID No:	8-22	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	1,875.00	HP	Engine Dataplate
Power Rating (avg):	1,399.25	KW	KW = HP / 1.34
Power Rating (max):	1,875.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	14.19	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.5000	g/bhp-hr	Vendor	
CO	0.1540	g/bhp-hr	Vendor	
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.2050	g/bhp-hr	Vendor	
Hazardous Air Pollutant (HAP)				
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Biphenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Formaldehyde	6.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Total Speciated VOCs	0.0697	lb/MMBTU		
Total Speciated TAP	0.0697	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0001	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.07	2.07	18,105.48	9.05	
CO	0.64	0.64	5,576.49	2.79	
PM ₁₀	0.14	0.14	1,241.44	0.62	
PM _{2.5}	0.14	0.14	1,241.44	0.62	
SO ₂	0.07	0.07	607.59	0.30	
VOC (Total)	0.85	0.85	7,423.25	3.71	
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	0.002	0.002	16.595	0.008	HAP, TAP, TRI
Acetaldehyde	0.059	0.059	519.592	0.260	HAP, TAP, TRI
Acrolein	0.036	0.036	319.462	0.160	HAP, TAP, TRI
Benzene	0.003	0.003	27.347	0.014	TAP, HAP, TRI
Biphenyl	0.002	0.002	13.176	0.007	HAP, TAP, TRI
Carbon Tetrachloride	0.000	0.000	2.281	0.001	HAP, TAP, TRI
Chlorobenzene	0.000	0.000	1.889	0.001	HAP, TAP, TRI
Chloroform	0.000	0.000	1.771	0.001	HAP, TAP, TRI
1,3-Dichloropropene	0.000	0.000	1.641	0.001	HAP, TAP, TRI
Ethylbenzene	0.000	0.000	2.467	0.001	HAP, TAP, TRI
Ethylene Dibromide	0.000	0.000	2.753	0.001	HAP, TAP, TRI
Formaldehyde	0.248	0.248	2,172.657	1.086	HAP, TAP, TRI
Methanol	0.018	0.018	155.381	0.078	HAP, TAP, TRI
Methylene Chloride	0.000	0.000	1.243	0.001	HAP, TAP, TRI
2-Methylnaphthalene	0.000	0.000	2.063	0.001	TAP
n-Hexane	0.008	0.008	68.989	0.034	HAP, TAP, TRI
Naphthalene	0.001	0.001	4.624	0.002	HAP, TRI, PAH
Styrene	0.000	0.000	1.467	0.001	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	0.000	0.000	2.486	0.001	HAP, TAP, TRI
Toluene	0.003	0.003	25.358	0.013	TAP, TRI
1,1,2-Trichloroethane	0.000	0.000	1.976	0.001	HAP, TAP, TRI
2,2,4-Trimethylpentane	0.002	0.002	15.538	0.008	HAP, TAP, TRI
Xylenes	0.001	0.001	11.436	0.006	TAP, HAP, TRI
Total Speciated VOCs	0.386	0.386	3,381.167	1.691	
Total Speciated TAP	0.386	0.386	3,381.228	1.691	
Total Speciated PAH	0.000	0.000	1.679	0.001	
Total Naphthalenes	0.001	0.001	6.688	0.003	

Engine Emissions
ET Gathering & Processing LLC
Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3606 Compressor Engine				
TEMPO ID:	EQT0013	Construction Year:	2022	Regulation:	MACT ZZZZ; NSPS JJJ
Source ID No:	9-22	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	1,875.00	HP	Engine Dataplate
Power Rating (avg):	1,399.25	KW	KW = HP / 1.34
Power Rating (max):	1,875.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	14.19	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS					
Pollutant	Value	Unit	Basis	Notes	
Criteria					
NOx	0.5000	g/bhp-hr	Vendor		
CO	0.1540	g/bhp-hr	Vendor		
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable	
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance		
VOC (Total)	0.2050	g/bhp-hr	Vendor		
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI	
Biphenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Formaldehyde	6.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI	
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP	
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH	
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI	
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI	
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI	
Total Speciated VOCs	0.0697	lb/MMBTU			
Total Speciated TAP	0.0697	lb/MMBTU			
Total Speciated PAH	0.0000	lb/MMBTU			
Total Naphthalenes	0.0001	lb/MMBTU			

MISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.07	2.07	18,105.48	9.05	
CO	0.64	0.64	5,576.49	2.79	
PM ₁₀	0.14	0.14	1,241.44	0.62	
PM _{2.5}	0.14	0.14	1,241.44	0.62	
SO ₂	0.07	0.07	607.59	0.30	
VOC (Total)	0.85	0.85	7,423.25	3.71	
Hazardous Air Pollutant (HAP)					
1,3-Butadiene	0.002	0.002	16.595	0.008	HAP, TAP, TRI
Acetaldehyde	0.059	0.059	519.592	0.260	HAP, TAP, TRI
Acrolein	0.036	0.036	319.462	0.160	HAP, TAP, TRI
Benzene	0.003	0.003	27.347	0.014	TAP, HAP, TRI
Biphenyl	0.002	0.002	13.176	0.007	HAP, TAP, TRI
Carbon Tetrachloride	0.000	0.000	2.281	0.001	HAP, TAP, TRI
Chlorobenzene	0.000	0.000	1.889	0.001	HAP, TAP, TRI
Chloroform	0.000	0.000	1.771	0.001	HAP, TAP, TRI
1,3-Dichloropropene	0.000	0.000	1.641	0.001	HAP, TAP, TRI
Ethylbenzene	0.000	0.000	2.467	0.001	HAP, TAP, TRI
Ethylene Dibromide	0.000	0.000	2.753	0.001	HAP, TAP, TRI
Formaldehyde	0.248	0.248	2,172.657	1.086	HAP, TAP, TRI
Methanol	0.018	0.018	155.381	0.078	HAP, TAP, TRI
Methylene Chloride	0.000	0.000	1.243	0.001	HAP, TAP, TRI
2-Methylnaphthalene	0.000	0.000	2.063	0.001	TAP
n-Hexane	0.008	0.008	68.989	0.034	HAP, TAP, TRI
Naphthalene	0.001	0.001	4.624	0.002	HAP, TRI, PAH
Styrene	0.000	0.000	1.467	0.001	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	0.000	0.000	2.486	0.001	HAP, TAP, TRI
Toluene	0.003	0.003	25.358	0.013	TAP, TRI
1,1,2-Trichloroethane	0.000	0.000	1.976	0.001	HAP, TAP, TRI
2,2,4-Trimethylpentane	0.002	0.002	15.538	0.008	HAP, TAP, TRI
Xylenes	0.001	0.001	11.436	0.006	TAP, HAP, TRI
Total Speciated VOCs	0.386	0.386	3,381.167	1.691	
Total Speciated TAP	0.386	0.386	3,381.228	1.691	
Total Speciated PAH	0.000	0.000	1.679	0.001	
Total Naphthalenes	0.001	0.001	6.688	0.003	

Engine Emissions
 T Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION					
Source Description:	CAT G3606 Compressor Engine				
TEMPO ID:	EQT0014	Construction Year:	2022	Regulation:	MACT ZZZZ; NSPS JJJJ
Source ID No:	10-22	Manufacturer:	Caterpillar	Calculated by:	C. Giambrone
Location:	Ajax	Classification:	4SLB	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Power Rating (avg):	1,875.00	HP	Engine Dataplate
Power Rating (avg):	1,399.25	KW	KW = HP / 1.34
Power Rating (max):	1,875.00	HP	Assumed to be same as average from Engine Dataplate
Operating Hours:	8,760.00	Hours/Year	
Firing Rate:	14.19	MMBTU/hr	MMBTU/hr = BSFC x Power Rating / 1,000,000
BSFC:	7,568.00	BTU/hp-hr	Per Historical Enable Data
NG Heat Content:	1,020.00	BTU/scf	AP-42 Table 3.2-1 footnote b
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.5000	g/bhp-hr	Vendor	
CO	0.1540	g/bhp-hr	Vendor	
PM ₁₀	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
PM _{2.5}	0.0100	lb/MMBTU	AP-42 3.2-2	Filterable + Condensable
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.2050	g/bhp-hr	Vendor	
Hazardous Air Pollutant (HAP)				
1,3-Butadiene	1.34E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acetaldehyde	4.18E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Acrolein	2.57E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Benzene	2.20E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Biphenyl	1.06E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Carbon Tetrachloride	1.84E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chlorobenzene	1.52E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Chloroform	1.43E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,3-Dichloropropene	1.32E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylbenzene	1.99E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Ethylene Dibromide	2.22E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Formaldehyde	6.00E-02	g/bhp-hr	Vendor	HAP, TAP, TRI
Methanol	1.25E-03	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Methylene Chloride	1.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2-Methylnaphthalene	1.66E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP
n-Hexane	5.55E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Naphthalene	3.72E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TRI, PAH
Styrene	1.18E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
1,1,2,2-Tetrachloroethane	2.00E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Toluene	2.04E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, TRI
1,1,2-Trichloroethane	1.59E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
2,2,4-Trimethylpentane	1.25E-04	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	HAP, TAP, TRI
Xylenes	9.20E-05	lb/MMBTU	AP-42 3.2-2 w/ 50% DRE	TAP, HAP, TRI
Total Speciated VOCs	0.0697	lb/MMBTU		
Total Speciated TAP	0.0697	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0001	lb/MMBTU		

MISSION RATES						
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:	
Criteria						
NOx	2.07	2.07	18,105.48	9.05		
CO	0.64	0.64	5,576.49	2.79		
PM ₁₀	0.14	0.14	1,241.44	0.62		
PM _{2.5}	0.14	0.14	1,241.44	0.62		
SO ₂	0.07	0.07	607.59	0.30		
VOC (Total)	0.85	0.85	7,423.25	3.71		
Hazardous Air Pollutant (HAP)						
1,3-Butadiene	0.002	0.002	16.595	0.008	HAP, TAP, TRI	
Acetaldehyde	0.059	0.059	519.592	0.260	HAP, TAP, TRI	
Acrolein	0.036	0.036	319.462	0.160	HAP, TAP, TRI	
Benzene	0.003	0.003	27.347	0.014	TAP, HAP, TRI	
Biphenyl	0.002	0.002	13.176	0.007	HAP, TAP, TRI	
Carbon Tetrachloride	0.000	0.000	2.281	0.001	HAP, TAP, TRI	
Chlorobenzene	0.000	0.000	1.889	0.001	HAP, TAP, TRI	
Chloroform	0.000	0.000	1.771	0.001	HAP, TAP, TRI	
1,3-Dichloropropene	0.000	0.000	1.641	0.001	HAP, TAP, TRI	
Ethylbenzene	0.000	0.000	2.467	0.001	HAP, TAP, TRI	
Ethylene Dibromide	0.000	0.000	2.753	0.001	HAP, TAP, TRI	
Formaldehyde	0.248	0.248	2,172.657	1.086	HAP, TAP, TRI	
Methanol	0.018	0.018	155.381	0.078	HAP, TAP, TRI	
Methylene Chloride	0.000	0.000	1.243	0.001	HAP, TAP, TRI	
2-Methylnaphthalene	0.000	0.000	2.063	0.001	TAP	
n-Hexane	0.008	0.008	68.989	0.034	HAP, TAP, TRI	
Naphthalene	0.001	0.001	4.624	0.002	HAP, TRI, PAH	
Styrene	0.000	0.000	1.467	0.001	HAP, TAP, TRI	
1,1,2,2-Tetrachloroethane	0.000	0.000	2.486	0.001	HAP, TAP, TRI	
Toluene	0.003	0.003	25.358	0.013	TAP, TRI	
1,1,2-Trichloroethane	0.000	0.000	1.976	0.001	HAP, TAP, TRI	
2,2,4-Trimethylpentane	0.002	0.002	15.538	0.008	HAP, TAP, TRI	
Xylenes	0.001	0.001	11.436	0.006	TAP, HAP, TRI	
Total Speciated VOCs	0.386	0.386	3,381.167	1.691		
Total Speciated TAP	0.386	0.386	3,381.228	1.691		
Total Speciated PAH	0.000	0.000	1.679	0.001		
Total Naphthalenes	0.001	0.001	6.688	0.003		

Reboilers

Reboiler Emissions
 ET Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	CO ₂ Dehydrator Reboiler		
TEMPO ID:	TBD		
Source ID No:	5-23B	Calculated by:	C. Giambone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	1.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	1.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	1.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0980	lb/MMBTU	1998 AP-42, Table 1.4-1	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	0.10	0.10	858.82	0.43	
CO	0.08	0.08	721.41	0.36	
PM ₁₀	0.01	0.01	65.27	0.03	
PM _{2.5}	0.01	0.01	65.27	0.03	
SO ₂	0.00	0.00	42.82	0.02	
VOC (Total)	0.01	0.01	47.24	0.02	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.002	0.002	15.459	0.008	HAP, TAP, TRI
Total Speciated VOCs	0.002	0.002	16.166	0.008	
Total Speciated TAP	0.002	0.002	16.508	0.008	
Total Speciated PAH	0.000	0.000	0.001	0.000	
Total Naphthalenes	0.000	0.000	0.005	0.000	

Boiler Emissions
 Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 1 Amine Hot Oil Heater		
TEMPO ID:	EQT0002		
Source ID No:	1-22B	Calculated by:	C. Giambone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	85.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	85.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	85.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Vendor	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Benzene	2.06E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Formaldehyde	7.35E-05	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Toluene	3.33E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	5.48	5.48	48,026.70	24.01	
CO	7.00	7.00	61,320.00	30.66	
PM ₁₀	0.63	0.63	5,548.00	2.77	
PM _{2.5}	0.63	0.63	5,548.00	2.77	
SO ₂	0.42	0.42	3,639.55	1.82	
VOC (Total)	0.46	0.46	4,015.00	2.01	
Hazardous Air Pollutant (HAP)					
Benzene	0.000	0.000	1.533	0.001	HAP, TAP, TRI
Formaldehyde	0.006	0.006	54.750	0.027	HAP, TAP, TRI
Hexane (n-)	0.150	0.150	1,314.000	0.657	HAP, TAP, TRI
Toluene	0.000	0.000	2.482	0.001	HAP, TAP, TRI
Total Speciated VOCs	0.157	0.157	1,374.151	0.687	
Total Speciated TAP	0.160	0.160	1,403.212	0.702	
Total Speciated PAH	0.000	0.000	0.047	0.000	
Total Naphthalenes	0.000	0.000	0.463	0.000	

Reboiler Emissions
 Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 1 Glycol Dehy Reboiler		
TEMPO ID:	EQT0004		
Source ID No:	2-22B	Calculated by:	C. Giambrone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	5.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	5.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	5.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Vendor	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Benzene	2.06E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Formaldehyde	7.35E-05	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Toluene	3.33E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	0.32	0.32	2,825.10	1.41	
CO	0.41	0.41	3,607.06	1.80	
PM ₁₀	0.04	0.04	326.35	0.16	
PM _{2.5}	0.04	0.04	326.35	0.16	
SO ₂	0.02	0.02	214.09	0.11	
VOC (Total)	0.03	0.03	236.18	0.12	
Hazardous Air Pollutant (HAP)					
Formaldehyde	0.000	0.000	3.221	0.002	HAP, TAP, TRI
Hexane (n-)	0.009	0.009	77.294	0.039	HAP, TAP, TRI
Total Speciated VOCs	0.009	0.009	80.832	0.040	
Total Speciated TAP	0.009	0.009	82.542	0.041	
Total Speciated PAH	0.000	0.000	0.003	0.000	
Total Naphthalenes	0.000	0.000	0.027	0.000	

Boiler Emissions
 Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 2 Amine Hot Oil Heater		
TEMPO ID:	EQT0006		
Source ID No:	3-22B	Calculated by:	C. Giambrone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	85.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	85.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	85.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Vendor	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Benzene	2.06E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Formaldehyde	7.35E-05	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Toluene	3.33E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	5.48	5.48	48,026.70	24.01	
CO	7.00	7.00	61,320.00	30.66	
PM ₁₀	0.63	0.63	5,548.00	2.77	
PM _{2.5}	0.63	0.63	5,548.00	2.77	
SO ₂	0.42	0.42	3,639.55	1.82	
VOC (Total)	0.46	0.46	4,015.00	2.01	
Hazardous Air Pollutant (HAP)					
Benzene	0.000	0.000	1.533	0.001	HAP, TAP, TRI
Formaldehyde	0.006	0.006	54.750	0.027	HAP, TAP, TRI
Hexane (n-)	0.150	0.150	1,314.000	0.657	HAP, TAP, TRI
Toluene	0.000	0.000	2.482	0.001	HAP, TAP, TRI
Total Speciated VOCs	0.157	0.157	1,374.151	0.687	
Total Speciated TAP	0.160	0.160	1,403.212	0.702	
Total Speciated PAH	0.000	0.000	0.047	0.000	
Total Naphthalenes	0.000	0.000	0.463	0.000	

boiler Emissions
 Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 2 Glycol Dehy Reboiler		
TEMPO ID:	EQT0008		
Source ID No:	4-22B	Calculated by:	C. Giambrone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	5.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	5.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	5.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Vendor	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Benzene	2.06E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Formaldehyde	7.35E-05	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Toluene	3.33E-06	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	0.32	0.32	2,825.10	1.41	
CO	0.41	0.41	3,607.06	1.80	
PM ₁₀	0.04	0.04	326.35	0.16	
PM _{2.5}	0.04	0.04	326.35	0.16	
SO ₂	0.02	0.02	214.09	0.11	
VOC (Total)	0.03	0.03	236.18	0.12	
Hazardous Air Pollutant (HAP)					
Formaldehyde	0.000	0.000	3.221	0.002	HAP, TAP, TRI
Hexane (n-)	0.009	0.009	77.294	0.039	HAP, TAP, TRI
Total Speciated VOCs	0.009	0.009	80.832	0.040	
Total Speciated TAP	0.009	0.009	82.542	0.041	
Total Speciated PAH	0.000	0.000	0.003	0.000	
Total Naphthalenes	0.000	0.000	0.027	0.000	

Loading

Sulfur Loading Emissions
ET Gathering & Processing LLC
Ajax Amine Plant

SOURCE INFORMATION	
Source Description:	Sulfur Loading and Handling
TEMPO ID:	TBD
Source ID No:	3-23
Location:	Ajax

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes:
Average Operating Rate:	182.50	tons/yr	1,000 lb/day Sulfur
Operating Time:	8,760	hr/yr	
Mean Wind Speed:	7.2	mph	AP-42, Table 7.1-7 (Shreveport, LA)
Material Moisture Content:	15	%	Provided by Enable
Material Silt Content:	4.9	%	AP-42, Table 13.2.4-1 (Assumed Coke Breeze, Fine Coke)
Precipitation:	100	# Days w/ 0.01" Precip.	AP-42, Figure 13.2.2-1
Time Wind Speed > 12 mph:	15	%	Engineering Estimate (Based on Shreveport Max 2018-2022)
Pile Size:	0.004	acres	22' x 8'
Control Efficiency:	0%	%	Engineering Estimate

EMISSION FACTORS & RATES - SULFUR PILE LOAD-IN							
Pollutant	Particle Size Multiplier ¹	Mean Wind Speed (mph)	Moisture Content (%)	Calculated Uncontrolled Emission Factor (lb/ton of Sulfur) ²	Average Annual Operating Rate (tons/yr)	Control Efficiency (%)	Annual Emissions ²
	k	U	M	E	ORavg	ce	(tons/yr)
PM	0.74	7.2	15	2.27E-04	182.50	0%	2.07E-05
PM ₁₀	0.35	7.2	15	1.07E-04	182.50	0%	9.78E-06
PM _{2.5}	0.053	7.2	15	1.62E-05	182.50	0%	1.48E-06

EMISSION FACTORS & RATES - SULFUR PILE WIND EROSION							
Pollutant	Material Silt Content (%)	No. Days w/ 0.01" Precip. (days)	Percent of Time Wind Speed > 12 mph (%)	Calculated Uncontrolled Emission Factor ³ (lb/day/acre)	Pile Size (acre)	Control Efficiency (%)	Annual Emissions ³
	s	p	r	E	OR	ce	(tons/yr)
PM	4.9	100	15	6.26	0.004	0%	4.62E-03
PM ₁₀	4.9	100	15	6.26	0.004	0%	4.62E-03
PM _{2.5}	4.9	100	15	6.26	0.004	0%	4.62E-03

EMISSION RATES SUMMARY - SULFUR PILE LOAD-IN & WIND EROSION				
Pollutant	Percent Total	Average Hourly Emissions (lb/hr)	Annual Emissions (tons/yr)	Notes
PM	-	0.001	0.005	
PM ₁₀	-	0.001	0.005	
PM _{2.5}	-	0.001	0.005	

Notes:

¹ Particle Size Multiplier, k, was obtained from AP-42, Section 13.2.4.3.

² Emission Factor, E (lb/ton of Sulfur) = $k(0.0032) \times (U/5)^{1.3} / (M/2)^{1.4}$; AP-42 Section 13.2.4.5;
 Average Annual Uncontrolled Emissions (lb/yr) = E x ORavg;
 Average Annual Controlled Emissions (tons/yr) = Average Annual Uncontrolled Emissions (lb/yr) x (1 - ce)

³ Emission Factor, E (lb/day/acre) = $1.7 \times (s/1.5) \times (365-p) / 235 \times (r/15)$; Table 21 of EPA Air/Superfund National Technical Guidance Study Series - Volume III, January 1989;
 Average Annual Uncontrolled Emissions (lb/yr) = E x OR;
 Average Annual Controlled Emissions (tons/yr) = Average Annual Uncontrolled Emissions (lb/yr) x (1 - ce)

Carbon Capture Produced Water Loading Emissions
ET Gathering & Processing LLC
Ajax Amine Plant

Material Name	Vapor Fraction ¹	Saturation Factor ² (S)	True Vapor Pressure (P) (psia)	Molecular Weight of Vapors (M) (lb/lb-mole)	Temp of Loaded Liquid (F)	Emission Factor ² (lb VOC/10 ³ gal)	Estimated Hourly Throughput ³ (gal)	Annual Throughput ³ (gals)	Hourly Emissions ⁴ (lb/hr)	Annual Emissions ⁵ (T/yr)
Produced Water	N/A	0.6	0.40	18	67.41	0.103	8,400	3,066,000	0.86	0.16
Condensate	0.10	N/A	N/A	N/A	N/A	N/A	N/A	N/A	0.09	0.02
Water	0.90	N/A	N/A	N/A	N/A	N/A	N/A	N/A	0.78	0.14

Notes:

¹ As taken from produced water storage tank calculation (EPN: 6-23 & EPN: 7-23)

² Per AP-42, 5th Edition (6/08), Section 5.2, Equation 1, Emission Factor (lb VOC/10³ gal) = 12.46 x [(S x P x M)/(F+460)], S = Submerged loading: dedicated normal service

³ Annual Throughput is the amount of produced water loaded out from Carbon Capture Project Produced Water Tanks. Hourly Throughput is the amount of produced water loaded out in one (1) truck load.

⁴ Hourly Emissions = Hourly Throughput / 1000 x Emission Factor

⁵ Annual Emissions = Annual Throughput / 1000 x Emission Factor / 2000 lb/T

Storage Tanks

TankESP
Emissions Report - Detail Format
Tank Identification and Physical Characteristics
6-23

Identification
 User Identification: 6-23
 City: Ajax
 State: Louisiana
 Company: ET Gathering & Processing LLC
 Type of Tank: FRT (no floating roof)
 Description: Energy Transfer - Ajax PTE

Tank Dimensions
 Shell Height (ft): 22.06
 Diameter (ft): 18.00
 Liquid Height (ft): 21.06
 Avg. Liquid Height (ft): 11.03
 Volume (gallons): 41,992.43
 Turnovers: 80.58
 Net Throughput(gal/yr): 3,076,920.00
 Is Tank Insulated (y/n): N

Paint Characteristics
 Shell Color/Shade: Light Gray Paint
 Shell Condition: Average
 Roof Color/Shade: Light Gray Paint
 Roof Condition: Average

Roof Characteristics
 Type: Column-Supported (Cone)
 Height (ft): 0.56
 Roof Slope (ft/ft): 0.06

Breather Vent Settings
 Vacuum Settings (psig): -0.03
 Pressure Settings (psig): 0.03

Meteorological Data used in Emissions Calculations: Alexandria, LA (Avg Atmospheric Pressure = 14.63 psia)

TankESP
Emissions Report - Detail Format
Liquid Contents of Storage Tank

6-23 - Vertical Fixed Roof Tank
Ajax, Louisiana

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg. F)			Liquid Bulk	Vapor Pressure (psia)			Vapor Mol.	Liquid Mass	Vapor Mass	Mol. Weight. Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.	Temp (deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	
Produced Water	All	71.00	63.17	78.84	68.72	0.3859	0.2955	0.4998	0.0000			0.00 N/A
Condensate									66.0000	1.0000	10.0906	82.00 Option 2: A=6.806, B=1276.2, C=273.15
Water									18.0200	99.0000	89.9094	18.02 Option 2: A=8.277, B=1838.7, C=241.41

TankESP
Emissions Report - Detail Format
Detail Calculations (AP-42)

6-23 - Vertical Fixed Roof Tank
Ajax, Louisiana

Annual Emission Calculations

Standing Losses (lb):	76.9341
Vapor Space Volume (cu ft):	2,854.5061
Vapor Density (lb/cu ft):	0.0000
Vapor Space Expansion Factor:	0.0692
Vented Vapor Saturation Factor:	0.8134

Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	2,854.5061
Tank Diameter (ft):	18.0000
Vapor Space Outage (ft):	11.2175
Tank Shell Height (ft):	22.0600
Average Liquid Height (ft):	11.0300
Roof Outage (ft):	0.1875

Roof Outage (Cone Roof)	
Roof Outage (ft):	0.1875
Roof Height (ft):	0.5625
Roof Slope (ft/ft):	0.0625
Shell Radius (ft):	9.0000

Vapor Density	
Vapor Density (lb/cu ft):	0.0000
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Daily Avg. Liquid Surface Temp. (deg. R):	71.0044
Daily Average Ambient Temp. (deg. F):	66.2492
Ideal Gas Constant R (psia cu ft / (lb-mol-deg R)):	10.7310
Liquid Bulk Temperature (deg. R):	68.7178
Tank Paint Solar Absorptance (Shell):	0.5800
Tank Paint Solar Absorptance (Roof):	0.5800
Daily Total Solar Insulation Factor (Btu/sqft day):	1,418.7669

Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.0692
Daily Vapor Temperature Range (deg. R):	31.3382
Daily Vapor Pressure Range (psia):	0.2043
Breather Vent Press. Setting Range (psia):	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psi)	0.2955
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psi)	0.4998
Daily Avg. Liquid Surface Temp. (deg R):	71.0044
Daily Min. Liquid Surface Temp. (deg R):	63.1699
Daily Max. Liquid Surface Temp. (deg R):	78.8390
Daily Ambient Temp. Range (deg. R):	21.9311

Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	0.8134
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Vapor Space Outage (ft):	11.2175

Working Losses (lb):	290.8914
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Annual Net Throughput (gal/yr.):	3,076,920.0000
Annual Turnovers:	80.5786
Turnover Factor:	0.5390
Maximum Liquid Volume (gal):	41,992.4319
Maximum Liquid Height (ft):	21.0600
Tank Diameter (ft):	18.0000
Working Loss Product Factor:	1.0000
Total Losses (lb):	367.8255

TankESP
Emissions Report - Detail Format
Tank Identification and Physical Characteristics
7-23

Identification
 User Identification: 7-23
 City: Ajax
 State: Louisiana
 Company: ET Gathering & Processing LLC
 Type of Tank: FRT (no floating roof)
 Description: Energy Transfer - Ajax PTE

Tank Dimensions
 Shell Height (ft): 22.06
 Diameter (ft): 18.00
 Liquid Height (ft) : 21.06
 Avg. Liquid Height (ft): 11.03
 Volume (gallons): 41,992.43
 Turnovers: 80.58
 Net Throughput(gal/yr): 3,076,920.00
 Is Tank Insulated (y/n): N

Paint Characteristics
 Shell Color/Shade: Light Gray Paint
 Shell Condition: Average
 Roof Color/Shade: Light Gray Paint
 Roof Condition: Average

Roof Characteristics
 Type: Column-Supported (Cone)
 Height (ft) 0.56
 Roof Slope (ft/ft) 0.06

Breather Vent Settings
 Vacuum Settings (psig): -0.03
 Pressure Settings (psig): 0.03

Meteorological Data used in Emissions Calculations: Alexandria, LA (Avg Atmospheric Pressure = 14.63 psia)

TankESP
Emissions Report - Detail Format
Liquid Contents of Storage Tank

7-23 - Vertical Fixed Roof Tank
 Ajax, Louisiana

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg. F)			Liquid Bulk	Vapor Pressure (psia)			Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.	Temp (deg F)	Avg.	Min.	Max.					
Produced Water	All	71.00	63.17	78.84	68.72	0.3859	0.2955	0.4998	0.0000			0.00	N/A
Condensate									66.0000	1.0000	10.0906	92.00	Option 2: A=6.806, B=1276.2, C=273.15
Water									18.0200	99.0000	89.9094	18.02	Option 2: A=8.277, B=1838.7, C=241.41

TankESP

Emissions Report - Detail Format
Detail Calculations (AP-42)7-23 - Vertical Fixed Roof Tank
Ajax, Louisiana

Annual Emission Calculations

Standing Losses (lb):	76.9341
Vapor Space Volume (cu ft):	2,854.5061
Vapor Density (lb/cu ft):	0.0000
Vapor Space Expansion Factor:	0.0692
Vented Vapor Saturation Factor:	0.8134

Tank Vapor Space Volume:

Vapor Space Volume (cu ft):	2,854.5061
Tank Diameter (ft):	18.0000
Vapor Space Outage (ft):	11.2175
Tank Shell Height (ft):	22.0600
Average Liquid Height (ft):	11.0300
Roof Outage (ft):	0.1875

Roof Outage (Cone Roof)

Roof Outage (ft):	0.1875
Roof Height (ft):	0.5625
Roof Slope (ft/ft):	0.0625
Shell Radius (ft):	9.0000

Vapor Density

Vapor Density (lb/cu ft):	0.0000
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Daily Avg. Liquid Surface Temp. (deg. R):	71.0044
Daily Average Ambient Temp. (deg. F):	66.2492
Ideal Gas Constant R (psia cu/ft / (lb-mol-deg R)):	10.7310
Liquid Bulk Temperature (deg. R):	68.7178
Tank Paint Solar Absorptance (Shell):	0.5800
Tank Paint Solar Absorptance (Roof):	0.5800
Daily Total Solar Insulation Factor (Btu/sqft day):	1,418.7669

Vapor Space Expansion Factor

Vapor Space Expansion Factor:	0.0692
Daily Vapor Temperature Range (deg. R):	31.3382
Daily Vapor Pressure Range (psia):	0.2043
Breather Vent Press. Setting Range (psia):	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psi)	0.2955
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psi)	0.4998
Daily Avg. Liquid Surface Temp. (deg. R):	71.0044
Daily Min. Liquid Surface Temp. (deg. R):	63.1699
Daily Max. Liquid Surface Temp. (deg. R):	78.8390
Daily Ambient Temp. Range (deg. R):	21.9311

Vented Vapor Saturation Factor

Vented Vapor Saturation Factor:	0.8134
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Vapor Space Outage (ft):	11.2175

Working Losses (lb):	290.8914
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psi)	0.3859
Annual Net Throughput (gal/yr):	3,076,920.0000
Annual Turnovers:	80.5786
Turnover Factor:	0.5390
Maximum Liquid Volume (gal):	41,992.4319
Maximum Liquid Height (ft):	21.0600
Tank Diameter (ft):	18.0000
Working Loss Product Factor:	1.0000
Total Losses (lb):	367.8255

Thermal Oxidizers

Thermal Oxidizer Emissions
 ET Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 1 Thermal Oxidizer		
TEMPO ID:	EQT0009		
Source ID No:	5-22	Calculated by:	C. Giambone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	33.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	33.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	33.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP
Destruction Efficiency (ThOx):	98%	%	

FACTORS AND BASIS - NG COMBUSTION				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Manufacturer Data	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES - NG COMBUSTION (ThOx Control)					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.13	2.13	18,645.66	9.32	
CO	2.72	2.72	23,806.59	11.90	
PM ₁₀	0.25	0.25	2,153.93	1.08	
PM _{2.5}	0.25	0.25	2,153.93	1.08	
SO ₂	0.16	0.16	1,413.00	0.71	
VOC (Total)	0.18	0.18	1,558.76	0.78	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.058	0.058	510.141	0.255	HAP, TAP, TRI
Total Speciated VOCs	0.061	0.061	533.494	0.267	
Total Speciated TAP	0.062	0.062	544.776	0.272	
Total Speciated PAH	0.000	0.000	0.018	0.000	
Total Naphthalenes	0.000	0.000	0.180	0.000	

UNCONTROLLED WASTE STREAMS BASIS - WASTE STREAMS TO CONTROL (ThOx)					
Pollutant	Plant 1 Amine Unit		Plant 1 Glycol Dehy Unit		Notes:
	Flash Vent	Acid Gas Vent	Flash Vent	BTEX Vent	
	Tons/Year	Tons/Year	Tons/Year	Tons/Year	
Criteria					
VOC (Total)	0.16	0.01	0.13	0.44	
H ₂ S	0.00	61.44	0.00	0.00	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.03	0.00	0.07	0.36	

EMISSION RATES - ThOx CONTROLLED WASTE STREAMS					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
VOC (Total)	0.00	0.00	29.54	0.01	
H ₂ S	0.28	0.28	2,457.61	1.23	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.00	0.00	18.13	0.01	HAP, TAP, TRI
EMISSION RATES - TOTAL					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.13	2.13	18,645.66	9.32	
CO	2.72	2.72	23,806.59	11.90	
PM ₁₀	0.25	0.25	2,153.93	1.08	
PM _{2.5}	0.25	0.25	2,153.93	1.08	
SO ₂	26.04	26.04	228,091.26	114.05	
VOC (Total)	0.18	0.18	1,588.30	0.79	
H ₂ S	0.28	0.28	2,457.61	1.23	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.060	0.060	528.271	0.264	HAP, TAP, TRI
Total Speciated VOCs	0.065	0.065	565.355	0.283	
Total Speciated TAP	0.066	0.066	576.638	0.288	
Total Speciated PAH	0.001	0.001	5.438	0.003	
Total Naphthalenes	0.000	0.000	0.180	0.000	

Thermal Oxidizer Emissions
 Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Plant 2 Thermal Oxidizer		
TEMPO ID:	EQT0010		
Source ID No:	6-22	Calculated by:	C. Giambrone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Burner:	33.00	MMBTU/hr (HHV)	Design
Firing Rate - Pilot:	0.00	MMBTU/hr (HHV)	Pilot Included in Design
Firing Rate - Annual (Avg):	33.00	MMBTU/hr (HHV)	Design
Firing Rate - Hourly (Max):	33.00	MMBTU/hr (HHV)	Design
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP
Destruction Efficiency (ThOx):	98%	%	

FACTORS AND BASIS - NG COMBUSTION				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0645	lb/MMBTU	Manufacturer Data	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	
Hazardous Air Pollutant (HAP)				
Hexane (n-)	1.76E-03	lb/MMBTU	1998 AP-42, Table 1.4-3	HAP, TAP, TRI
Total Speciated VOCs	0.0018	lb/MMBTU		
Total Speciated TAP	0.0019	lb/MMBTU		
Total Speciated PAH	0.0000	lb/MMBTU		
Total Naphthalenes	0.0000	lb/MMBTU		

EMISSION RATES - NG COMBUSTION (ThOx Control)					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.13	2.13	18,645.66	9.32	
CO	2.72	2.72	23,806.59	11.90	
PM ₁₀	0.25	0.25	2,153.93	1.08	
PM _{2.5}	0.25	0.25	2,153.93	1.08	
SO ₂	0.16	0.16	1,413.00	0.71	
VOC (Total)	0.18	0.18	1,558.76	0.78	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.058	0.058	510.141	0.255	HAP, TAP, TRI
Total Speciated VOCs	0.061	0.061	533.494	0.267	
Total Speciated TAP	0.062	0.062	544.776	0.272	
Total Speciated PAH	0.000	0.000	0.018	0.000	
Total Naphthalenes	0.000	0.000	0.180	0.000	

UNCONTROLLED WASTE STREAMS BASIS - WASTE STREAMS TO CONTROL (ThOx)					
Pollutant	Plant 2 Amine Unit		Plant 2 Glycol Dehy Unit		Notes:
	Flash Vent	Acid Gas Vent	Flash Vent	BTEX Vent	
	Tons/Year	Tons/Year	Tons/Year	Tons/Year	
Criteria					
VOC (Total)	0.16	0.01	0.13	0.44	
H ₂ S	0.00	61.44	0.00	0.00	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.03	0.00	0.07	0.36	

EMISSION RATES - ThOx CONTROLLED WASTE STREAMS

Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
VOC (Total)	0.00	0.00	29.54	0.01	
H ₂ S	0.28	0.28	2,457.61	1.23	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.00	0.00	18.13	0.01	HAP, TAP, TRI

EMISSION RATES - TOTAL

Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	2.13	2.13	18,645.66	9.32	
CO	2.72	2.72	23,806.59	11.90	
PM ₁₀	0.25	0.25	2,153.93	1.08	
PM _{2.5}	0.25	0.25	2,153.93	1.08	
SO ₂	26.04	26.04	228,091.26	114.05	
VOC (Total)	0.18	0.18	1,588.30	0.79	
H ₂ S	0.28	0.28	2,457.61	1.23	
Hazardous Air Pollutant (HAP)					
Hexane (n-)	0.060	0.060	528.271	0.264	HAP, TAP, TRI
Total Speciated VOCs	0.065	0.065	565.355	0.283	
Total Speciated TAP	0.066	0.066	576.638	0.288	
Total Speciated PAH	0.001	0.001	5.438	0.003	
Total Naphthalenes	0.000	0.000	0.180	0.000	

Flares

Flare Emissions
 T Gathering & Processing LLC
 Ajax Amine Plant

SOURCE INFORMATION			
Source Description:	Flare		
TEMPO ID:	EQT0023		
Source ID No:	19-22	Calculated by:	C. Giambrone
Location:	Ajax	Calculation Date:	September 1, 2023

OPERATING PARAMETERS			
Parameter	Rate	Eng Units	Basis & Notes
Firing Rate - Pilot Hourly:	0.10	MMBTU/hr (HHV)	Design
Firing Rate - Blanket Gas Hourly:	17.18	MMBTU/hr (HHV)	Based on the volume of 4 750-bbl tanks venting to the flare in 1 hour
Firing Rate - Total Hourly:	17.28	MMBTU/hr (HHV)	Pilot Flow + Blanket Flow
Firing Rate - Total Hourly (Max):	17.28	MMBTU/hr (HHV)	Pilot Flow + Blanket Flow
Firing Rate - Pilot Annualy:	884.58	MMBTU/yr (HHV)	Design
Firing Rate - Blanket Gas Annualy:	206.12	MMBTU/yr (HHV)	Based on tanks venting to flare once per month
Firing Rate - Total Annual (Avg):	1,090.71	MMBTU/yr (HHV)	Pilot Flow + Blanket Flow
Operating Hours:	8,760.00	Hours/Year	
Heat Content:	1,020.00	BTU/scf	Average HHV of Natural Gas
Ideal Gas Molar Volume:	385.50	scf/lbmol	Constant (Molar Volume of an Ideal Gas) at STP

FACTORS AND BASIS				
Pollutant	Value	Unit	Basis	Notes
Criteria				
NOx	0.0980	lb/MMBTU	1998 AP-42, Table 1.4-1	
CO	0.0824	lb/MMBTU	1998 AP-42, Table 1.4-1	
PM ₁₀	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
PM _{2.5}	0.0075	lb/MMBTU	1998 AP-42, Table 1.4-2	
SO ₂	0.0049	lb/MMBTU	30 ppmw Mass Balance	
VOC (Total)	0.0054	lb/MMBTU	1998 AP-42, Table 1.4-2	

EMISSION RATES					
Pollutant	Lbs/Hour (avg)	Lbs/Hour (max)	Lbs/Year	Tons/Year	Notes:
Criteria					
NOx	0.01	1.69	106.93	0.05	
CO	0.01	1.42	89.82	0.04	
PM ₁₀	0.00	0.13	8.13	0.00	
PM _{2.5}	0.00	0.13	8.13	0.00	
SO ₂	0.00	0.08	5.33	0.00	
VOC (Total)	0.00	0.09	5.88	0.00	

Fugitives

Fugitive Emissions
ET Gathering & Processing LLC
Ajax Amine Plant

Fugitive Component Counts

Component Type	Type of Service	Emission Factors (lb/hr-component) ¹	VOC Fraction	Number of Components Per Service				
				Existing	Acid Gas	CO2	NG	Produced Water
Valves	Gas/Vapor	9.92E-03	1%	990	119	270	95	-
	Heavy Oil	1.85E-05	100%	99	-	-	-	117
	Light Oil	5.51E-03	5%	99	-	15	-	-
Connectors	Gas/Vapor	4.41E-04	1%	-	140	234	69	-
	Heavy Oil	1.65E-05	100%	109	-	-	-	84
	Light Oil	4.63E-04	5%	109	-	-	-	-
Flanges	Gas/Vapor	8.60E-04	1%	1,089	-	-	-	-
	Heavy Oil	8.60E-07	100%	-	-	-	-	-
	Light Oil	2.43E-04	5%	-	-	-	-	-
Pump Seals	Gas/Vapor	5.29E-03	1%	396	-	-	-	-
	Heavy Oil	-	100%	6	-	-	-	-
	Light Oil	2.87E-02	5%	28	4	-	-	-
Other	Gas/Vapor	1.94E-02	1%	100	17	30	6	-
	Heavy Oil	7.05E-05	100%	10	-	-	-	-
	Light Oil	1.65E-02	5%	10	2	1	1	-
Open-ended Lines	Gas/Vapor	4.41E-03	1%	-	3	1	-	-
	Heavy Oil	3.09E-04	100%	-	-	-	-	-
	Light Oil	3.09E-03	5%	-	-	-	-	-

Stream Speciation

Constituent (as a function of VOC content)	Weight Percent				
	Existing	Acid Gas	CO2	NG	Produced Water
Benzene	6%	6%	0.001%	0%	0%
Toluene	6%	6%	0.001%	0%	0%
Ethylbenzene	6%	6%	0.001%	0%	0%
Xylene	6%	6%	0.001%	0%	0%
Hydrogen Sulfide	0.01%	0.01%	0.000%	0.01%	0%

Stream Emissions Summary

Constituent	Emissions (lb/hr)				
	Existing	Acid Gas	CO2	NG	Produced Water
Benzene	0.01	0.00	0.00	-	-
Toluene	0.01	0.00	0.00	-	-
Ethylbenzene	0.01	0.00	0.00	-	-
Xylene	0.01	0.00	0.00	-	-
Hydrogen Sulfide	0.00	0.00	-	0.00	-
Total VOC	0.23	0.02	0.04	0.01	0.00

Overall Emissions Summary

Constituent	Emissions ²	
	lb/hr	tpy
Benzene	0.01	0.07
Toluene	0.02	0.07
Ethylbenzene	0.01	0.07
Xylene	0.02	0.07
Hydrogen Sulfide	0.00	0.00
Total VOC	0.31	1.35

Notes:

- 1 Emission factors based on EPA's Protocol for Equipment Leak Emission Estimates Document (EPA-435/R-95-017, November 1995) Table 2-4 for Oil and Gas Production Operations.
- 2 Emission rates based on 8,760 hours of operation.

Uncontrolled Vents

**Uncontrolled Amine/Dehydrator Vents
ET Gathering & Processing LLC
Ajax Amine Plant**

Uncontrolled Hours		1200	hr/yr		VOC		H2S		n-Hexane	
Source			lb/hr	tpy	lb/hr	tpy	lb/hr	tpy		
Plant 1 Amine Unit (1-22A)	Amine Flash Vent	Process Stream 72 ¹	0.04	0.02	1.28E-04	7.67E-05	0.01	0.004		
	Amine Acid Gas	Process Stream 56 ¹	0.003	1.70E-03	14.03	8.42	3.90E-04	2.34E-04		
	Total		0.04	0.02	14.03	8.42	0.01	0.004		
Plant 1 Glycol Dehydrator Unit (2-22A)	Dehy Flash Vent	Process Stream 61 ¹	0.03	0.018	1.44E-05	8.61E-06	0.02	0.009		
	Dehy BTEX Vent	Process Stream 38 ¹	0.10	0.06	6.87E-05	4.12E-05	0.08	0.05		
	Total		0.13	0.08	8.31E-05	4.98E-05	0.10	0.06		
Plant 2 Amine Unit (3-22A)	Amine Flash Vent	Process Stream 72 ¹	0.04	0.02	1.28E-04	7.67E-05	0.01	0.004		
	Amine Acid Gas	Process Stream 56 ¹	0.00	1.70E-03	14.03	8.42	3.90E-04	2.34E-04		
	Total		0.04	0.02	14.03	8.42	0.01	0.00		
Plant 2 Glycol Dehydrator Unit (4-22A)	Dehy Flash Vent	Process Stream 61 ¹	0.03	0.018	1.44E-05	8.61E-06	0.02	0.009		
	Dehy BTEX Vent	Process Stream 38 ¹	0.10	0.06	6.87E-05	4.12E-05	0.08	0.05		
	Total		0.13	0.08	8.31E-05	4.98E-05	0.10	0.06		

Notes:

¹ Uncontrolled emissions from the amine and dehy vents were calculated to account for thermal oxidizer downtime.

Insignificant Activities

TankESP

Emissions Report - Detail Format

Tank Identification and Physical Characteristics

Carbon Capture Sump

Identification

User Identification:	Carbon Capture Sump
City:	Ajax
State:	Louisiana
Company:	ET Gathering & Processing LLC
Type of Tank:	FRT (no floating roof)
Description:	Energy Transfer - Ajax PTE

Tank Dimensions

Shell Height (ft):	6.00
Diameter (ft):	5.33
Liquid Height (ft):	5.00
Avg. Liquid Height (ft):	3.00
Volume (gallons):	1,001.44
Turnovers:	17.97
Net Throughput(gal/yr):	11,999.40
Is Tank Insulated (y/n):	N

Paint Characteristics

Shell Color/Shade:	Light Gray Paint
Shell Condition:	Average
Roof Color/Shade:	Light Gray Paint
Roof Condition:	Average

Roof Characteristics

Type:	Column-Supported (Cone)
Height (ft):	0.17
Roof Slope (ft/ft):	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig):	0.03

Meteorological Data used in Emissions Calculations: Alexandria, LA (Avg Atmospheric Pressure = 14.63 psia)

TankESP
Emissions Report - Detail Format
Liquid Contents of Storage Tank

Carbon Capture Sump - Vertical Fixed Roof Tank
Ajax, Louisiana

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk	Vapor Pressure (psia)			Vapor Mol	Liquid Mass	Vapor Mass	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg	Min	Max	Temp (deg F)	Avg	Min	Max	Weight	Fract	Fract		
Produced Water	All	71.06	63.23	78.89	68.72	0.3866	0.2961	0.5006	0.0000			0.00	N/A
Condensate									66.0000	1.0000	10.0831	92.00	Option 2 A=6.806, B=1276.2, C=273.15
Water									18.0200	99.0000	89.9169	18.02	Option 2 A=6.277, B=1838.7, C=241.41

TankESP
Emissions Report - Detail Format
Detail Calculations (AP-42)

Carbon Capture Sump - Vertical Fixed Roof Tank
Ajax, Louisiana

Annual Emission Calculations	
Standing Losses (lb):	2.1287
Vapor Space Volume (cu ft):	68.1757
Vapor Density (lb/cu ft):	0.0000
Vapor Space Expansion Factor:	0.0692
Vented Vapor Saturation Factor:	0.9411
Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	68.1757
Tank Diameter (ft):	5.3300
Vapor Space Outage (ft):	3.0555
Tank Shell Height (ft):	6.0000
Average Liquid Height (ft):	3.0000
Roof Outage (ft):	0.0555
Roof Outage (Cone Roof):	
Roof Outage (ft):	0.0555
Roof Height (ft):	0.1666
Roof Slope (ft/ft):	0.0625
Shell Radius (ft):	2.6650
Vapor Density:	
Vapor Density (lb/cu ft):	0.0000
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.3866
Daily Avg. Liquid Surface Temp. (deg. R):	71.0591
Daily Average Ambient Temp. (deg. F):	66.2482
Ideal Gas Constant R (psia cuft / (lb-mol-deg R)):	10.7310
Liquid Bulk Temperature (deg. R):	68.7178
Tank Paint Solar Absorptance (Shell):	0.5800
Tank Paint Solar Absorptance (Roof):	0.5800
Daily Total Solar Insulation Factor (Btu/sqft day):	1,418.7669
Vapor Space Expansion Factor:	
Vapor Space Expansion Factor:	0.0692
Daily Vapor Temperature Range (deg. R):	31.3222
Daily Vapor Pressure Range (psia):	0.2045
Breather Vent Press. Setting Range (psia):	0.0600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.3866
Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia):	0.2961
Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia):	0.5006
Daily Avg. Liquid Surface Temp. (deg. R):	71.0591
Daily Min. Liquid Surface Temp. (deg. R):	63.2285
Daily Max. Liquid Surface Temp. (deg. R):	78.8897
Daily Ambient Temp. Range (deg. R):	21.9311
Vented Vapor Saturation Factor:	
Vented Vapor Saturation Factor:	0.9411
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.3866
Vapor Space Outage (ft):	3.0555

Working Losses (lb):	2.1035
Vapor Molecular Weight (lb/lb-mole):	0.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.3866
Annual Net Throughput (gal/yr.):	11,999,4000
Annual Turnovers:	17.9732
Turnover Factor:	1.0000
Maximum Liquid Volume (gal):	1,001,4429
Maximum Liquid Height (ft):	5.0000
Tank Diameter (ft):	5.3300
Working Loss Product Factor:	1.0000
Total Losses (lb):	4.2322

Source Description: Surfactant (S200) Storage Tank
Source ID: S200 Tank
Tempo ID: IA-12

TOTAL TANK LOSSES

Pollutant	Breathing Losses	Working Losses	Total	Total
	(lb/yr)	(lb/yr)	(lb/yr)	(ton/yr)
2-Butoxyethanol	0.093	0.133	0.226	0.0001
TOTAL VOC	0.093	0.133	0.226	0.0001

Source Description: Surfactant (S200) Storage Tank

Source ID: S200 Tank

Tempo ID: IA-12

TANK INPUT

Parameter	UOM	IA-12
Variables		
Diameter (D)	ft	4
Height (H _S and H _{LX})	ft	5.32
Average Liquid Height in Tank	ft	2.7
Tank Cone Roof Slope (S _R)	ft/ft	0.0625
Breather Vent Pressure (P _{BP})	psig	0.03
Breather Vent Vacuum Setting (P _{BV})	psig	-0.03
Tank Paint Solar Absorptance (α)	-	0.58
Daily Total Solar Insolation Factor (I)	BTU/ft ² *day	1418.7669
Daily Average Ambient Temperature (T _{AA})	°R	530.674401
Daily Ambient Temperature Range (ΔT _A)	°R	15.669102
Liquid Bulk Temperature (T _B)	°R	528.39
Annual Throughput (Q)	bbl/yr	143
Annual Days Tank in Service	days	365
Annual Hours of Operation	hours	8760

Parameter	UOM	Value
Constants		
PI	-	3.14
Ideal Gas Constant	psia*ft ³ / lbmol*R	10.731
Atmospheric Pressure (P _A)	psia	14.63
Conversion Factor	lb/ton	2000

Speciation	WT %
Pollutant	
2-Butoxyethanol	100.0000

Source Description: Surfactant (S200) Storage Tank
 Source ID: S200 Tank
 Tempo ID: IA-12

TANK CALCULATIONS

Parameter	UOM	AP-42 Ch. 7.1 Formula Reference	IA-12
Daily Minimum and Daily Maximum Surface Temperatures			
Daily Average Liquid Surface Temperature (T_{LA})	°R	Eq. 1-27	532.61
Daily Vapor Temperature Range (ΔT_v)	°R	Eq. 1-6	26.13
Daily Minimum Liquid Surface Temperature (T_{LN})	°R	Figure 7.1-17	526.07
Daily Maximum Liquid Surface Temperature (T_{LN})	°R	Figure 7.1-17	539.14
Average Vapor Temperature			
Average Vapor Temperature (T_v)	°R	Eq. 1-32	536.82
Standing Losses [$L_s = 365 V_v W_v K_E K_S$]			
Tank Roof Height (H_R)	ft	Eq. 1-18	0.13
Roof Outage (H_{RO})	ft	Eq. 1-17	0.04
Vapor Space Outage (H_{VO})	ft	Eq. 1-16	2.70
Vapor Space Volume (V_v)	ft ³	Eq. 1-3	34
Vapor Density (W_v)	lb/ft ³	Eq. 1-22	0.00017
2-Butoxyethanol	lb/ft ³	Eq. 1-22	0.00017
Vapor Space Expansion Factor (K_E)	-	Eq. 1-12	0.0470
Vapor Space Expansion Factor (K_E)	-	Eq. 1-5	0.0451
Vented Vapor Saturation Factor (K_S)	-	Eq. 1-21	0.9988
Standing Losses (L_s)	lb/yr	Eq. 1-2	0.0925
2-Butoxyethanol	lb/yr	Eq. 1-2	0.0925
Average Working Losses [$L_w = V_Q K_N K_P W_v K_B$]			
Net Working Loss Throughput (V_Q)	ft ³ /yr	Eq. 1-39	802
Turnovers Per Year (N)	-	Eq. 1-36	19
Working Loss Turnover (Saturation) Factor (K_N) [N≤36]	-	Eq. 1-35	1
Working Loss Turnover (Saturation) Factor (K_N) [N>36]	-	Eq. 1-35	1.73
Working Loss Product Factor (K_P)	-	Eq. 1-35	1
Vent Setting Correction Factor (K_B)	-	Eq. 1-35	1
Working Losses (L_w)	lb/yr	Eq. 1-35	0.1330
2-Butoxyethanol	lb/yr	Eq. 1-35	0.1330

Source Description: Surfactant (S200) Storage Tank
 Source ID: S200 Tank
 Tempo ID: IA-12

VAPOR PRESSURE CALCULATIONS

Parameter	UOM	IA-12
Vapor Pressure at Daily Maximum Liquid Surface Temperature (P_{VM})	psia	0.01088
Vapor Pressure at Daily Minimum Liquid Surface Temperature (P_{VN})	psia	0.00595
Vapor Pressure at Daily Average Liquid Surface Temperature (P_{VA})	psia	0.00808
Daily Vapor Pressure Range (ΔP_V)	psi	0.0049
Breather Vent Pressure Setting Range (ΔP_B)	psi	0.0630

T_{LA} 73 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
2-Butoxyethanol	118.17	100.00	1	0.84624	1.00000	0.01	0.00808	1.00000	118.17
TOTAL		100.00	1.00	0.85	1.00		0.008	1.00	118.17

T_{LN} 66 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
2-Butoxyethanol	118.17	100.00	1	0.84624	1.00000	0.01	0.00595	1.00000	118.17
TOTAL		100.00	1.00	0.85	1.00		0.006	1.00	118.17

T_{LX} 79 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
2-Butoxyethanol	118.17	100.00	1	0.84624	1.00000	0.01	0.01088	1.00000	118.17
TOTAL		100.00	1.00	0.85	1.00		0.011	1.00	118.17

Source Description: Triethylene Glycol (TEG) Storage Tank

Source ID: TEG Tank

Tempo ID: IA-13

TOTAL TANK LOSSES

Pollutant	Breathing Losses	Working Losses	Total	Total
	(lb/yr)	(lb/yr)	(lb/yr)	(ton/yr)
Triethylene Glycol	0.001	0.001	0.002	0.000001
TOTAL VOC	0.001	0.001	0.002	0.000001

Source Description: Triethylene Glycol (TEG) Storage Tank

Source ID: TEG Tank

Tempo ID: IA-13

TANK INPUT

Parameter	UOM	IA-13
Variables		
Diameter (D)	ft	3.5
Height (H _S and H _{LX})	ft	4.58
Average Liquid Height in Tank	ft	2.3
Tank Cone Roof Slope (S _R)	ft/ft	0.0625
Breather Vent Pressure (P _{BP})	psig	0.03
Breather Vent Vacuum Setting (P _{BV})	psig	-0.03
Tank Paint Solar Absorptance (α)	-	0.58
Daily Total Solar Insolation Factor (I)	BTU/ft ² *day	1418.7669
Daily Average Ambient Temperature (T _{AA})	°R	530.674401
Daily Ambient Temperature Range (ΔT _A)	°R	15.669102
Liquid Bulk Temperature (T _B)	°R	528.39
Annual Throughput (Q)	bbl/yr	94
Annual Days Tank in Service	days	365
Annual Hours of Operation	hours	8760

Parameter	UOM	Value
Constants		
PI	-	3.14
Ideal Gas Constant	psia*ft ³ / lbmol*R	10.731
Atmospheric Pressure (P _A)	psia	14.63
Conversion Factor	lb/ton	2000

Speciation	WT %
Pollutant	
Triethylene Glycol	100.0000

Source Description: Triethylene Glycol (TEG) Storage Tank
 Source ID: TEG Tank
 Tempo ID: IA-13

TANK CALCULATIONS

Parameter	UOM	AP-42 Ch. 7.1 Formula Reference	IA-13
Daily Minimum and Daily Maximum Surface Temperatures			
Daily Average Liquid Surface Temperature (T_{LA})	°R	Eq. 1-27	532.61
Daily Vapor Temperature Range (ΔT_v)	°R	Eq. 1-6	26.14
Daily Minimum Liquid Surface Temperature (T_{LN})	°R	Figure 7.1-17	526.08
Daily Maximum Liquid Surface Temperature (T_{LX})	°R	Figure 7.1-17	539.15
Average Vapor Temperature			
Average Vapor Temperature (T_v)	°R	Eq. 1-32	536.84
Standing Losses [$L_s = 365 V_v W_v K_E K_S$]			
Tank Roof Height (H_R)	ft	Eq. 1-18	0.11
Roof Outage (H_{RO})	ft	Eq. 1-17	0.04
Vapor Space Outage (H_{VO})	ft	Eq. 1-16	2.33
Vapor Space Volume (V_v)	ft ³	Eq. 1-3	22
Vapor Density (W_v)	lb/ft ³	Eq. 1-22	0.00000
Triethylene Glycol	lb/ft ³	Eq. 1-22	0.00000
Vapor Space Expansion Factor (K_E)	-	Eq. 1-12	0.0470
Vapor Space Expansion Factor (K_E)	-	Eq. 1-5	0.0448
Vented Vapor Saturation Factor (K_S)	-	Eq. 1-21	1.0000
Standing Losses (L_s)	lb/yr	Eq. 1-2	0.0007
Triethylene Glycol	lb/yr	Eq. 1-2	0.0007
Average Working Losses [$L_w = V_o K_N K_P W_v K_B$]			
Net Working Loss Throughput (V_o)	ft ³ /yr	Eq. 1-39	529
Turnovers Per Year (N)	-	Eq. 1-36	21
Working Loss Turnover (Saturation) Factor (K_N) [$N \leq 36$]	-	Eq. 1-35	1
Working Loss Turnover (Saturation) Factor (K_N) [$N > 36$]	-	Eq. 1-35	1.58
Working Loss Product Factor (K_P)	-	Eq. 1-35	1
Vent Setting Correction Factor (K_B)	-	Eq. 1-35	1
Working Losses (L_w)	lb/yr	Eq. 1-35	0.0010
Triethylene Glycol	lb/yr	Eq. 1-35	0.0010

Source Description: Triethylene Glycol (TEG) Storage Tank
 Source ID: TEG Tank
 Tempo ID: IA-13

VAPOR PRESSURE CALCULATIONS

Parameter	UOM	IA-13
Vapor Pressure at Daily Maximum Liquid Surface Temperature (P_{VX})	psia	0.00010
Vapor Pressure at Daily Minimum Liquid Surface Temperature (P_{VN})	psia	0.00005
Vapor Pressure at Daily Average Liquid Surface Temperature (P_{VA})	psia	0.00007
Daily Vapor Pressure Range (ΔP_V)	psi	0.0000
Breather Vent Pressure Setting Range (ΔP_B)	psi	0.0630

T_{LA} 73 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
Triethylene Glycol	150.17	100.00	1	0.66591	1.00000	0.00	0.00007	1.00000	150.17
TOTAL		100.00	1.00	0.67	1.00	0.000	0.000	1.00	150.17

T_{LN} 66 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
Triethylene Glycol	150.17	100.00	1	0.66591	1.00000	0.00	0.00005	1.00000	150.17
TOTAL		100.00	1.00	0.67	1.00	0.000	0.000	1.00	150.17

T_{LX} 79 °F

Compound	Mole Weight of Compound	Composition of Liquid	Composition of Liquid	Moles per 100 lb of liquid	Mole Fraction in liquid	Pure Component Vapor Pressure	Component Partial Press	Vapor Mole Fraction	Vapor Molecular Weight
	lb/lb-mole	wt%	wt fraction			psia	psia		lb/lb-mole
Triethylene Glycol	150.17	100.00	1	0.66591	1.00000	0.00	0.00010	1.00000	150.17
TOTAL		100.00	1.00	0.67	1.00	0.000	0.000	1.00	150.17

APPENDIX B: FEE CALCULATION

**ET Gathering & Processing LLC
Ajax Amine Plant
Permit Application Fees Determination
Title V Permit Minor Modification for Permit No. 0760-01944-V0**

REFERENCE:**LAC.33:III.Chapter 2****Section 223 Fee Schedule Listing**

Fee Number: 1712
SIC Code: 1389
Title V Minor Modification Fee = \$1,452.00

Section 211.A PSD Application Fee

Surcharge of 50% of the application fee when a PSD Permit Application is being processed. ETGP is proposing a minor modification; therefore, not requiring the preparation of a PSD Permit Application; therefore, this fee does not apply.

Section 211.A Air Toxics Permit Application Fee

Surcharge of 10% of the permit application fee to be charged when there is an increase in toxic air pollutant emissions above the Minimum Emission Rates (MERs) listed in LAC.33:III.5112, Table 51.1. There is an increase in H₂S toxic air pollutant emissions above the MER; therefore, this fee applies.

Section 211.A "NSPS" Maintenance Fee

Surcharge of 25% of the permit application fee to be charged for any permit application that includes the addition of new equipment subject to NSPS regulations. Because the two newly proposed compressors are subject to the provisions of NSPS JJJJ, the NSPS maintenance fee applies.

Permit Application Fees Determination

= \$1,452.00 [Title V Minor Modification Fee] + \$0.00 [50% PSD Application Fee] + \$145.20 [10% Air Toxics Application Fee] + \$363.00 [25% NSPS Maintenance Fee]

Total Fees = \$1,960.20¹

Online Payment Transaction Number # O25F1C0TGF

¹ ETGP has paid via Online Payment Transaction O25F1C0TGF in an amount of \$2,053.00 utilizing minor modification Fee Code 0130 as there is no available Fee Code of 1712 with NSPS and Toxics surcharge.

APPENDIX C: SECRETARY OF STATE CERTIFICATION

10/5/23, 9:30 AM

Commercial - Search

State of
Louisiana
Secretary of
State



COMMERCIAL DIVISION
225.925.4704

Fax Numbers
225.932.5317 (Admin. Services)
225.932.5314 (Corporations)
225.932.5318 (UCC)

Name	Type	City	Status
ET GATHERING & PROCESSING LLC	Limited Liability Company (Non-Louisiana)	DALLAS	Active

Previous Names

Business: ET GATHERING & PROCESSING LLC
Charter Number: 45576820Q
Registration Date: 8/31/2023

Domicile Address

8111 WESTCHESTER DRIVE, SUITE 600
DALLAS, TX 75225

Mailing Address

8801 S. YALE AVENUE, SUITE 200
TULSA, OK 74137

Principal Business Office

8111 WESTCHESTER DRIVE, SUITE 600
DALLAS, TX 75225

Registered Office in Louisiana

450 LAUREL STREET, 8TH FLOOR
BATON ROUGE, LA 70801

Principal Business Establishment in Louisiana

450 LAUREL STREET, 8TH FLOOR
BATON ROUGE, LA 70801

Status

Status: Active
Annual Report Status: In Good Standing
Qualified: 8/31/2023
Last Report Filed: N/A
Type: Limited Liability Company (Non-Louisiana)

Registered Agent(s)

Agent:	CORPORATION SERVICE COMPANY
Address 1:	450 LAUREL STREET, 8TH FLOOR
City, State, Zip:	BATON ROUGE, LA 70801
Appointment Date:	8/31/2023

Officer(s)

Additional Officers: No

10/5/23, 9:30 AM

Commercial - Search

Officer:	LA GRANGE ACQUISITION, L.P.
Title:	Member
Address 1:	8111 WESTCHESTER DRIVE, SUITE 600
City, State, Zip:	DALLAS, TX 75225

Amendments on File (1)

Description	Date
Foreign LLC Statement of Change	9/1/2023

Print